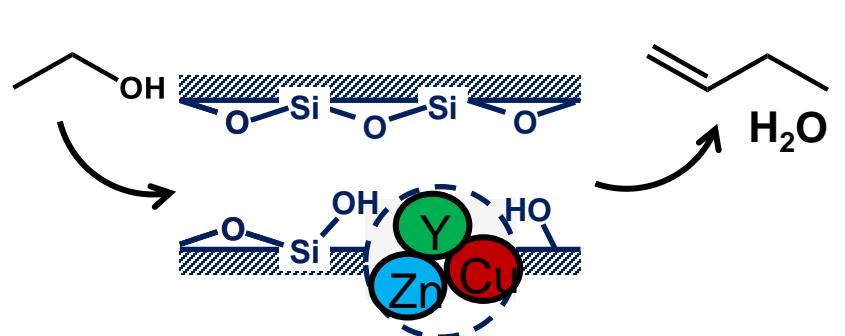


Quantification of Active Sites for Ethanol Upgrading over Yttrium-Containing Beta Zeotypes

James W. Harris



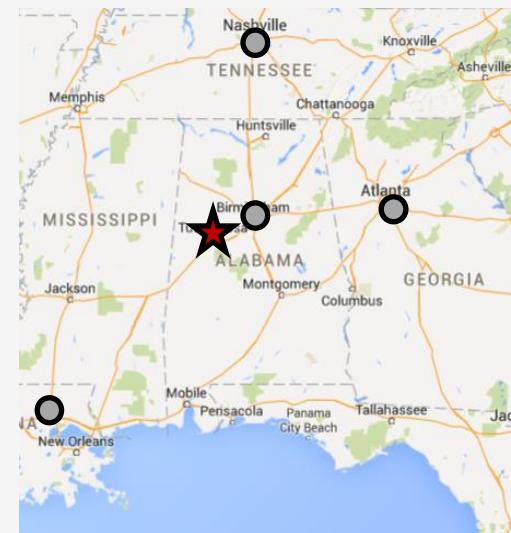
Department of Chemical and
Biological Engineering
The University of Alabama

Halder Topsoe Catalysis Forum
Gilleleje, Denmark
September 13th, 2023

The University of Alabama

Tuscaloosa, AL

Capstone state public university of Alabama (est. 1831)
1000 acre residential campus
37,842 students (2020)
Tuscaloosa, AL (pop. 101,129)



The University of Alabama

Tuscaloosa, AL



- 3rd oldest engineering program in the US (1837)
- Chemical engineering program over 100 years old (1910)
 - >600 UG students; 6th largest in US & Canada
 - ~55 PhD Students, 19 Faculty

Ranked #1 for **Goldwater Scholars** since 2007

Often ranked in the top 5 in the nation for **National Merit Finalists**

The University of Alabama

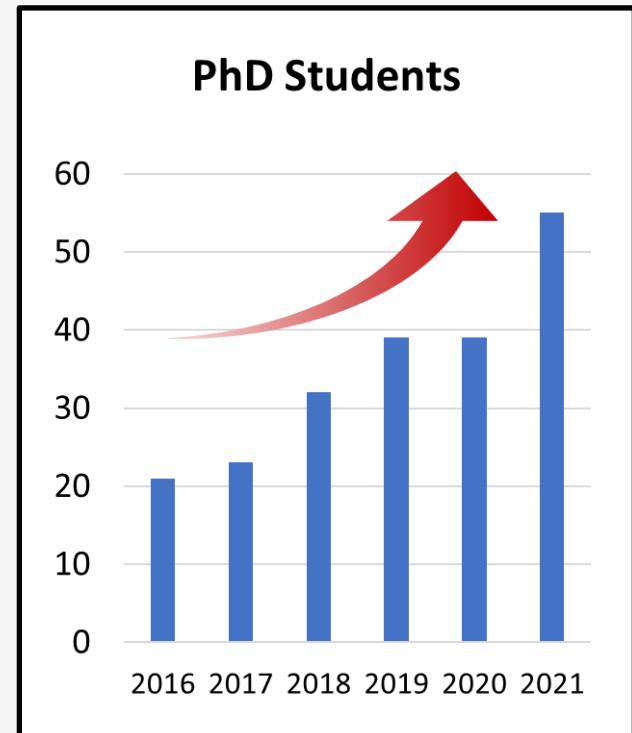
Tuscaloosa, AL

Rapid Expansion of Faculty Expertise

- 8 assistant professors
- ~30% of the faculty have received NSF-CAREER Awards

A Period of Unprecedented Growth

- Number of PhD students up 260% in over five years
- External research funding growing at an average pace of 36% per year over the last five years



Harris Laboratory Personnel



Research Group

1 Postdoc:

Dr. Adam Twombly

6 PhD Students:

Alex Minne

Syd Foster

Ethan Iaia

Shivangi Borate

Elyse Kimpiab

Britney Mack

5 B.S. ChBE students

Treycen Garton

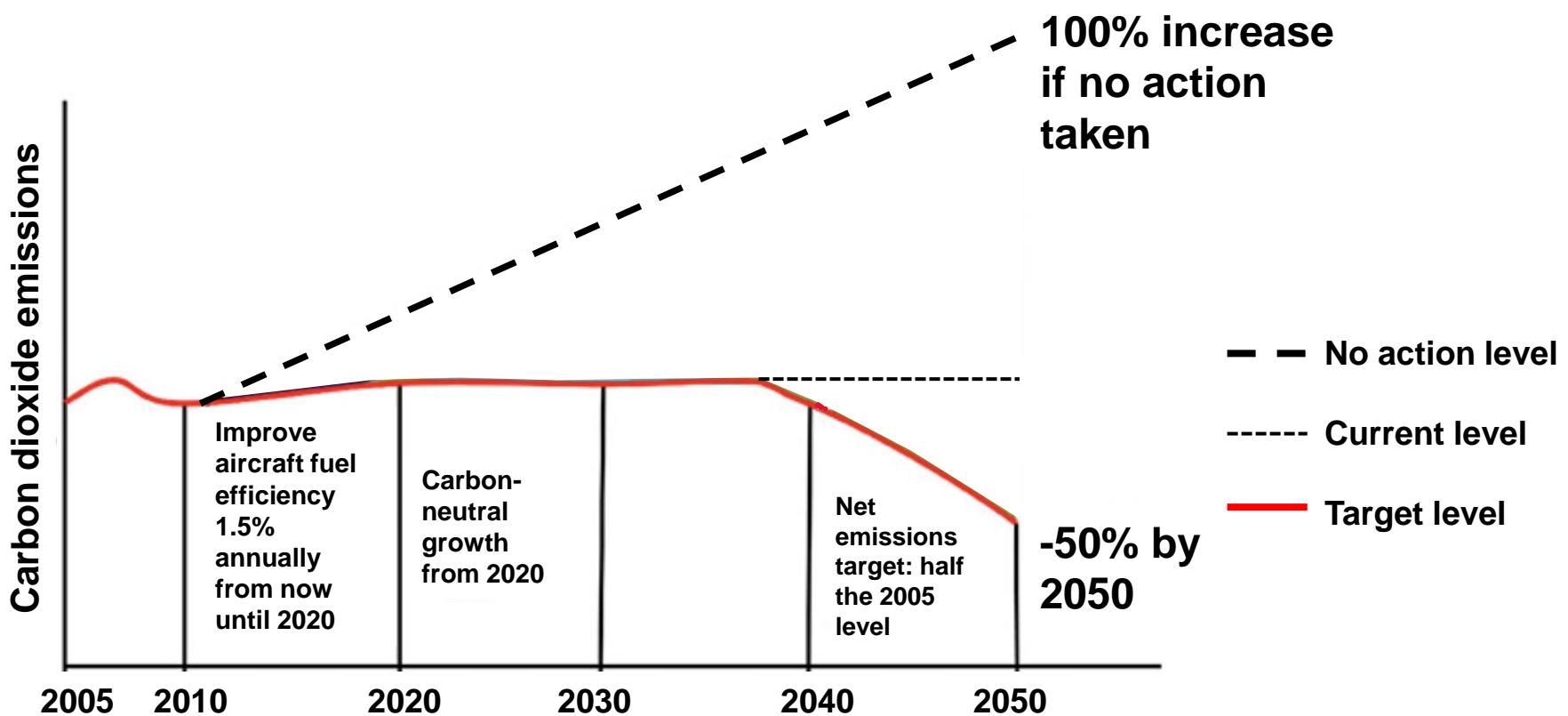
Adam Honson

Mary Elizabeth Martin

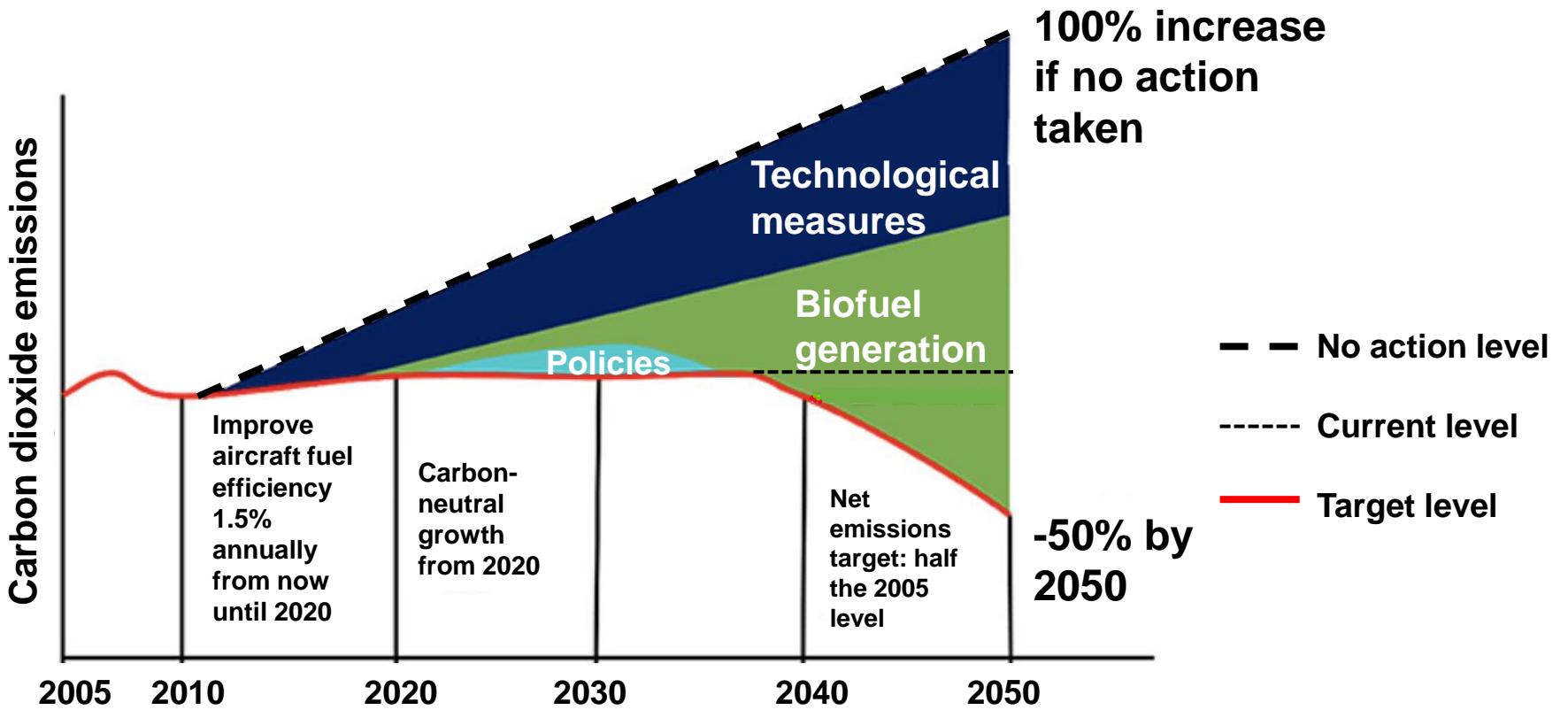
Gabe Miller

Katherine Perkinson

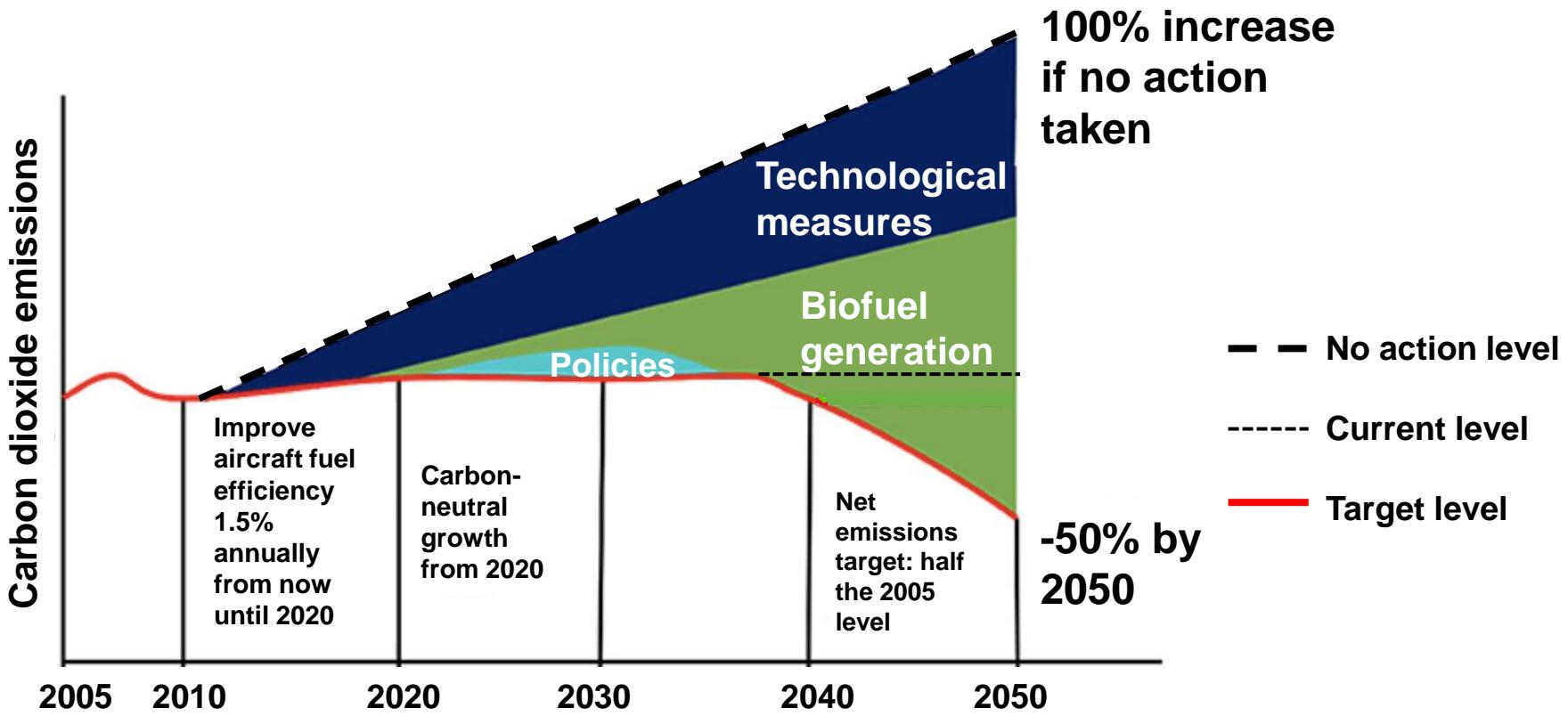
IATA's target net carbon emission



IATA's target net carbon emission



IATA's target net carbon emission



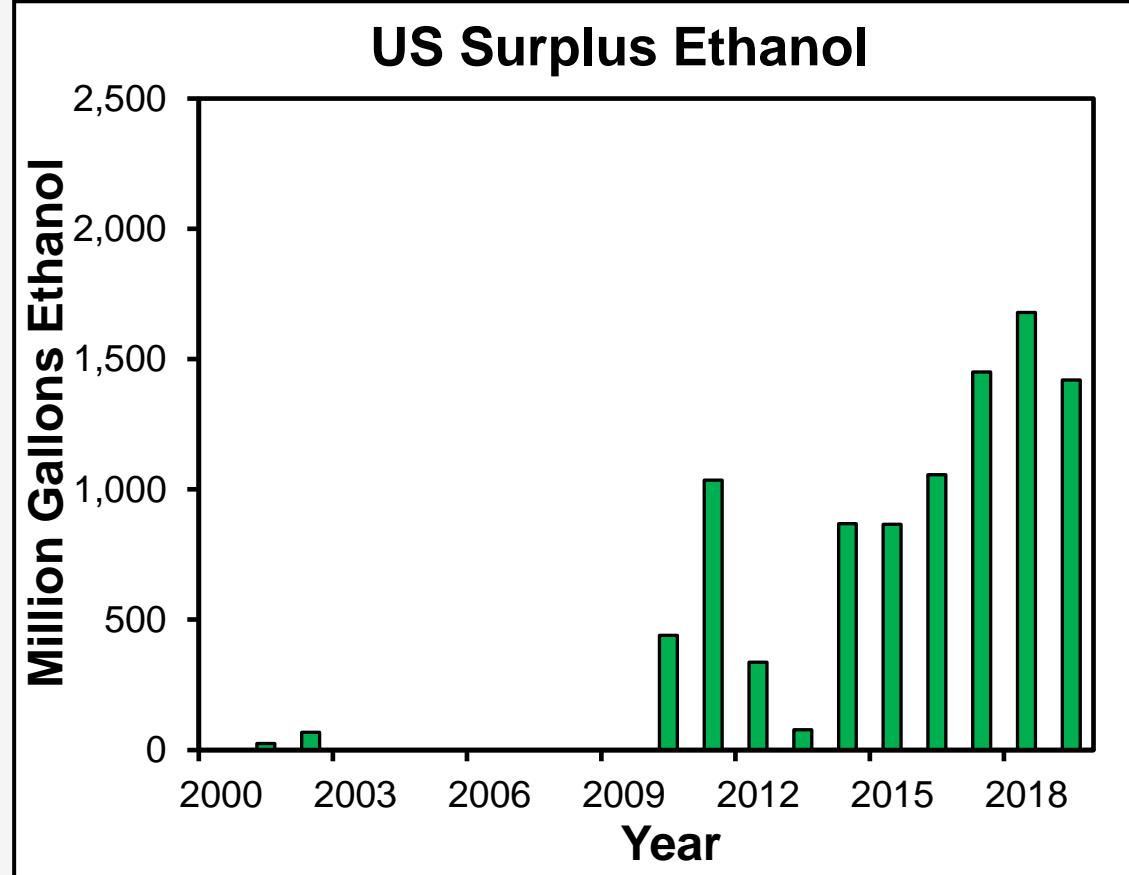
Highest mitigation contribution from sustainable jet fuel (SAF) generation

Increasingly Large Ethanol Surplus

Biomass (Corn)



Ethanol



Upgrading Ethanol to Jet Fuel

Biomass (Corn)



Ethanol

Jet Fuel ($C_{>9}$)



**Alkanes, Olefins,
BTX**

Upgrading Ethanol to Jet Fuel

Biomass (Corn)



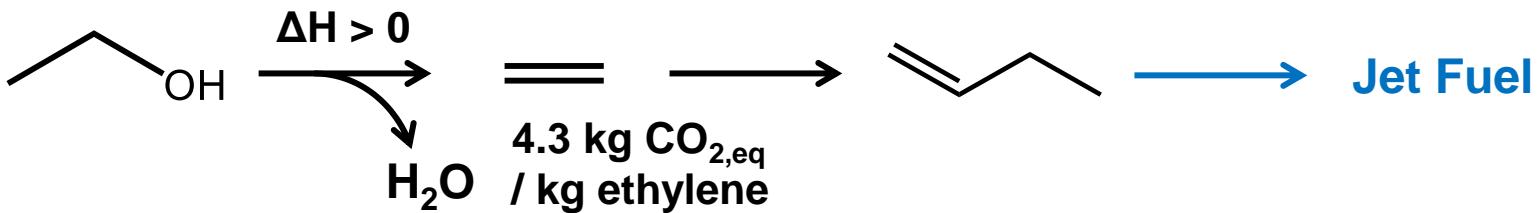
Ethanol

Jet Fuel ($C_{>9}$)

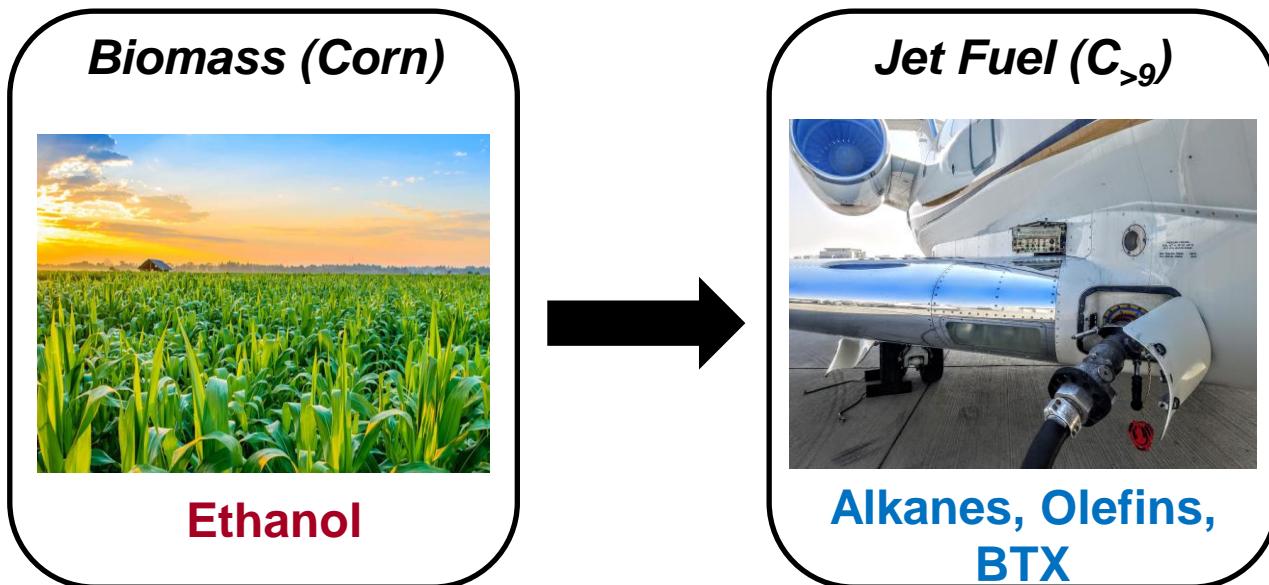


**Alkanes, Olefins,
BTX**

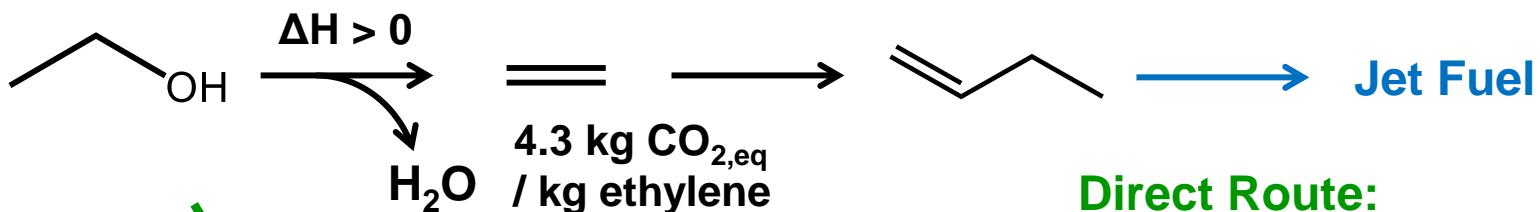
Current Route:



Upgrading Ethanol to Jet Fuel



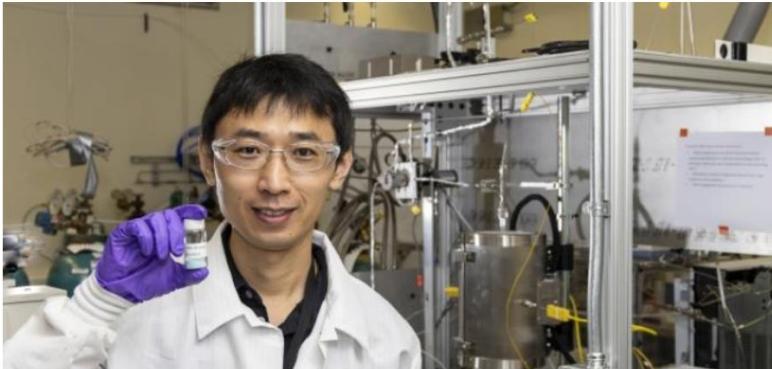
Current Route:



Direct Route:
Single step processes reduces GHG emission by 50%

Upgrading Ethanol to Jet Fuel

Prometheus Fuels licenses energy-saving ORNL ethanol-to-jet-fuel process



Vertimass licenses ORNL biofuel-to-hydrocarbon conversion technology

Topics: Materials • Clean Energy • Functional Materials for Energy • Biological Systems

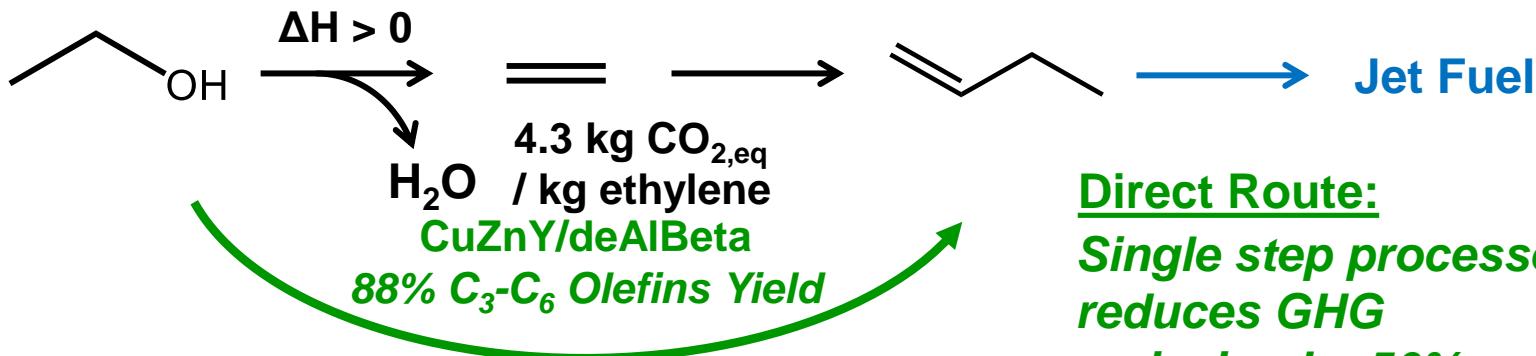
March 6, 2014

OAK RIDGE, Tenn., March 6, 2014 — Vertimass LLC, a California-based start-up company, has licensed an Oak Ridge National Laboratory technology that directly converts ethanol into a hydrocarbon blend-stock for use in transportation fuels.

The ORNL technology offers a new pathway to



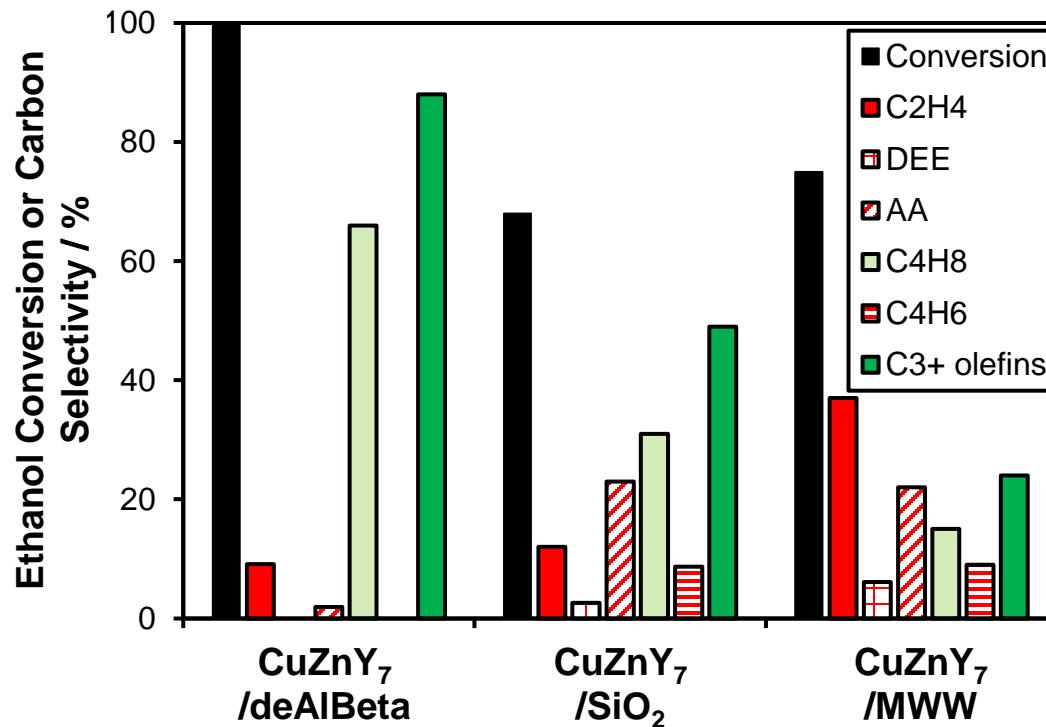
Current Route:



Direct Route:
Single step processes reduces GHG emission by 50%

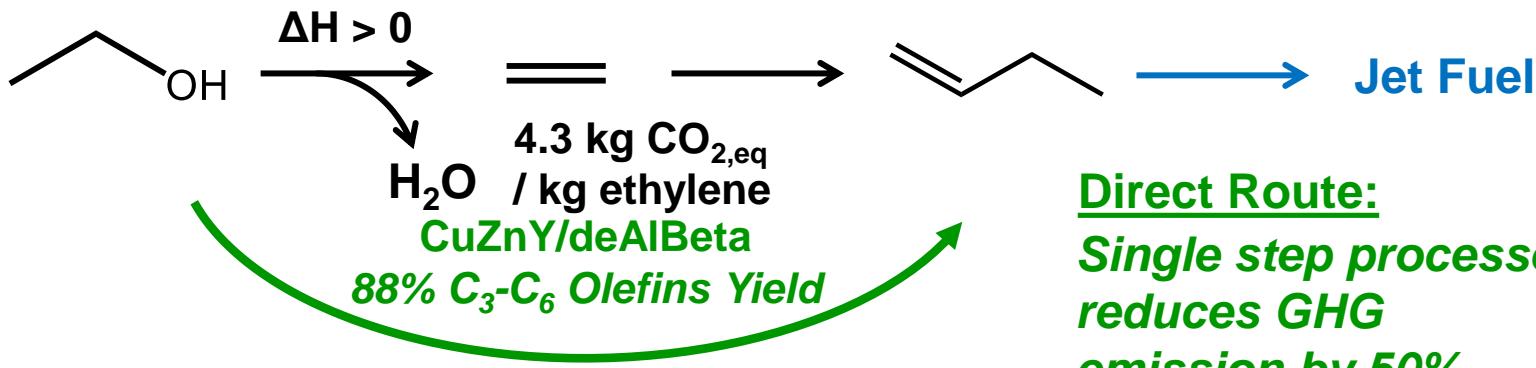
A cheaper and more sustainable route for converting ethanol to jet fuel

Upgrading Ethanol to Jet Fuel over CuZnY/deAlBeta



Reaction Conds.:
623 K, 7.1 kPa
C₂H₅OH, 94.3 kPa
H₂, WHSV 0.51 h⁻¹

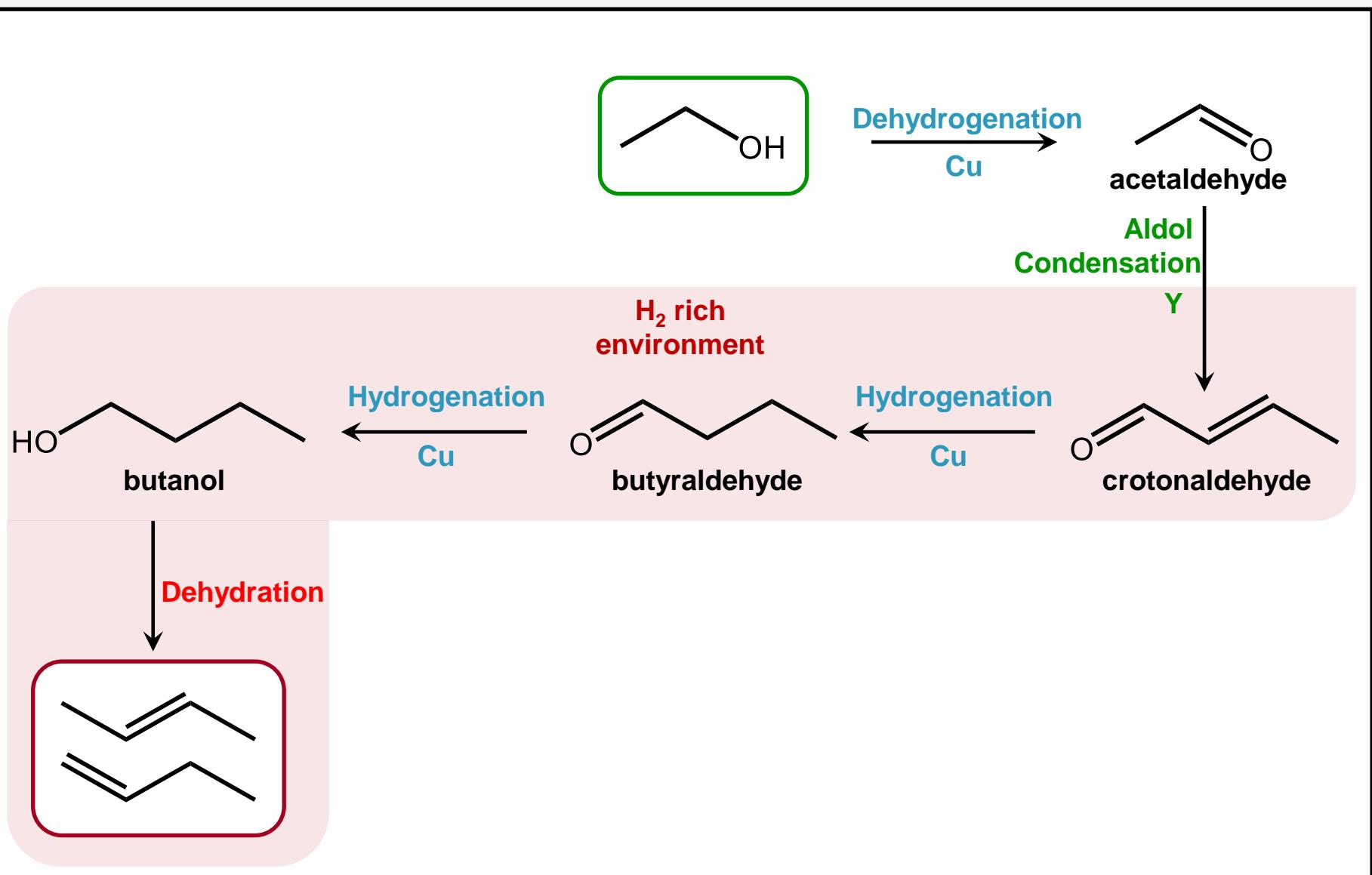
Zhang et al., ACS Catal., 11 (2021)
9885-9897



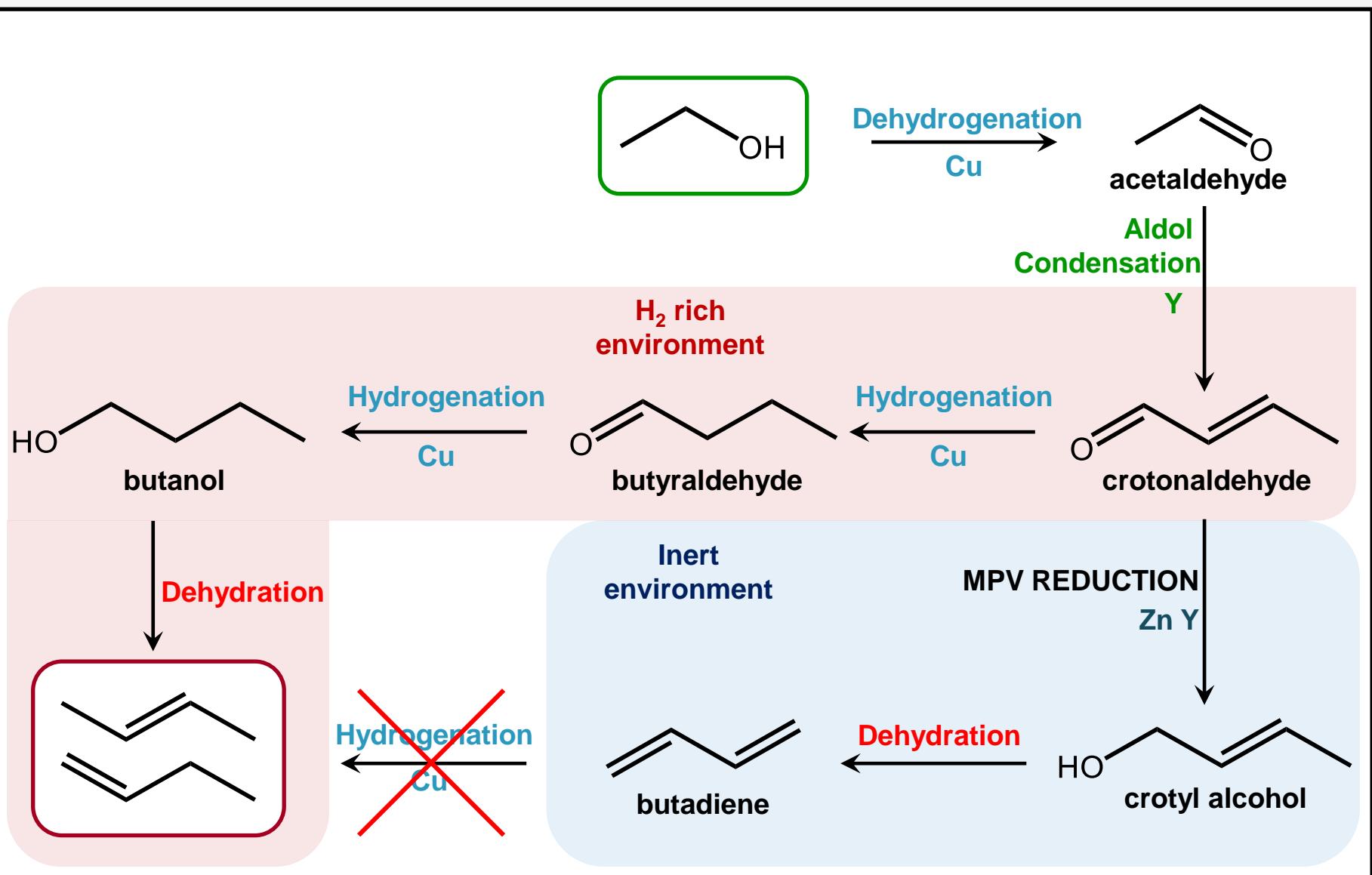
Direct Route:
Single step processes
reduces GHG
emission by 50%

High selectivity to C₃₊ olefins without significant C₂H₄, DEE, or C₄H₆ formation

Proposed Ethanol to Butene Reaction Pathway

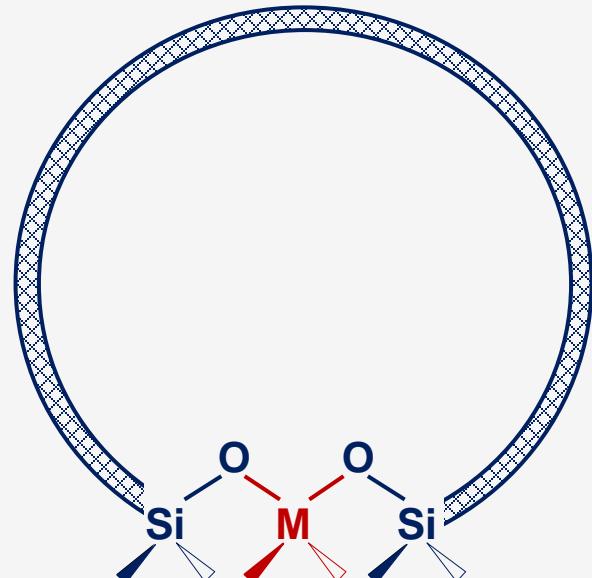


Proposed Ethanol to Butene Reaction Pathway



Metal-containing porous catalysts have broad site distributions

Secondary Confining Pore

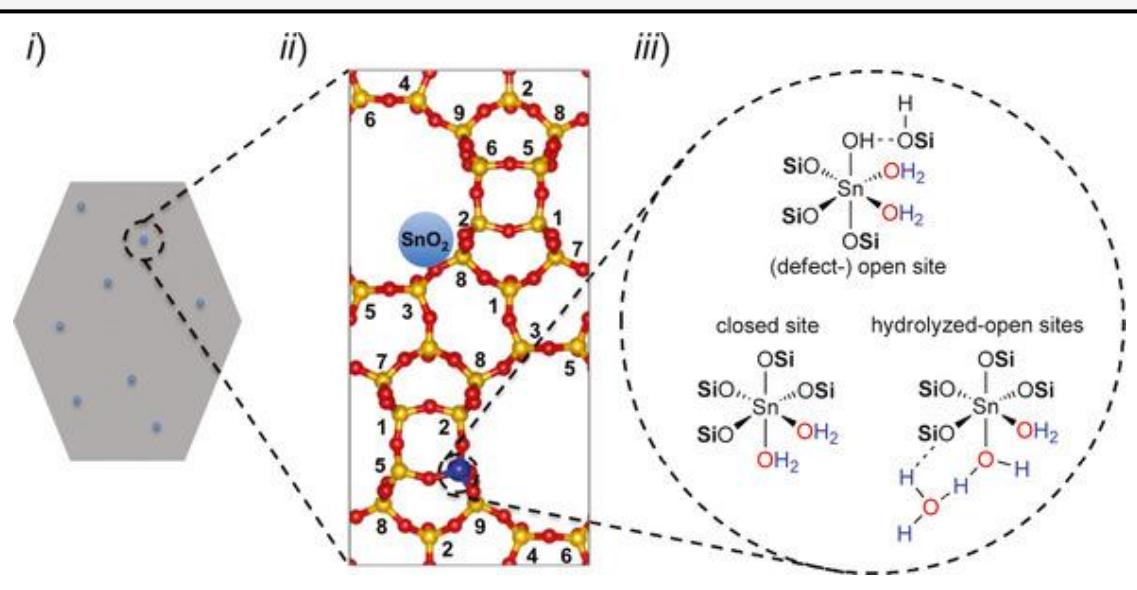


Primary Binding Site

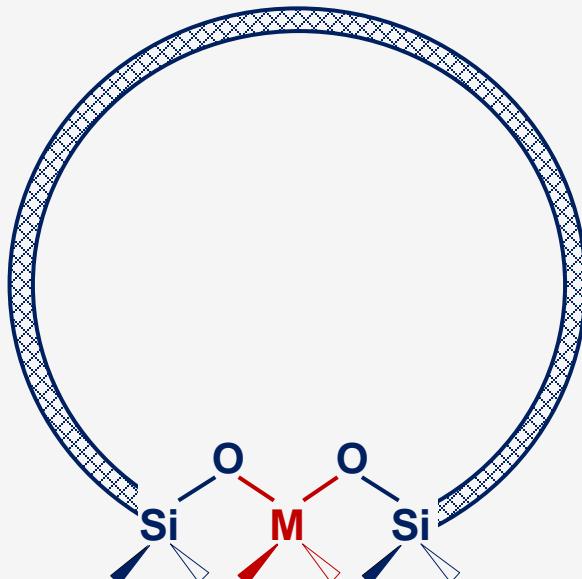
- Different oxidation number
- Different T-sites / pore geometry
- Spatial distributions
- Different local coordination

Metal-containing porous catalysts have broad site distributions

Zeolites With Framework Metal Atoms

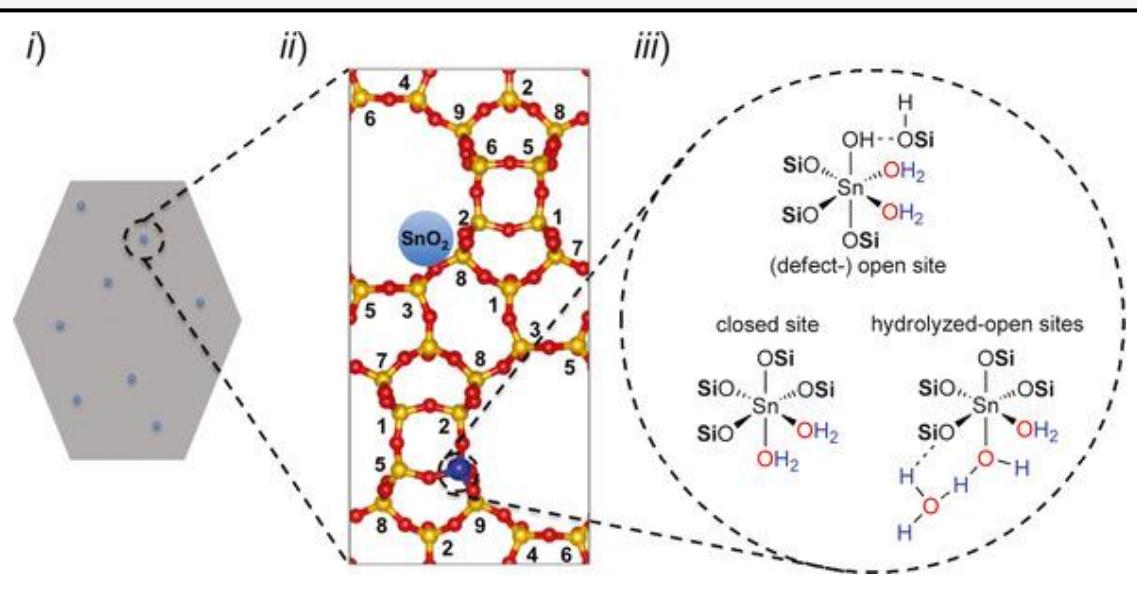


Secondary Confining Pore

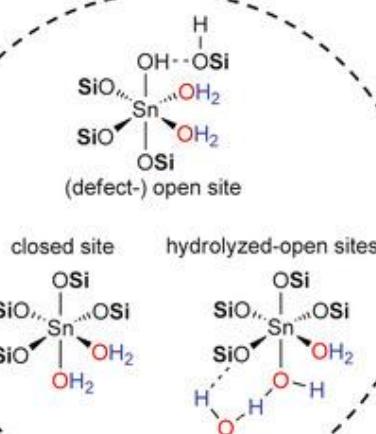


Metal-containing porous catalysts have broad site distributions

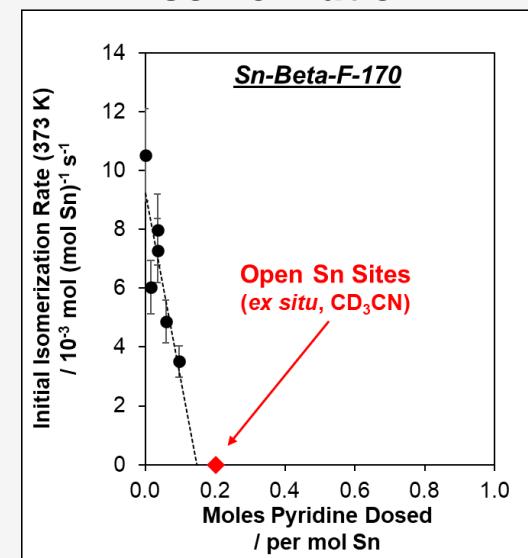
Zeolites With Framework Metal Atoms



iii)



~20% of Sn in Sn-Beta catalyzes glucose isomerization



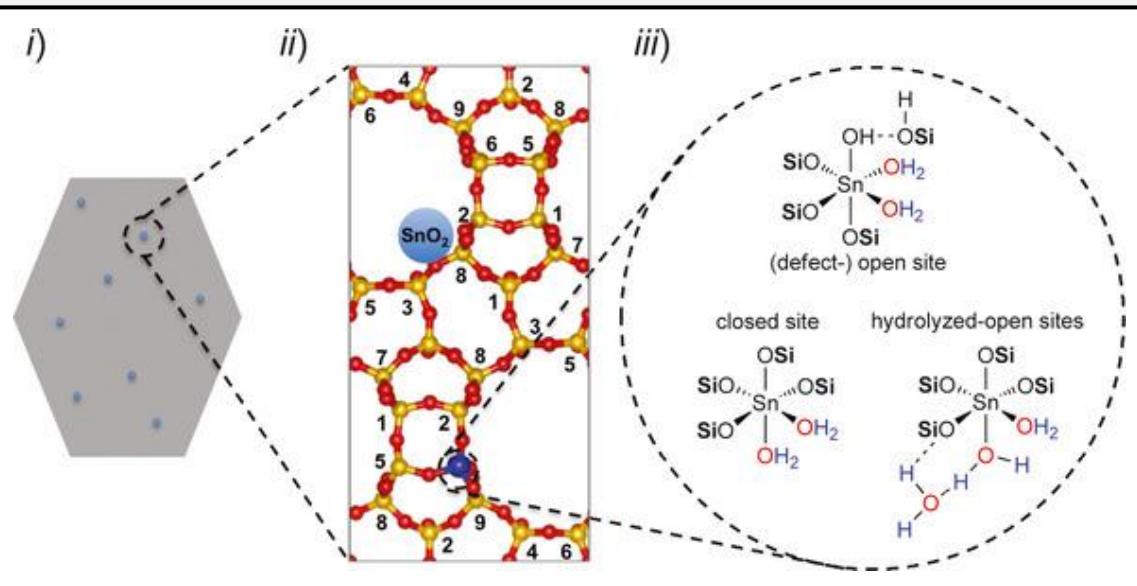
Metal-containing porous catalysts have broad site distributions

Zeolites With Framework Metal Atoms

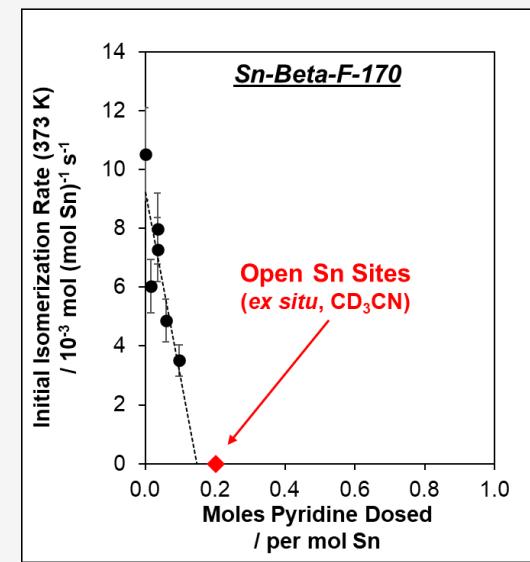
i)

ii)

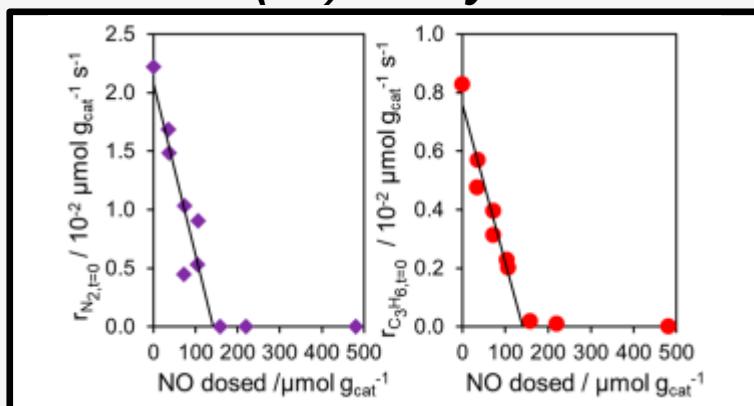
iii)



~20% of Sn in Sn-Beta catalyzes glucose isomerization



~6% of Fe in MIL-100(Fe) catalyzes C-H bond activation



Simons et al., JACS, 141 (2019) 18142-18151

Harris et al., J. Catal., 335 (2016) 141-154

Wolf et al., Helv. Chim. Acta, 99 (2016) 916-927

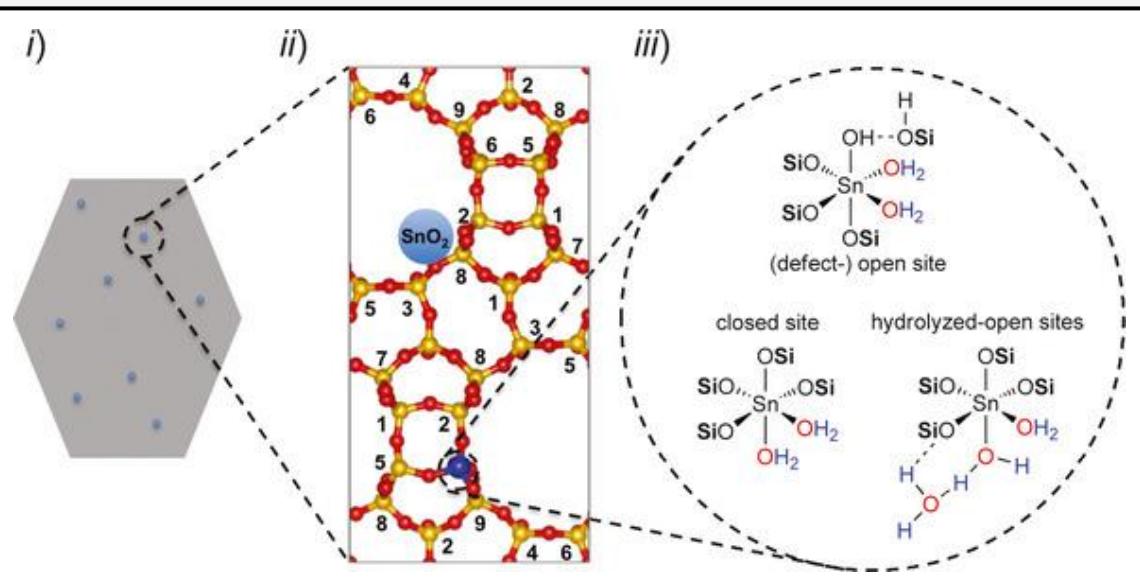
Metal-containing porous catalysts have broad site distributions

Zeolites With Framework Metal Atoms

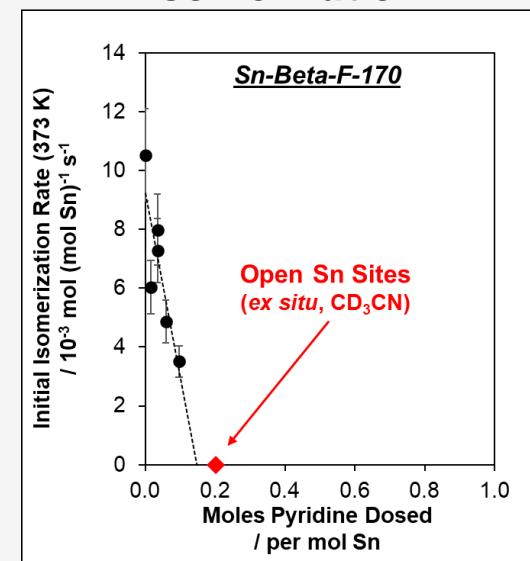
i)

ii)

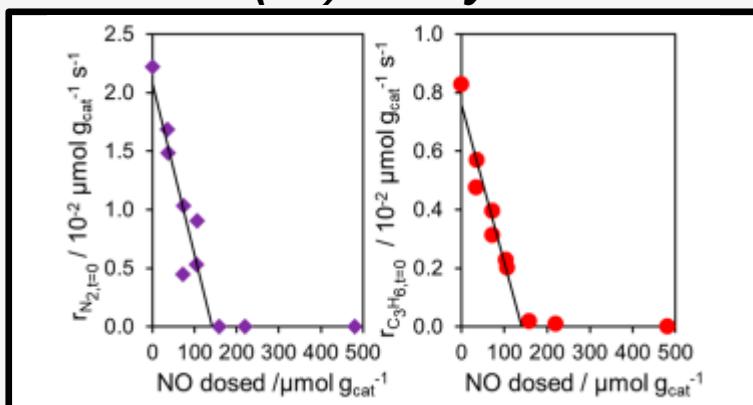
iii)



~20% of Sn in Sn-Beta catalyzes glucose isomerization



~6% of Fe in MIL-100(Fe) catalyzes C-H bond activation



Need to quantify the subset of sites that perform the catalysis!

Simons et al., JACS, 141 (2019) 18142-18151

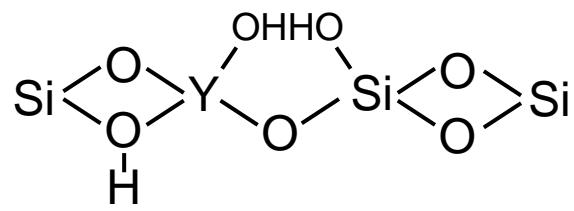
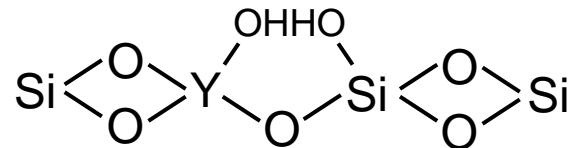
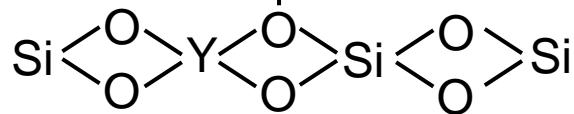
Harris et al., J. Catal., 335 (2016) 141-154

Wolf et al., Helv. Chim. Acta, 99 (2016) 916-927

What sites are relevant in (Cu, Zn)Y/deAlBeta catalysts?

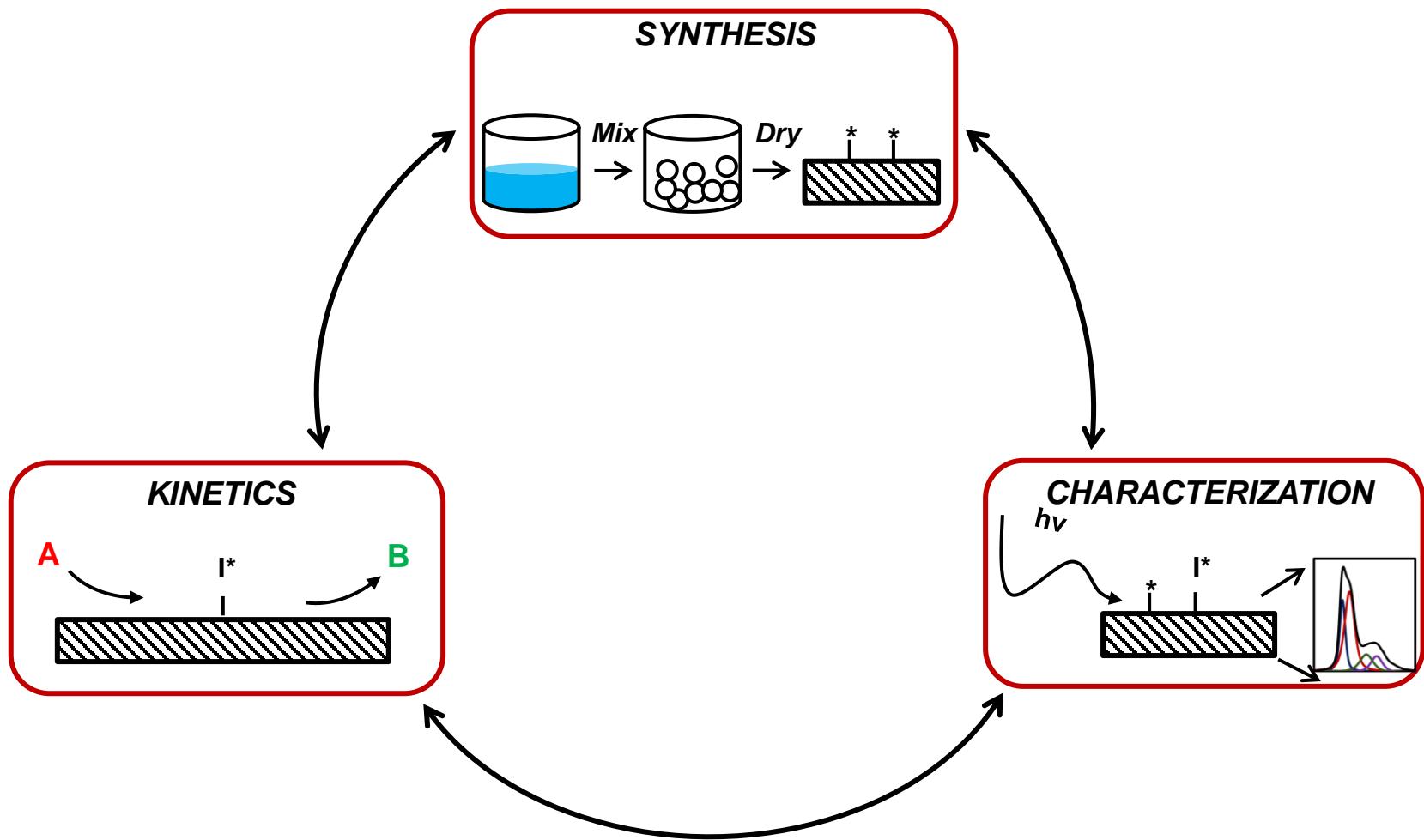
**What are the active sites
and how many are there?**

H⁺

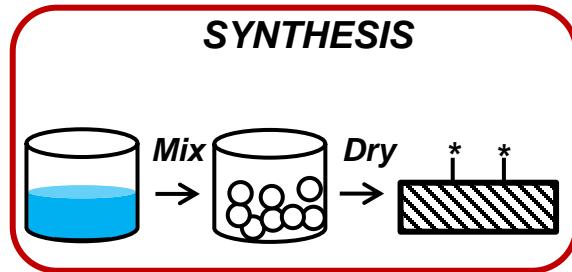


???

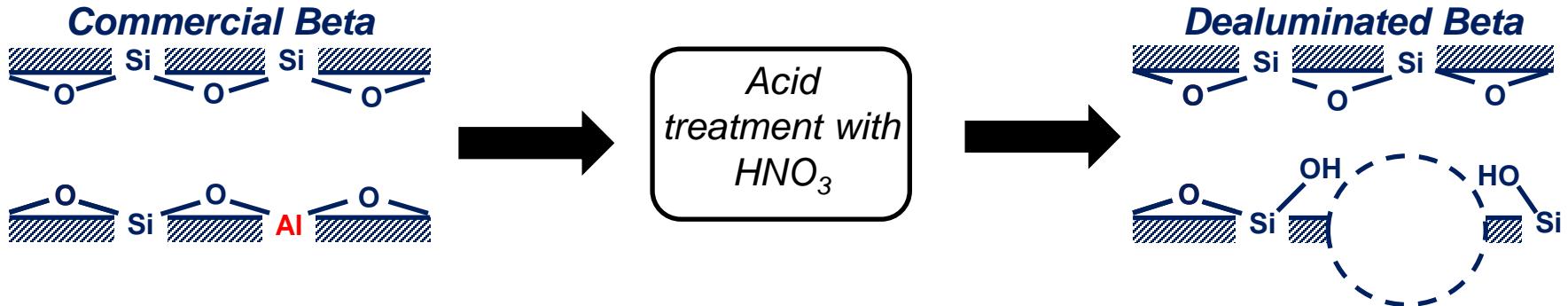
Research Strategy



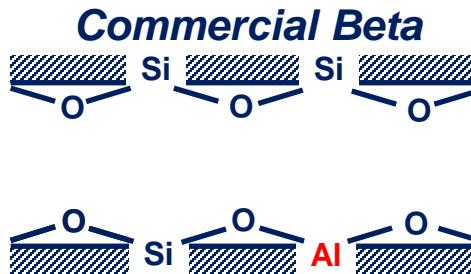
Synthesizing Beta zeolite



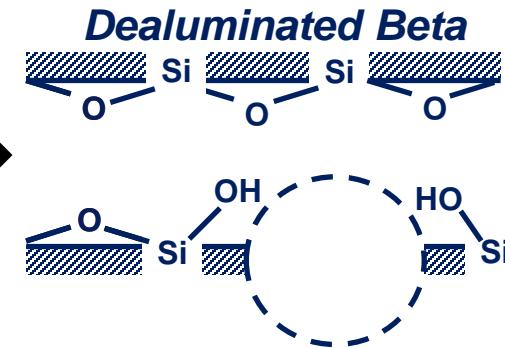
Dealuminating Beta zeolite



Metal incorporation into dealuminated Beta (deAlBeta)

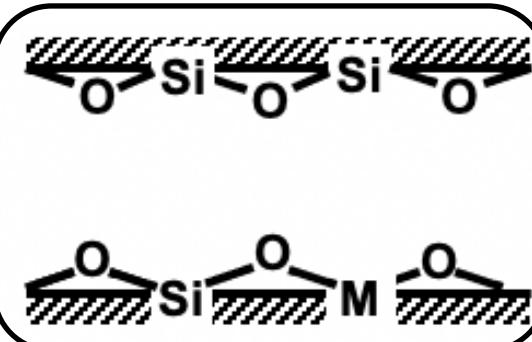


Acid treatment with HNO_3



Solid State Ion Exchange (SSIE)

deAlBeta + Metal nitrate salt

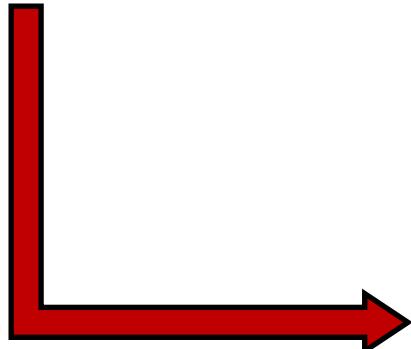


Incipient Wetness Impregnation (IWI)

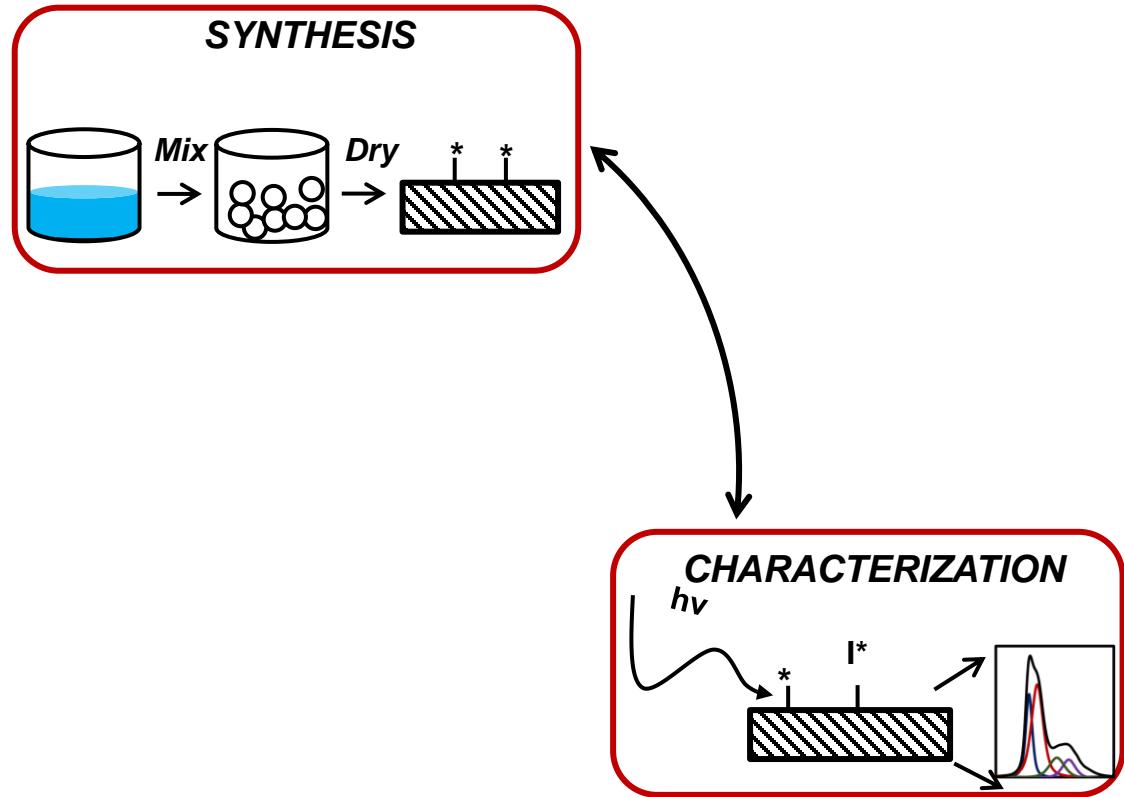
Metal nitrate salt sol'n
deAlBeta



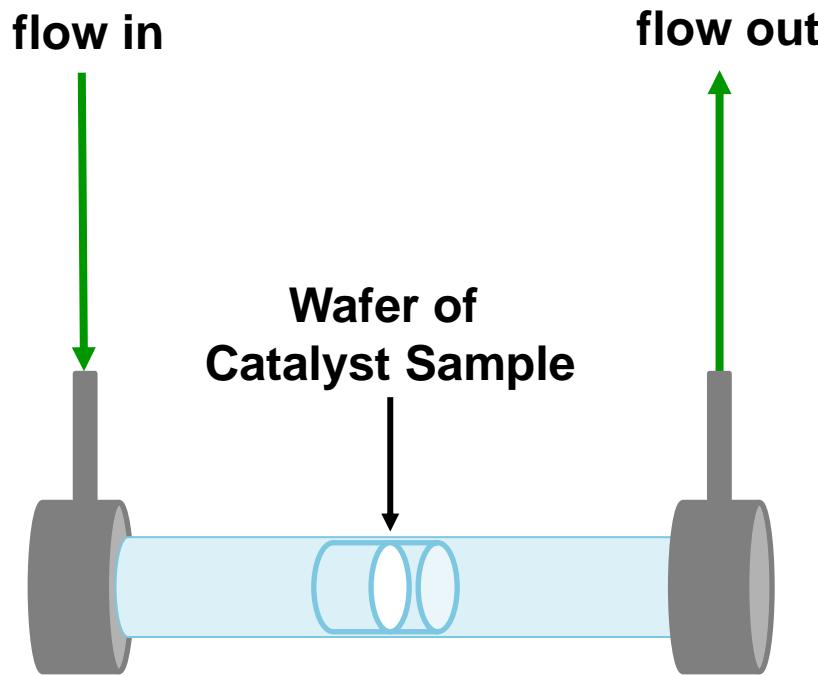
550 °C, 1 °C /min
Air



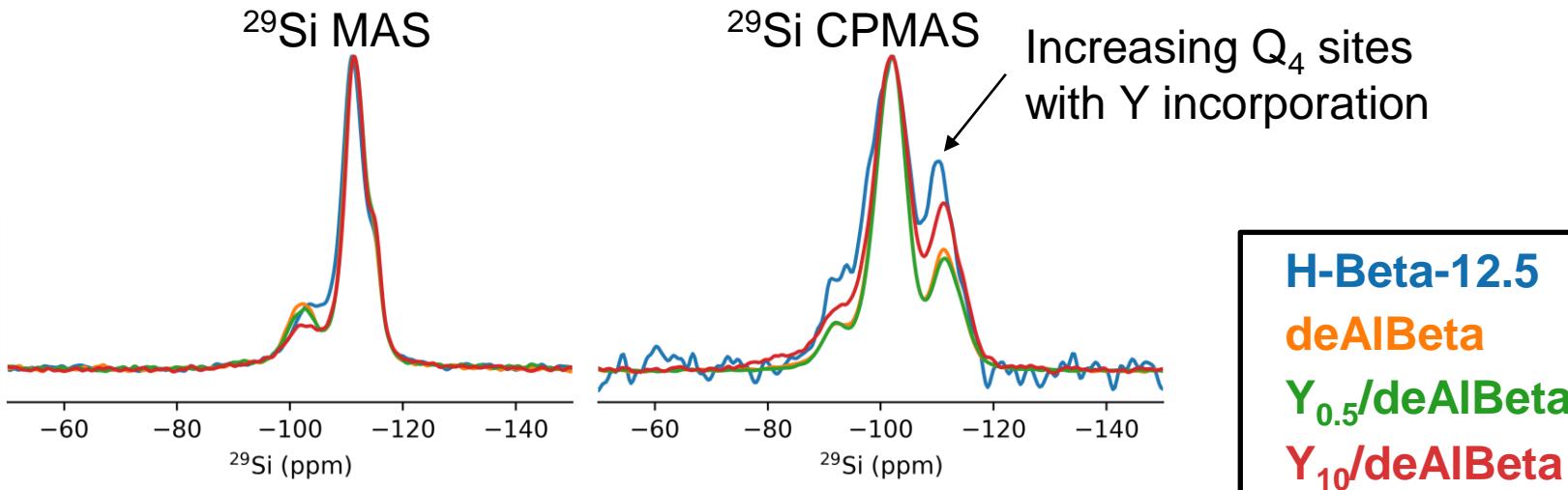
Characterizing the catalysts



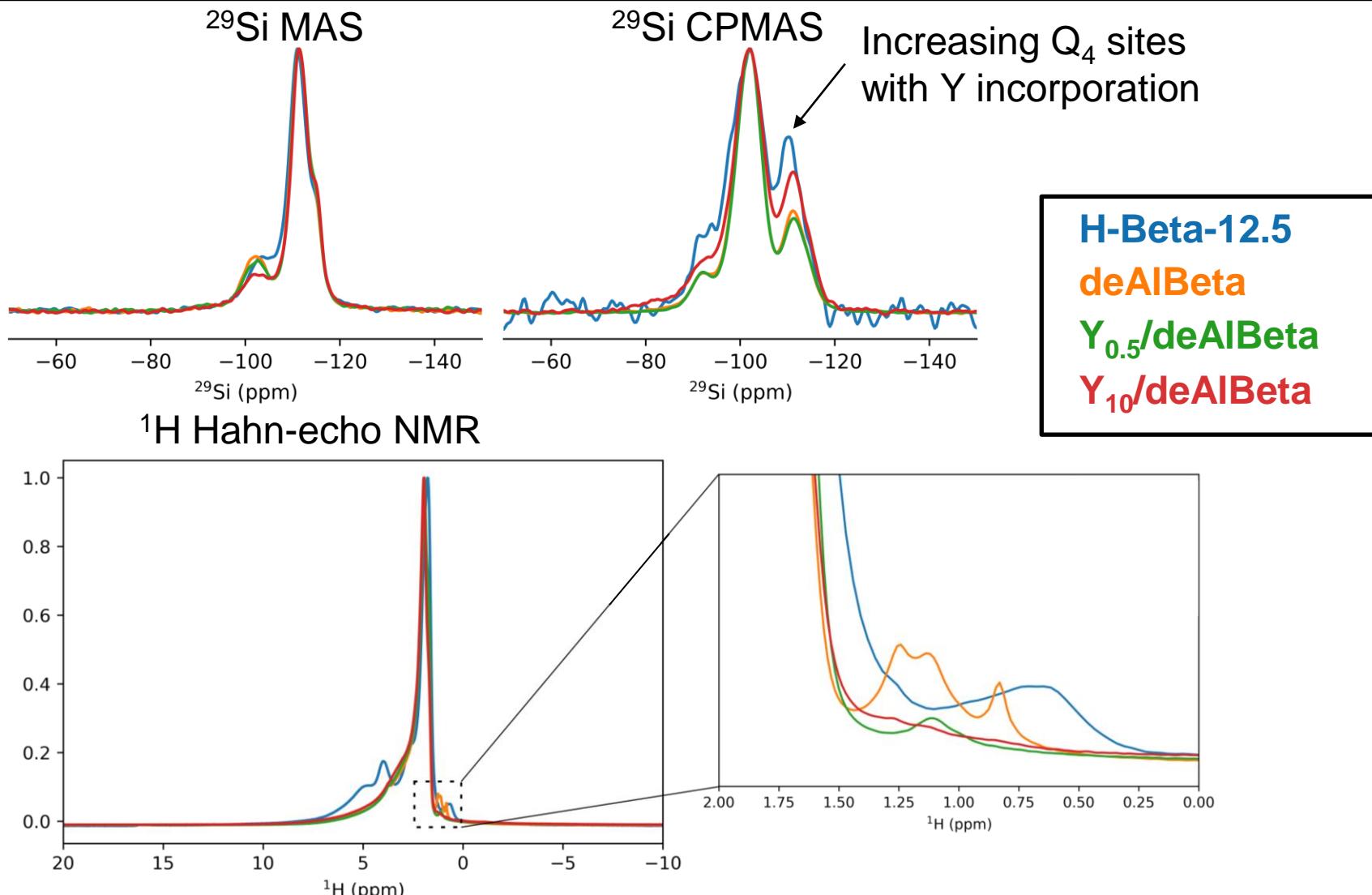
Fourier Transformed Infrared Spectroscopy



SSNMR of Y/deAlBeta Samples

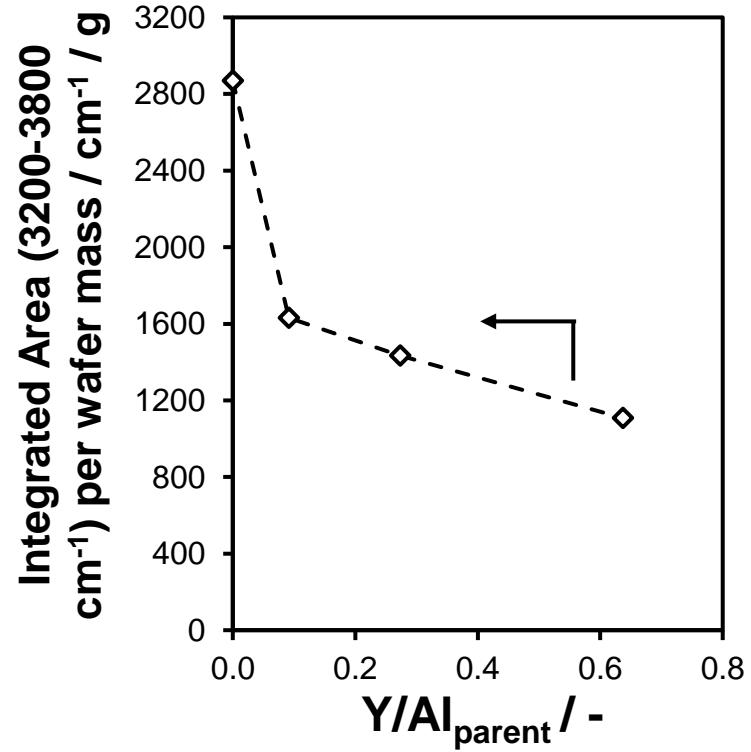
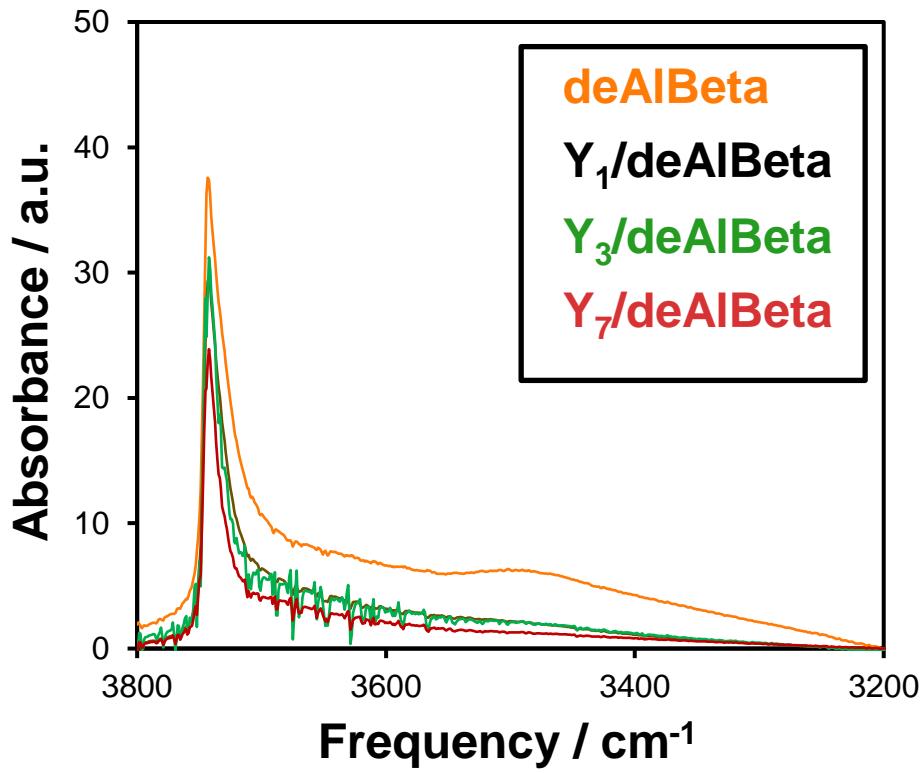


SSNMR of Y/deAlBeta Samples

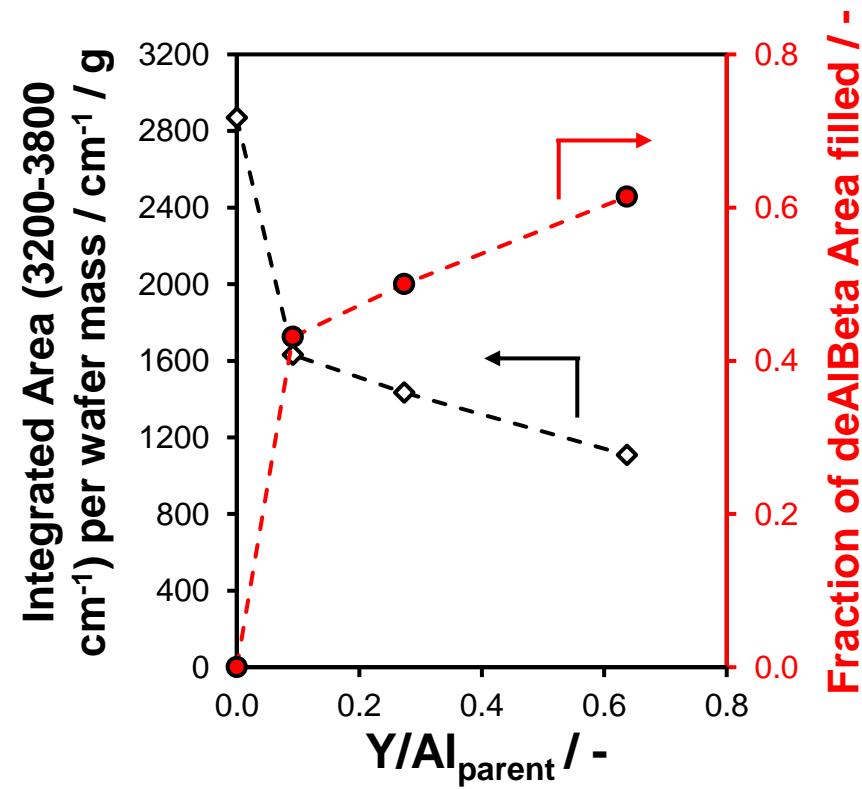
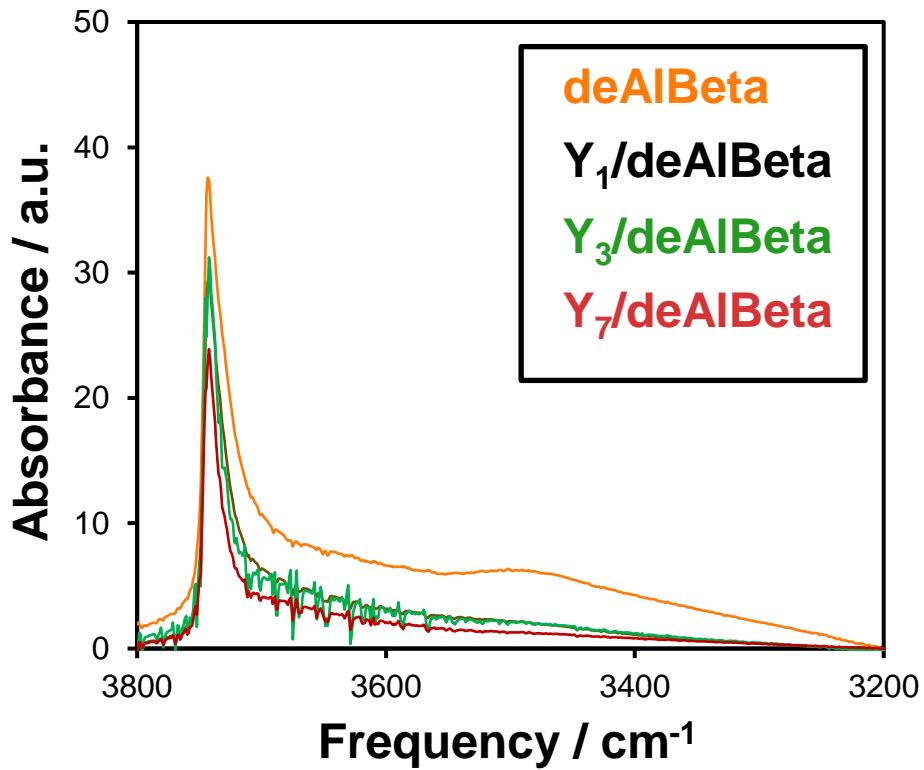


Hydroxyls generated by dealumination are largely eliminated by 0.5 wt% Y (0.05 Y/Al_{parent}), and completely by 10 wt% Y (0.9 Y/Al_{parent})

IR of Y/deAlBeta Samples – O-H region

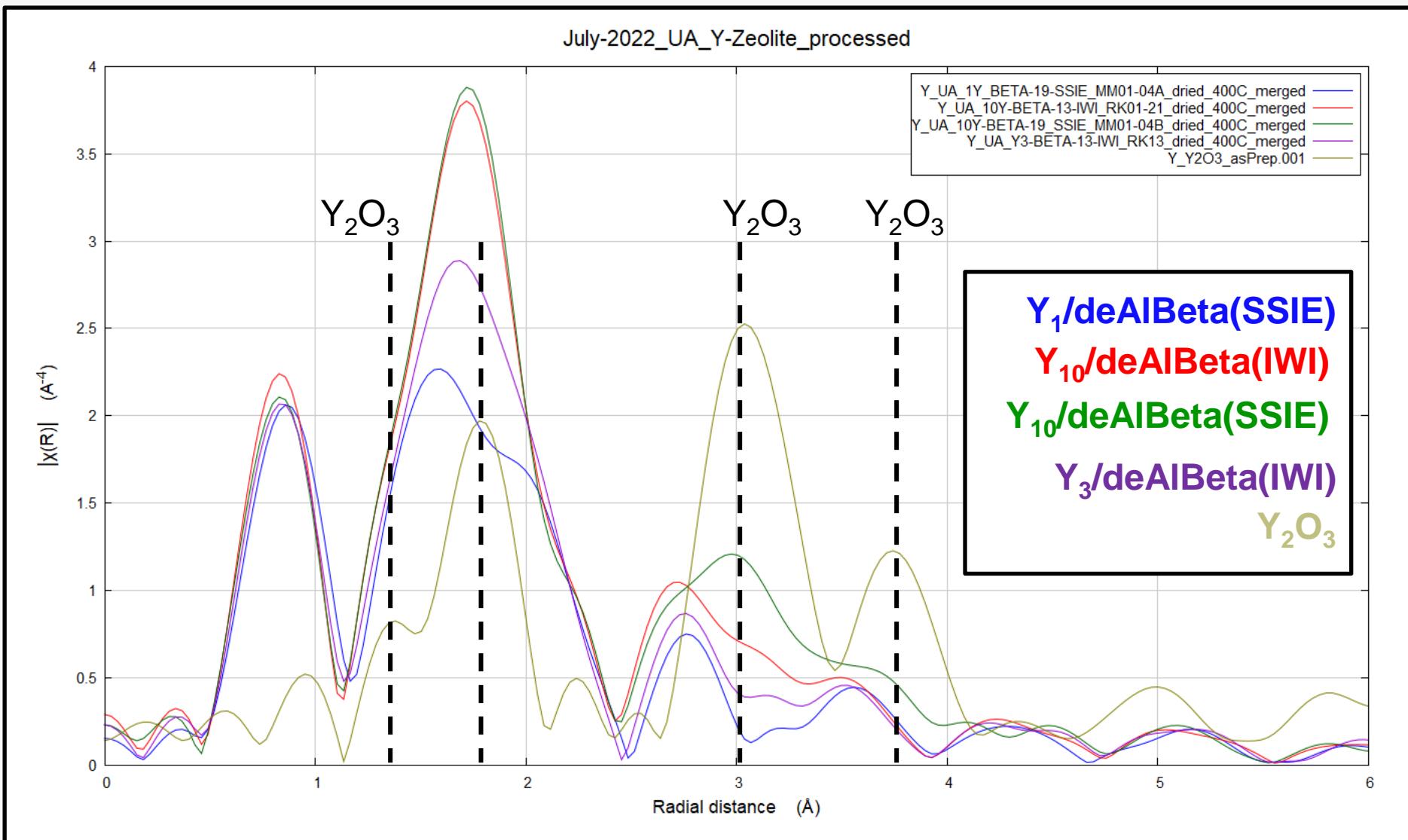


IR of Y/deAlBeta Samples – O-H region



Y incorporation by SSIE results in decreased $\nu(\text{O-H})$ region area, suggesting incorporation of Y at vacancies formed from dealumination

Y k-edge EXAFS of Y/deAlBeta samples



Above 1 wt%, all samples have some oxide-like peaks

Y k-edge EXAFS of Y/deAlBeta samples

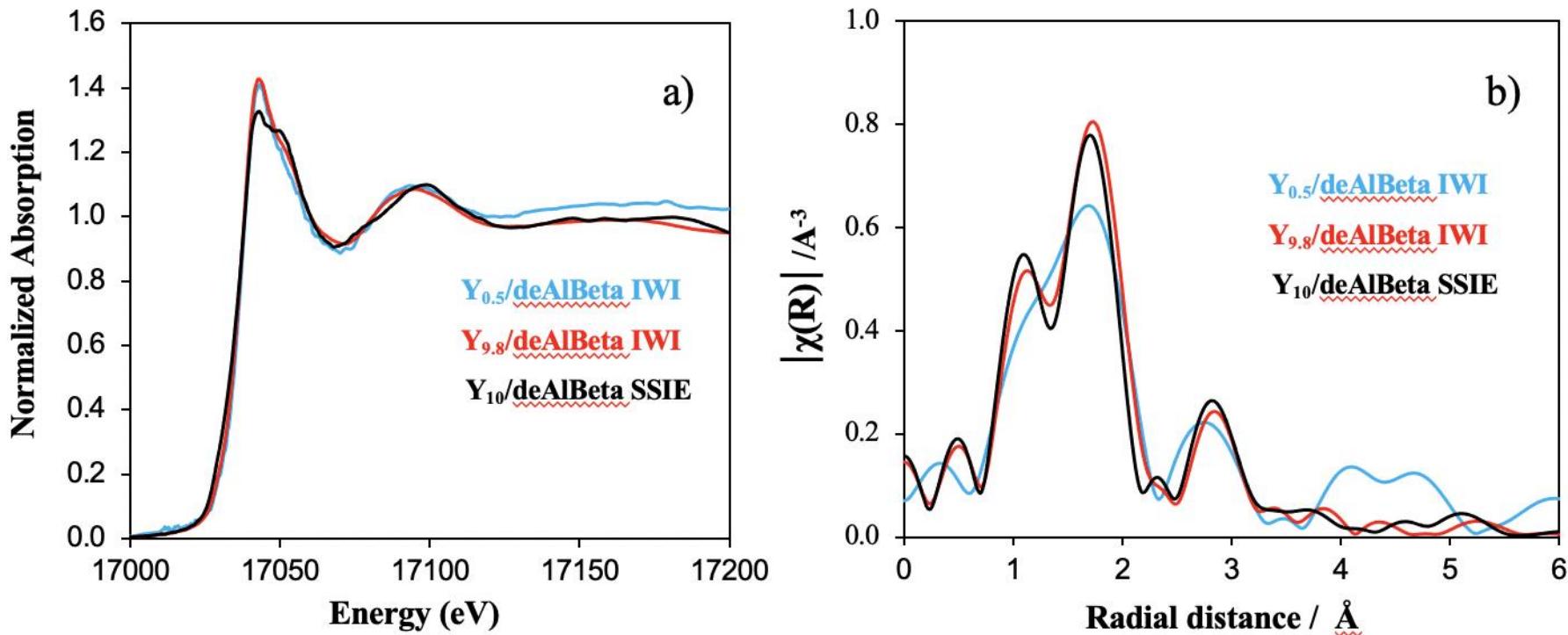
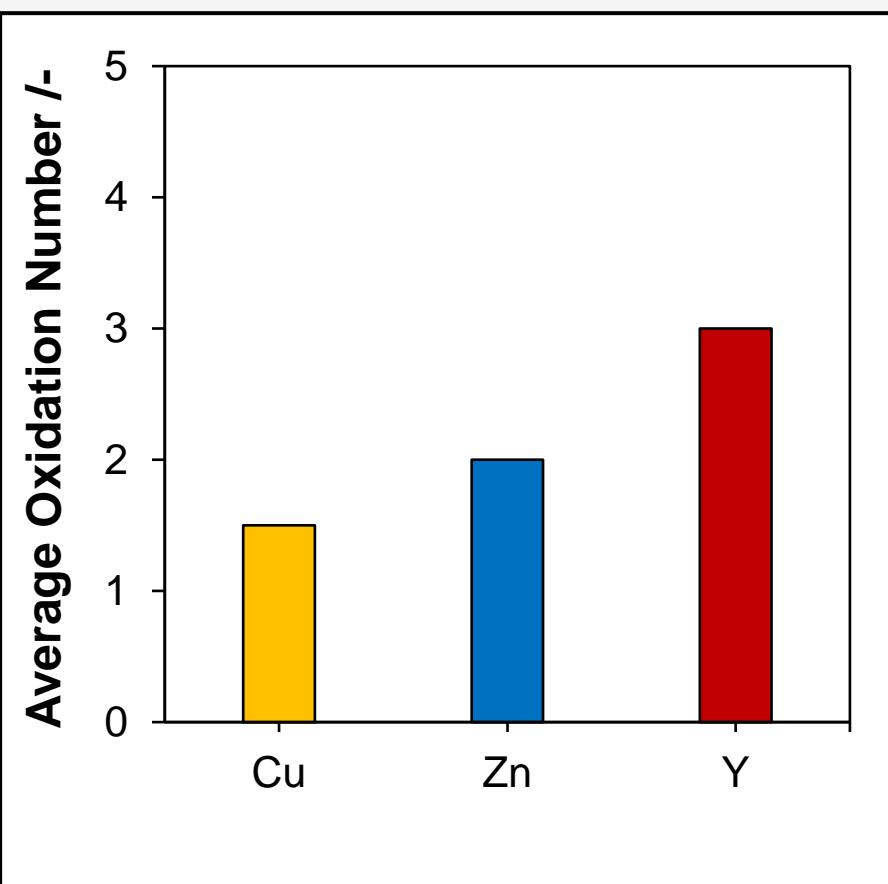


Figure 3 Y K edge XAS spectra of Y/deAlBeta of varied loading and synthesis techniques
(a) XANES spectra, (b) k²-Weighted FT EXAFS

Above 1 wt%, all samples have some oxide-like peaks

In-Situ Transmission X-ray Absorption Spectroscopy

XANES



Argonne National Laboratory
Advanced Photon Source (APS)

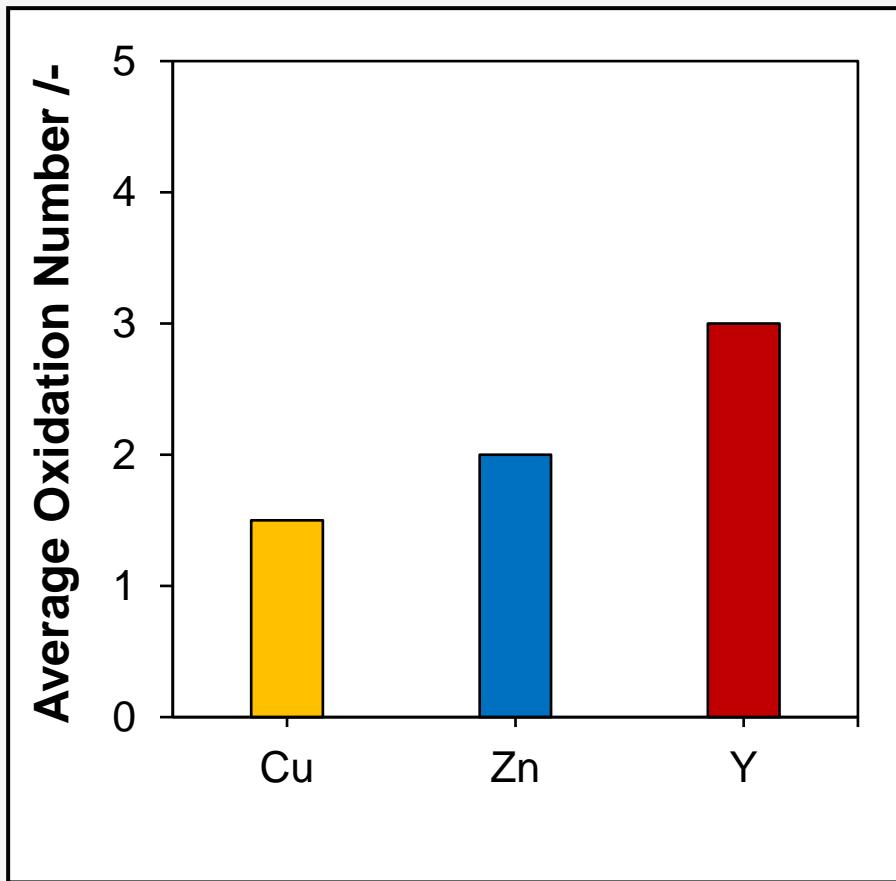


After treatment in flowing 3.5 kPa H₂, 98 kPa He, for 2 h at 673 K

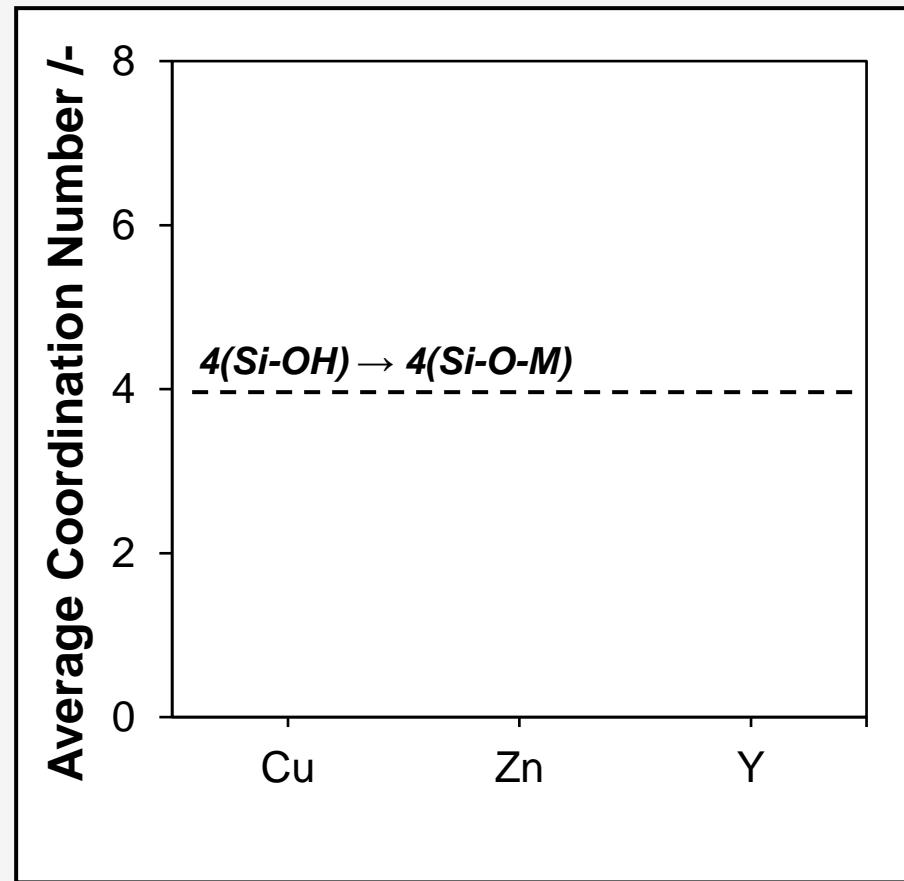
Zhang, Wegener, Samad et al., ACS Catal., 11 (2021) 9885-9897

In-Situ Transmission X-ray Absorption Spectroscopy

XANES



XAFS

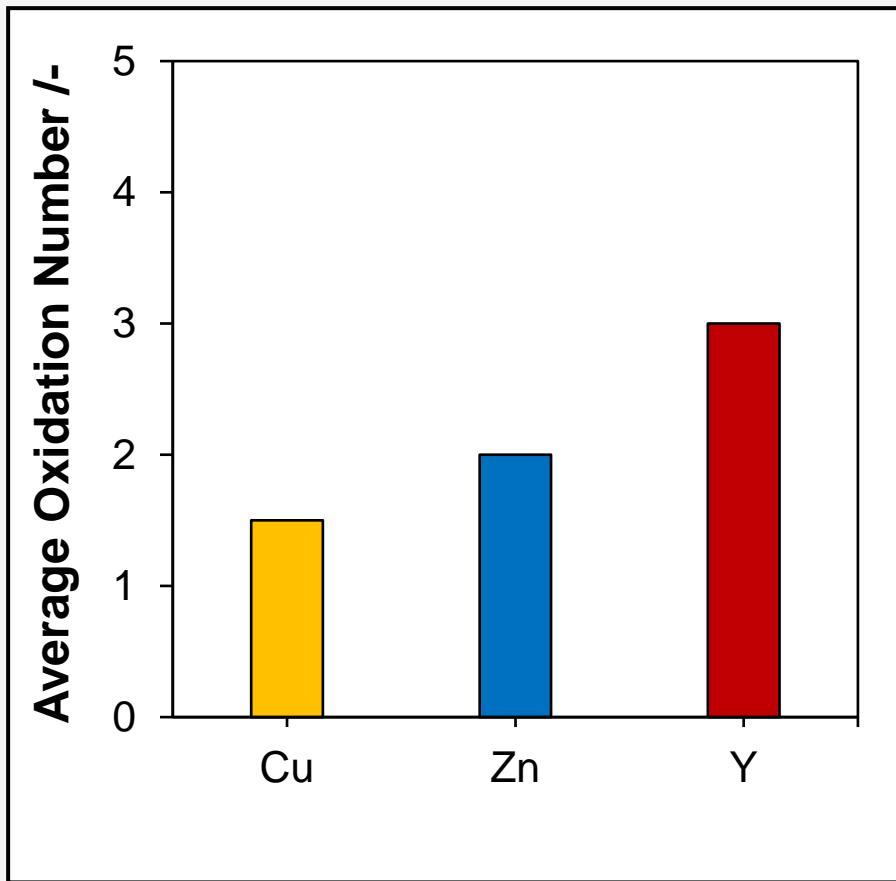


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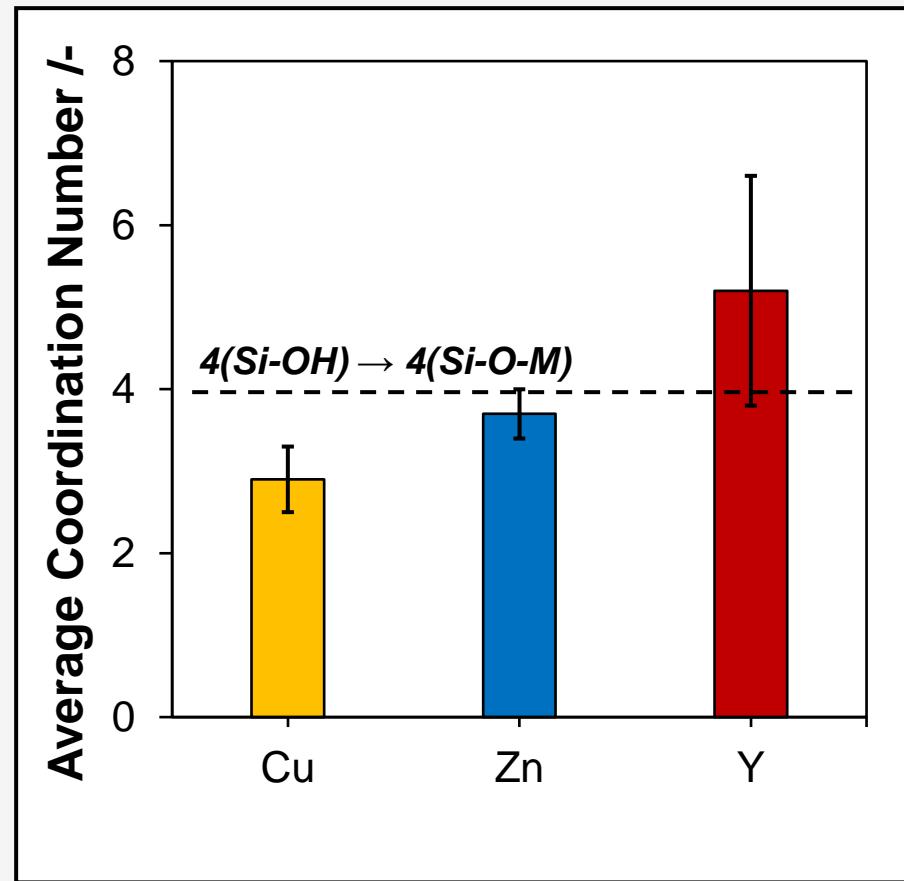
Zhang, Wegener, Samad et al., ACS Catal., 11 (2021) 9885-9897

In-Situ Transmission X-ray Absorption Spectroscopy

XANES



XAFS

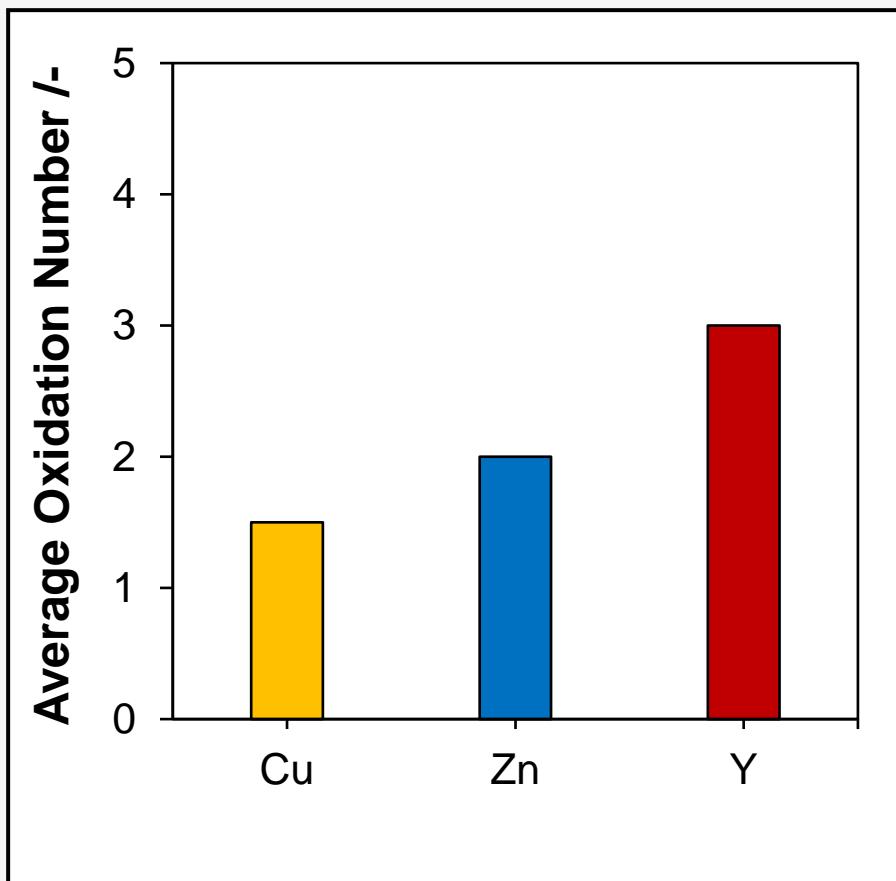


After treatment in flowing 3.5 kPa H₂, 98 kPa He, for 2 h at 673 K

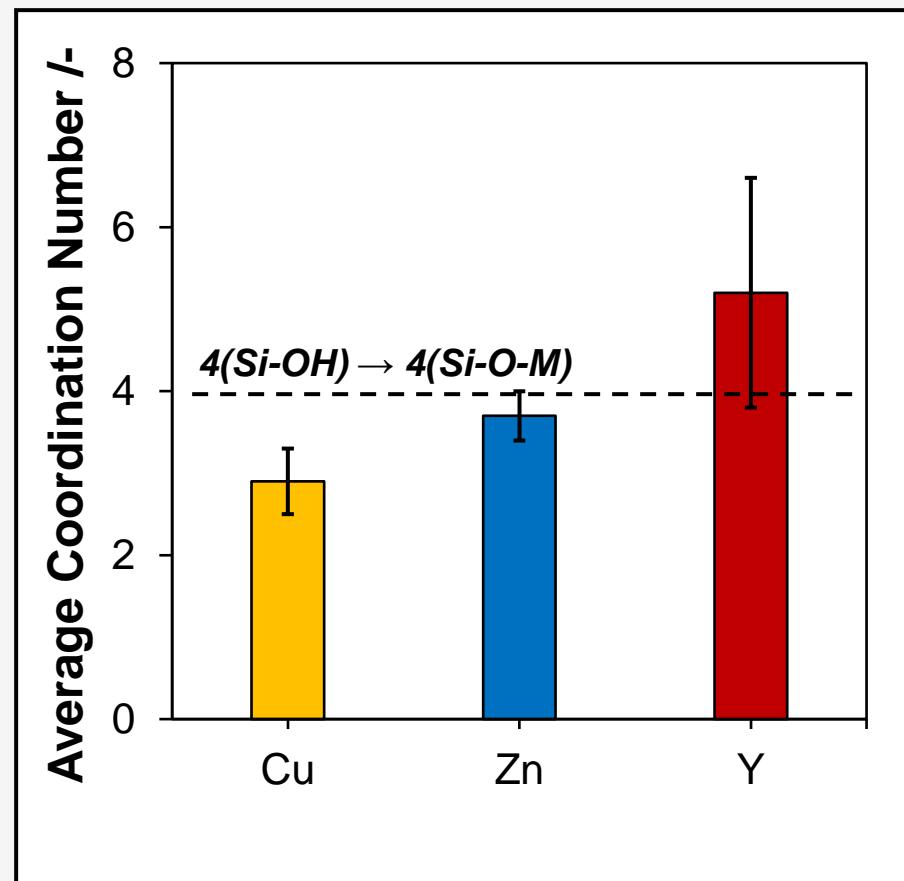
Zhang, Wegener, Samad et al., ACS Catal., 11 (2021) 9885-9897

In-Situ Transmission X-ray Absorption Spectroscopy

XANES



XAFS

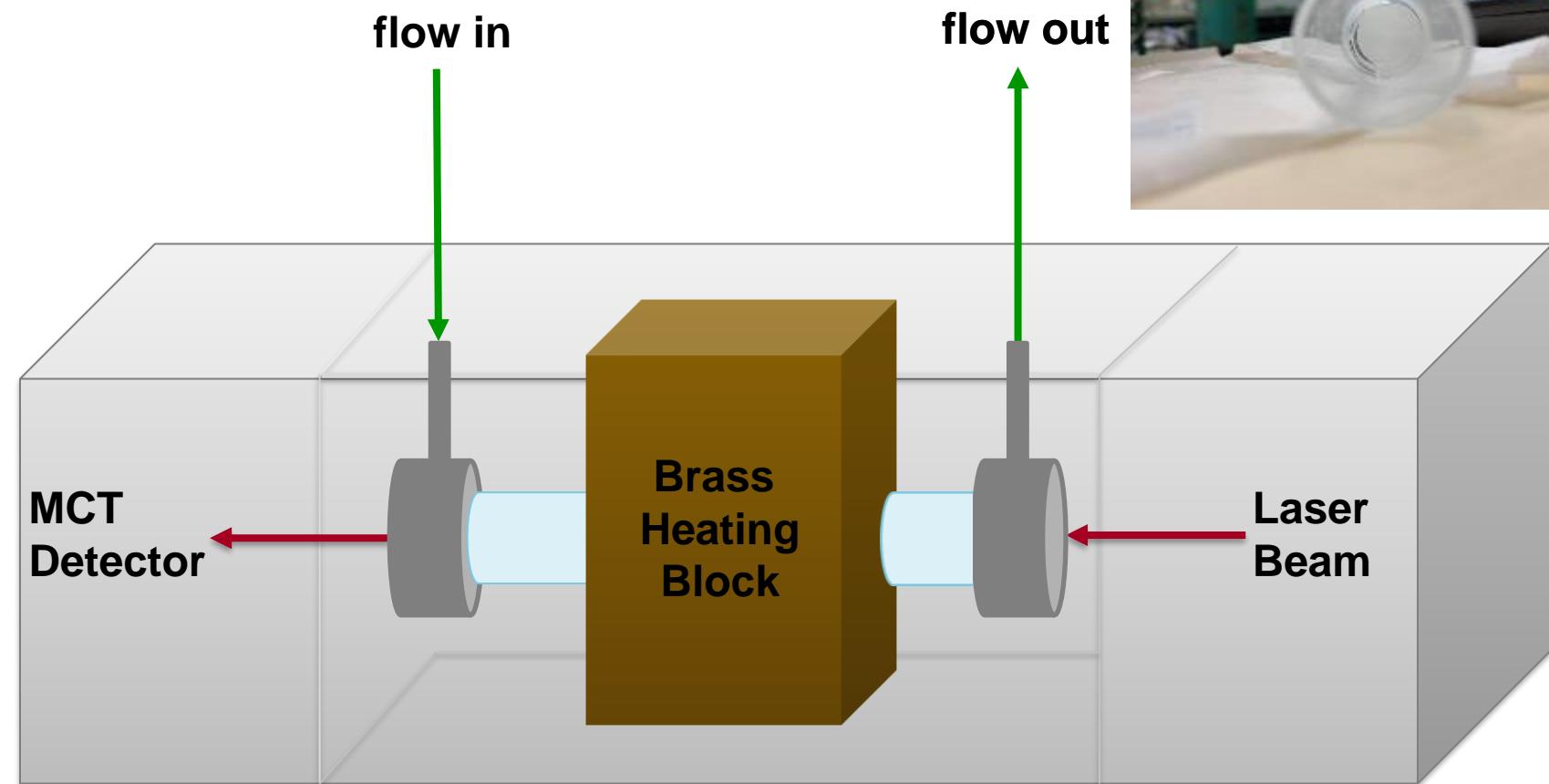


- Mixture of Y_2O_3 oligomers isolated Y sites?
- No Y_xO_y observed by HRTEM or XRD

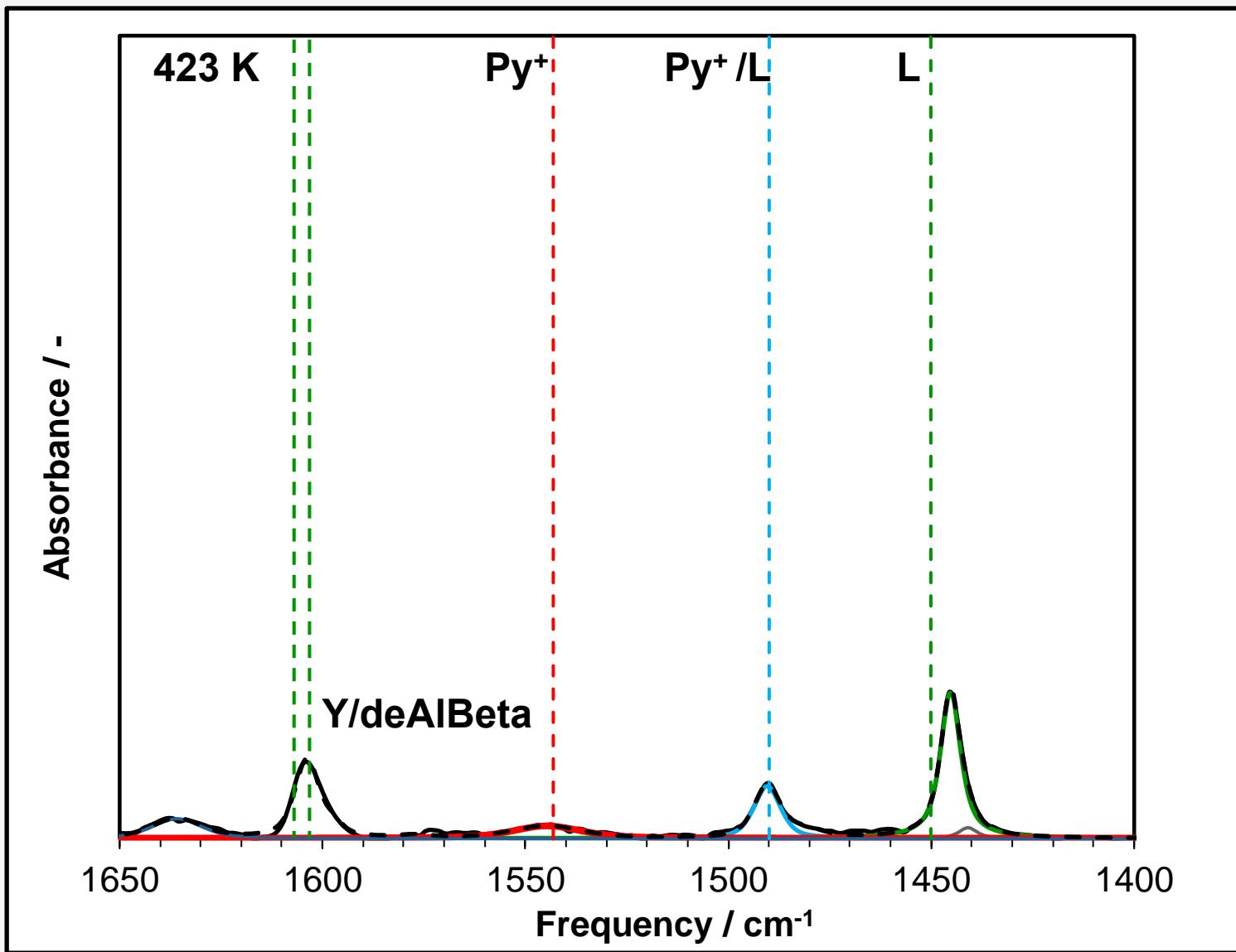
After treatment in flowing 3.5 kPa H_2 , 98 kPa He, for 2 h at 673 K

Zhang, Wegener, Samad et al., ACS Catal., 11 (2021) 9885-9897

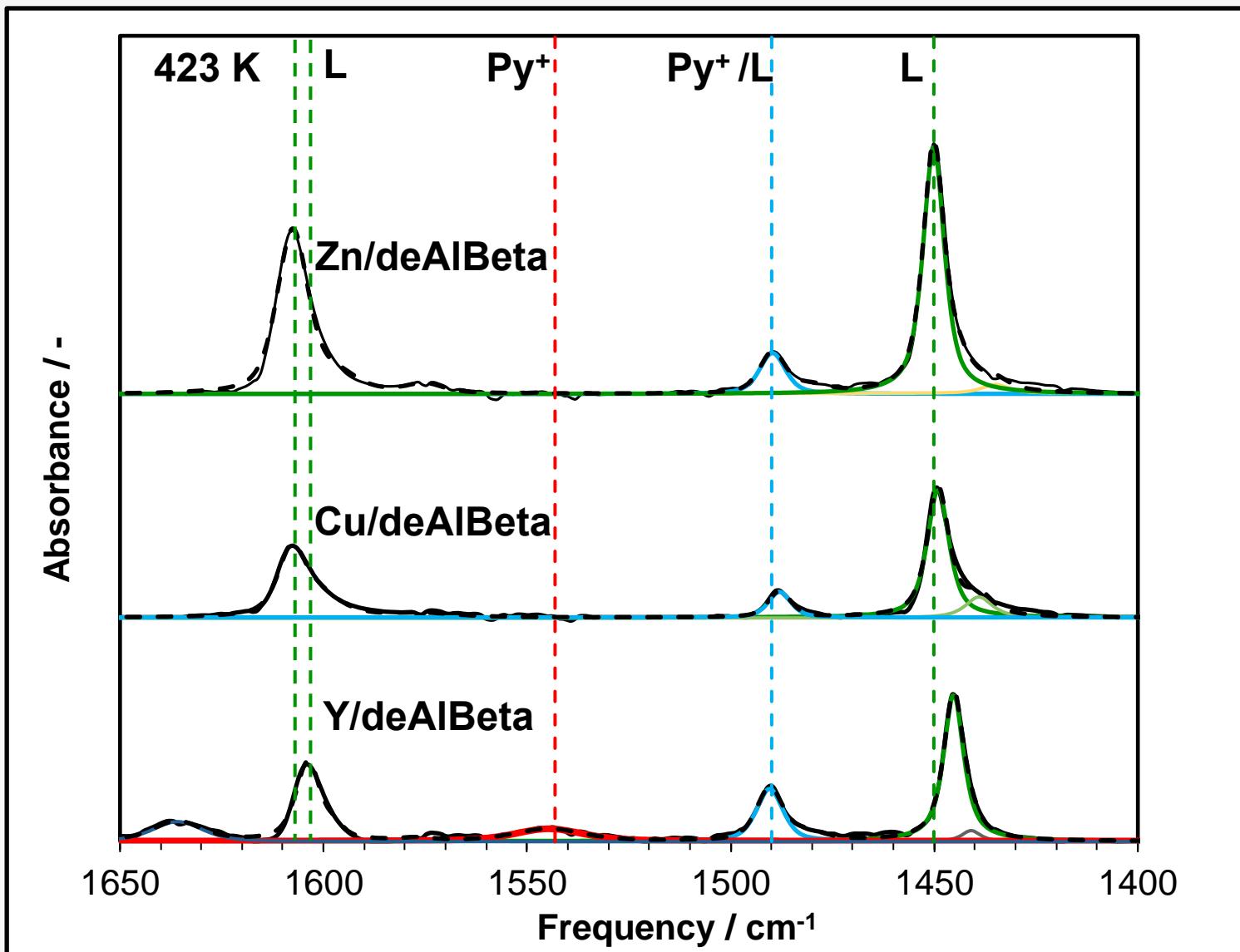
Fourier Transformed Infrared Spectroscopy



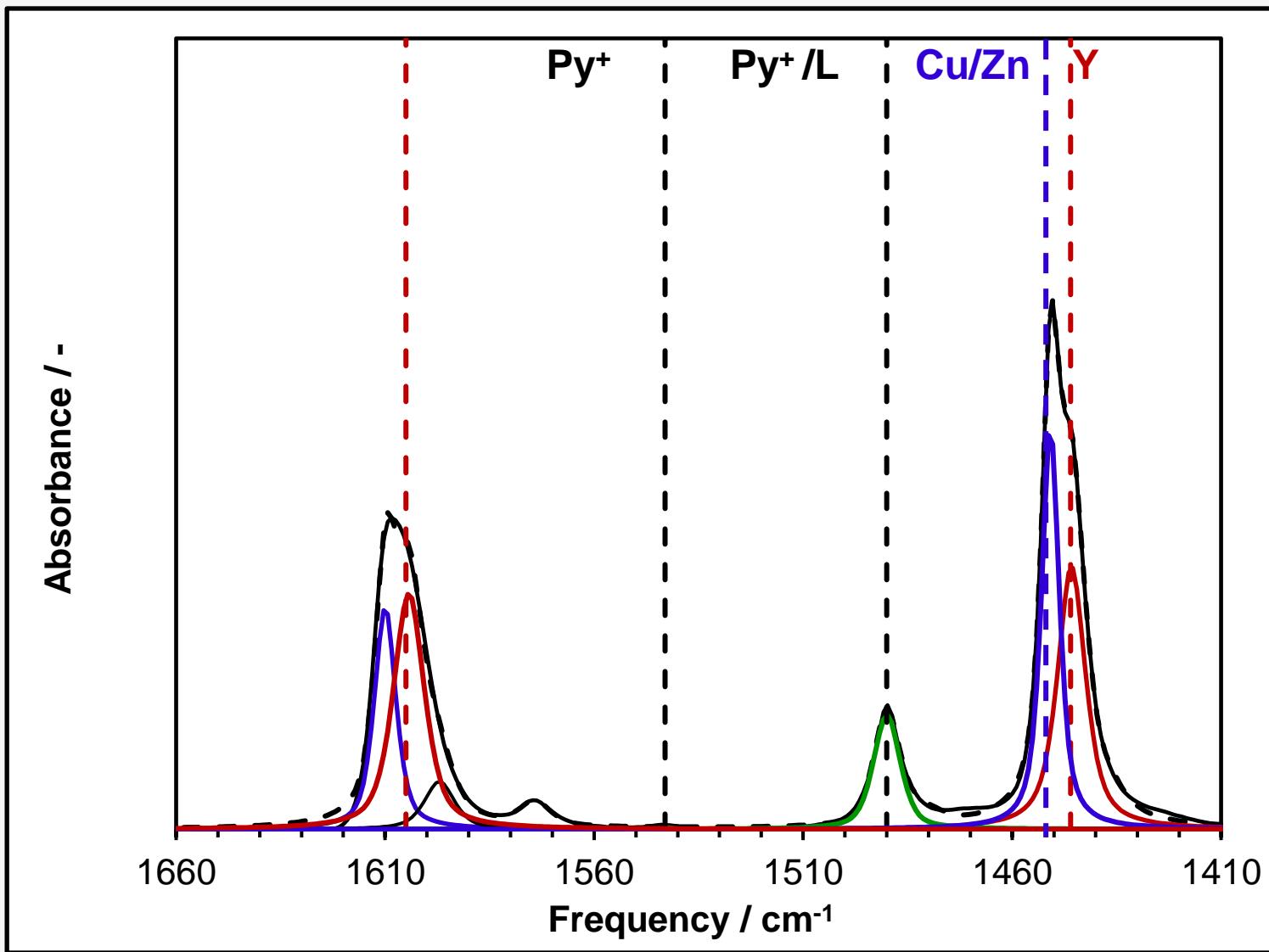
Pyridine IR: M/deAlBeta



Pyridine IR: M/deAlBeta

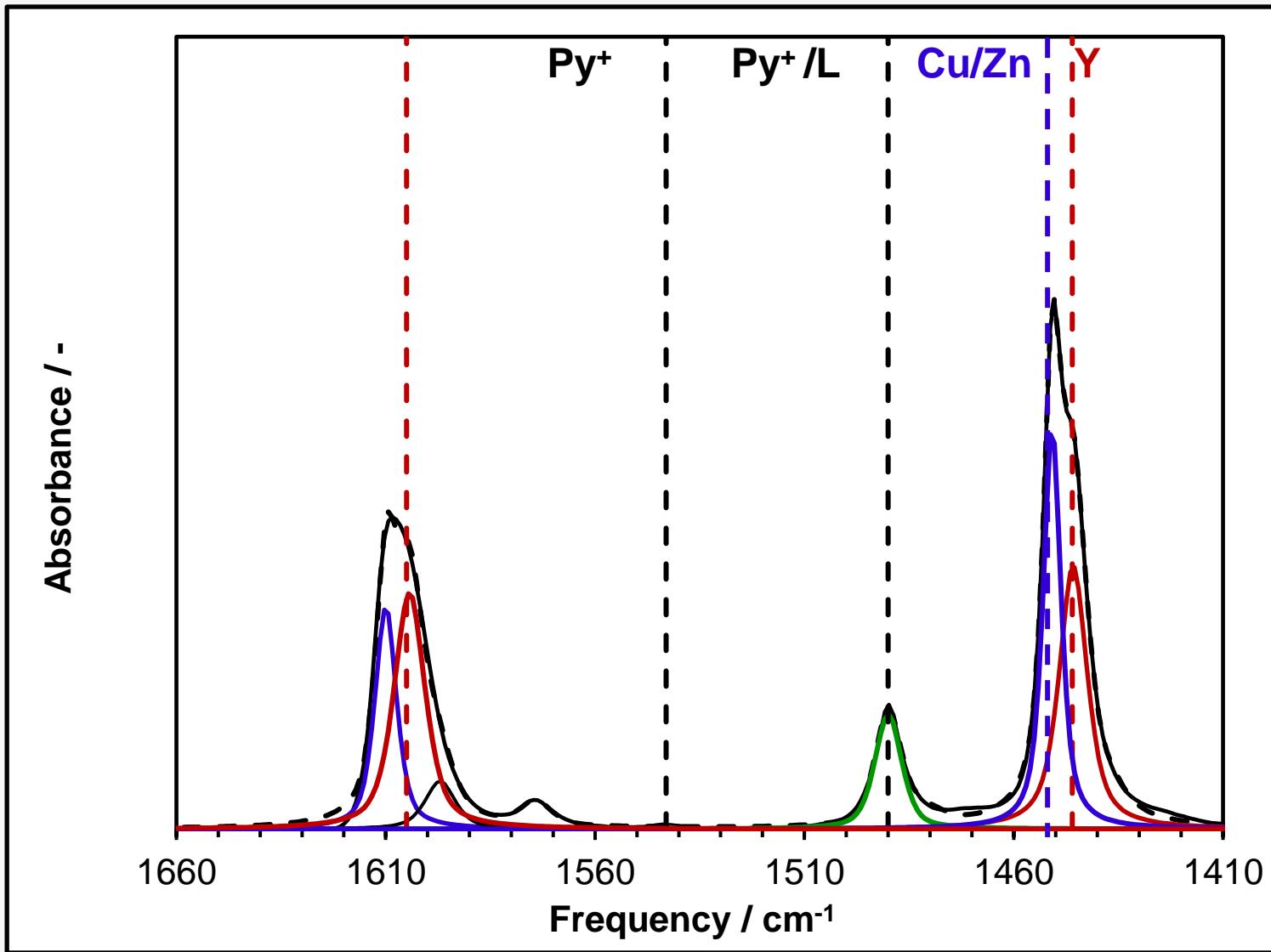


Pyridine IR: CuZn Y/deAlBeta



Can distinguish Y LAS sites from Cu & Zn LAS sites...

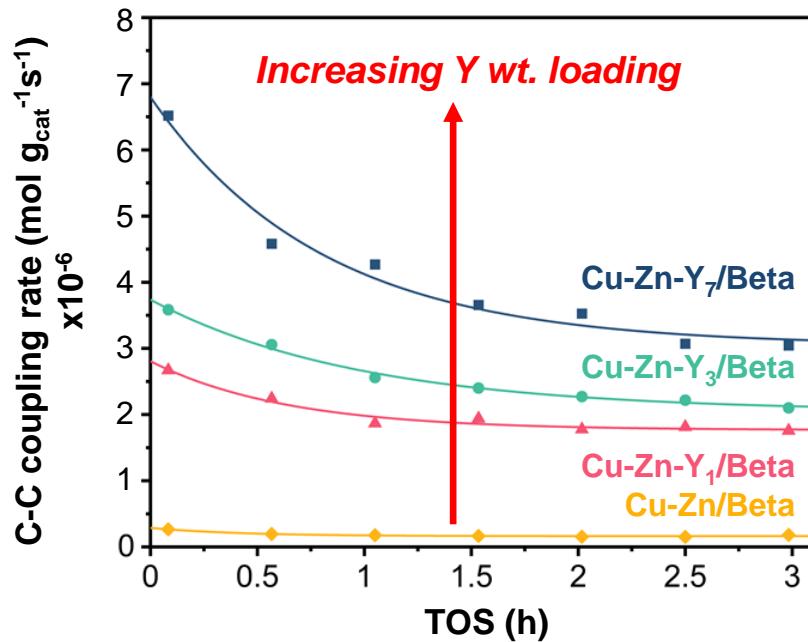
Pyridine IR: CuZn Y/deAlBeta



*Can distinguish Y LAS sites from Cu & Zn LAS sites... and
Py⁺ no longer present in CuZnY/Beta*

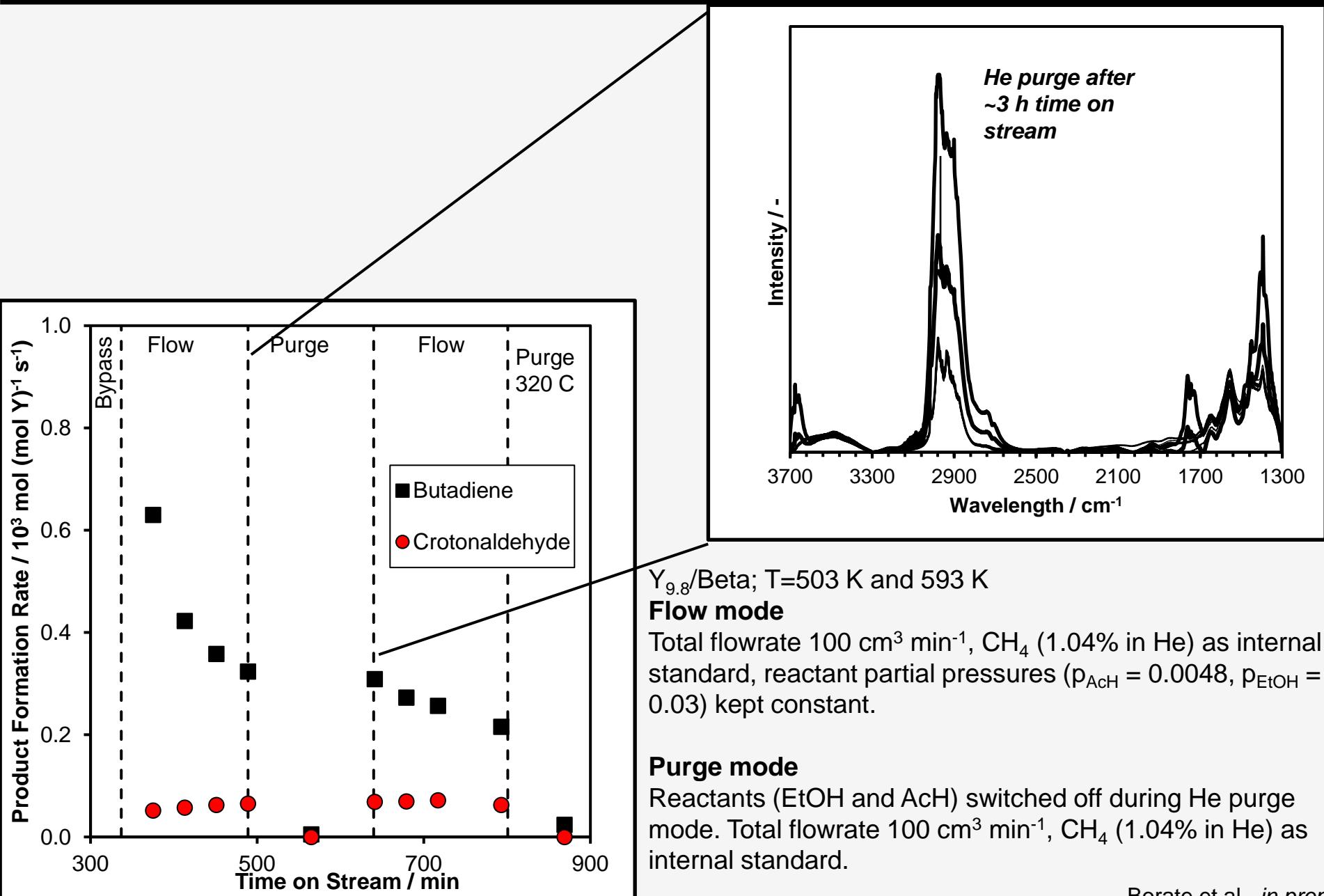
Measurement of product formation rates on CuZnY/deAlBeta

$$r_{C-C \text{ coupling}} = \frac{(r_{\text{butenes}} + r_{\text{butadiene}} + r_{\text{C4aldehydes}} + 2 \times r_{\text{hexenes}} + 3 \times r_{\text{octenes}})}{m_c}$$



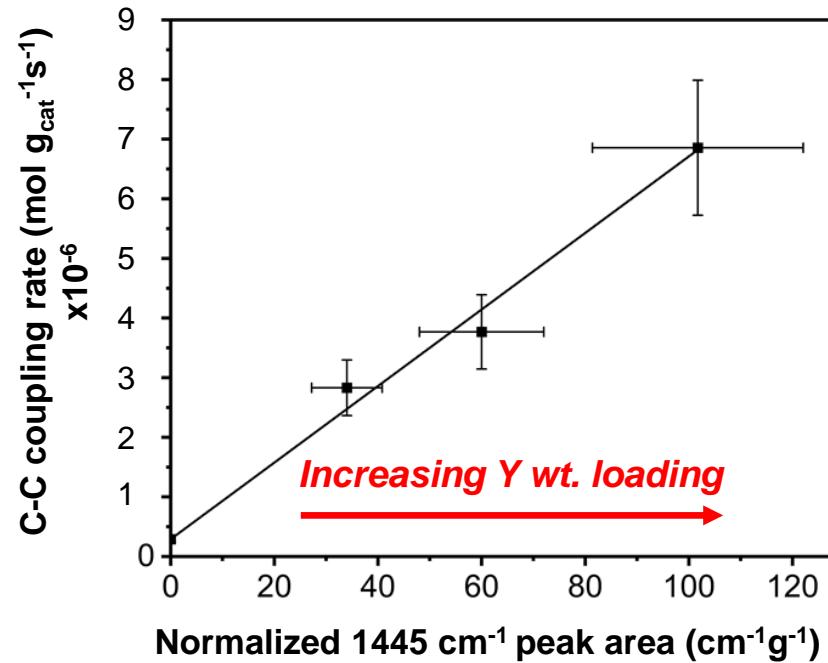
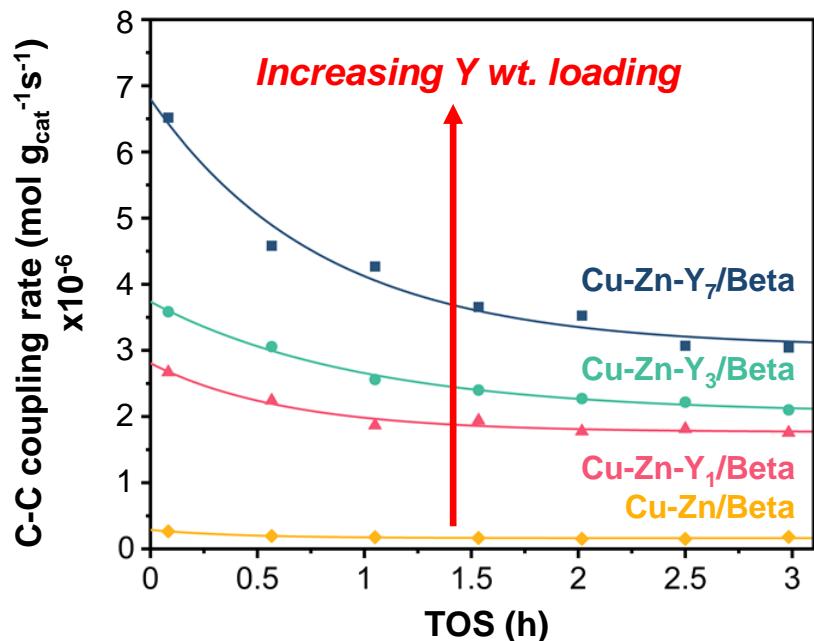
*Data Collected by Junyan Zhang, ORNL

Flow experiment on Y_{9.8}%/Beta in IR cell



Measurement of product formation rates on CuZnY/deAlBeta

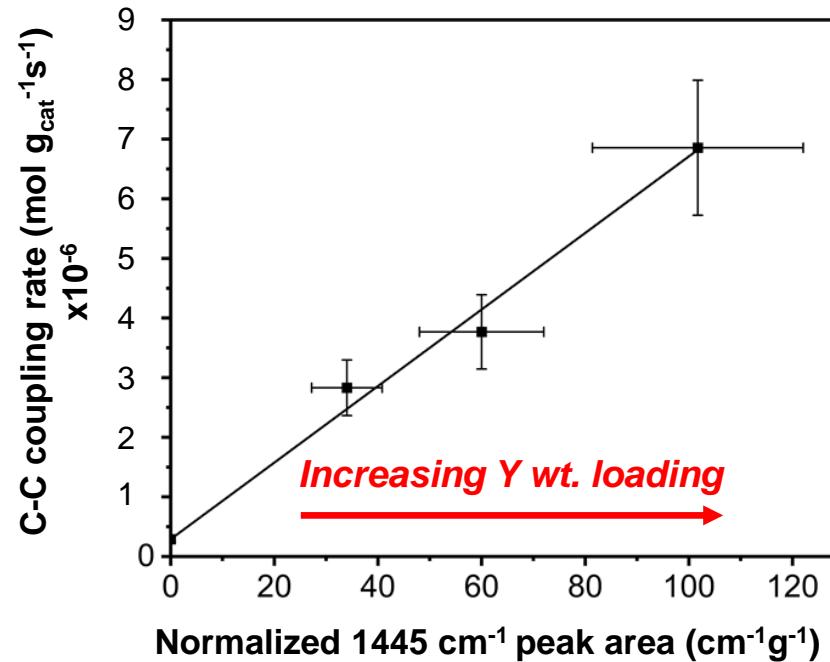
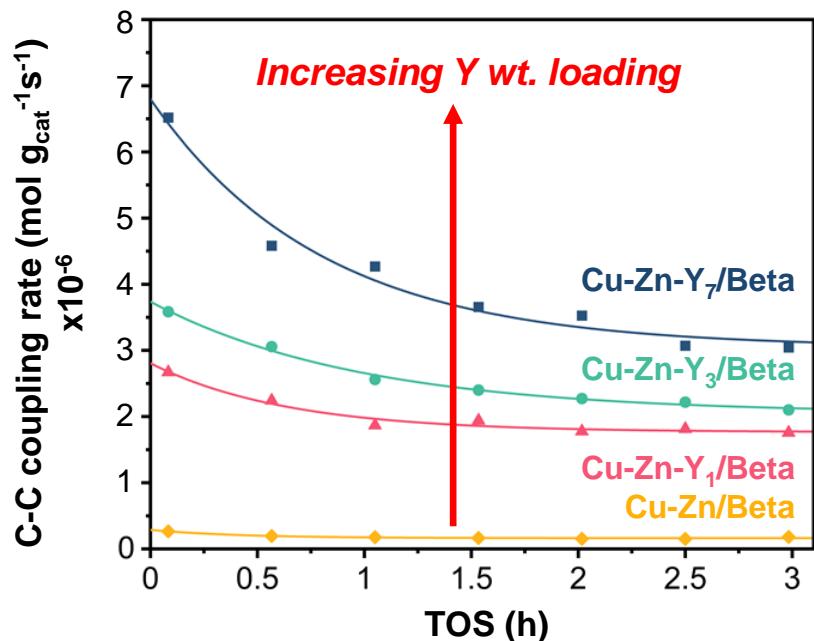
$$r_{C-C \text{ coupling}} = \frac{(r_{\text{butenes}} + r_{\text{butadiene}} + r_{\text{C4aldehydes}} + 2 \times r_{\text{hexenes}} + 3 \times r_{\text{octenes}})}{m_c}$$



*Data Collected by Junyan Zhang, ORNL

Measurement of product formation rates on CuZnY/deAlBeta

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*Data Collected by Junyan Zhang, ORNL

C-C coupling rates correlate linearly with Y_{LAS} density measured by pyridine IR

Quantification of IMECS to Enable Quantitative Chemisorption IR

Beer-Lambert law

$$A = \epsilon b C$$

A = absorbance

ϵ = molar extinction coefficient

b = path length

C = concentration

Quantification of IMECS to Enable Quantitative Chemisorption IR

Beer-Lambert law

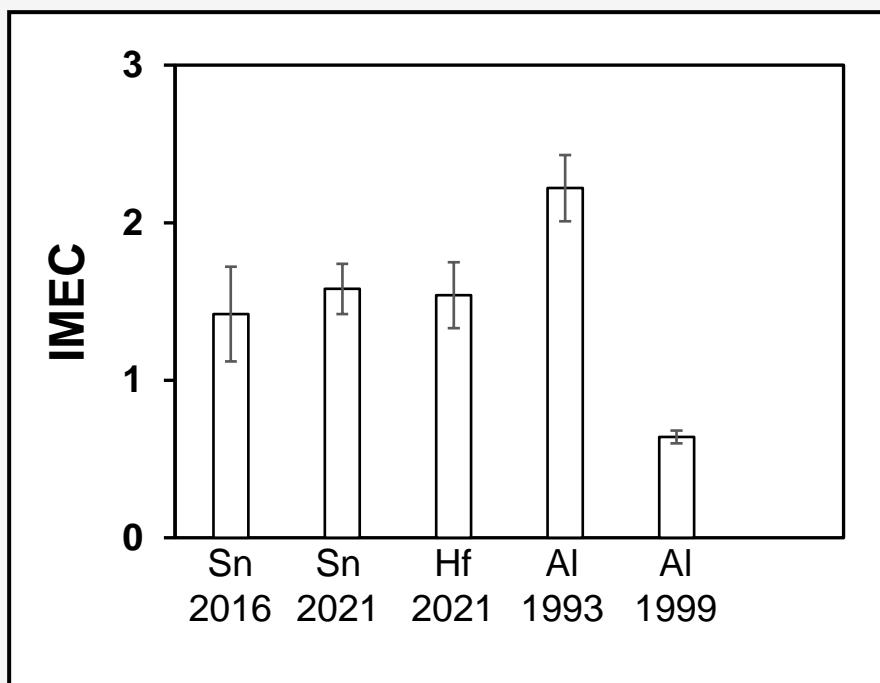
$$A = \epsilon b C$$

A = absorbance

ϵ = molar extinction coefficient

b = path length

C = concentration



- C. A. Emeis., *J Catal.*, 141 (1993) 347-354
Sell and Forni, *Micropor. Mesopor. Mat.*, 31 (1999) 129 - 140
Harris et al., *J Catal.*, 335 (2016) 141-154
Johnson et al., *J. Catal.*, 404 (2021) 607-619

Quantification of IMECS to Enable Quantitative Chemisorption IR

Beer-Lambert law

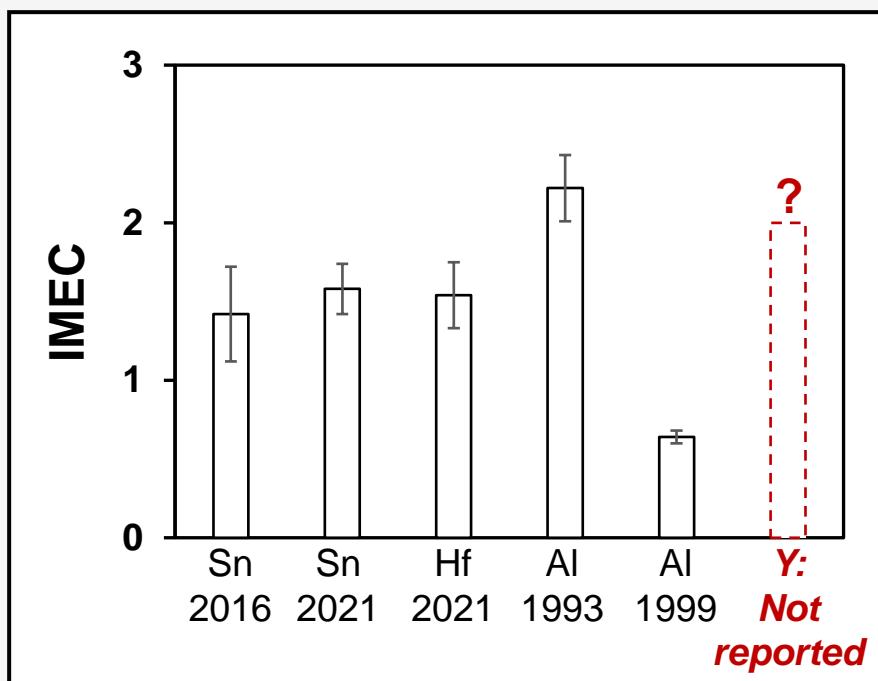
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Quantification of IMECS to Enable Quantitative Chemisorption IR

Beer-Lambert law

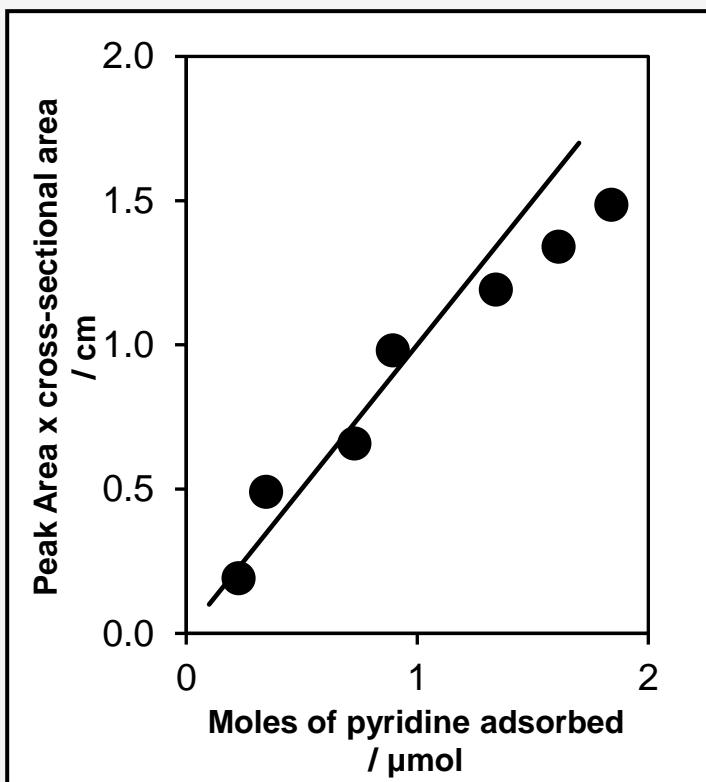
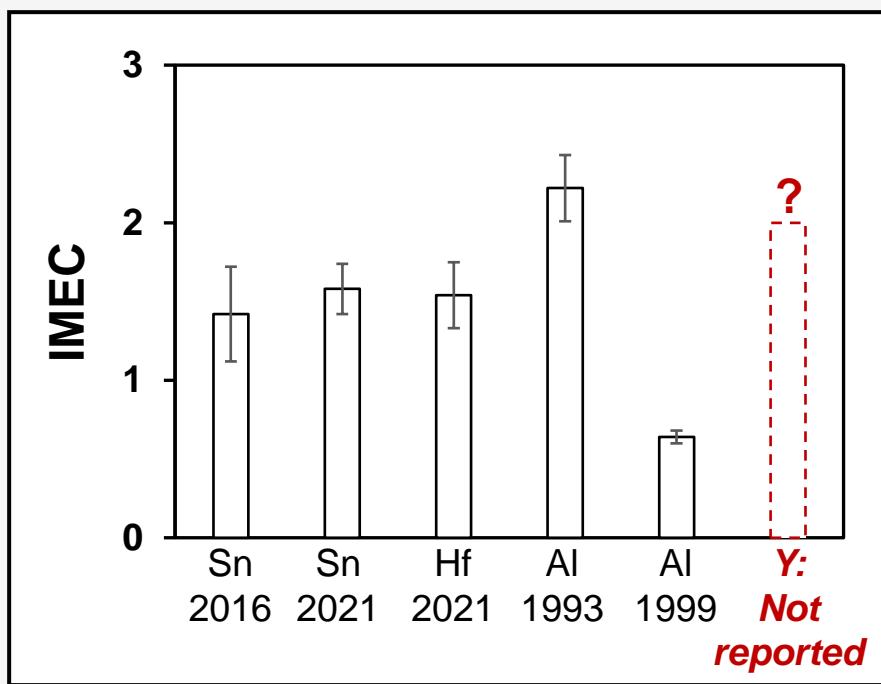
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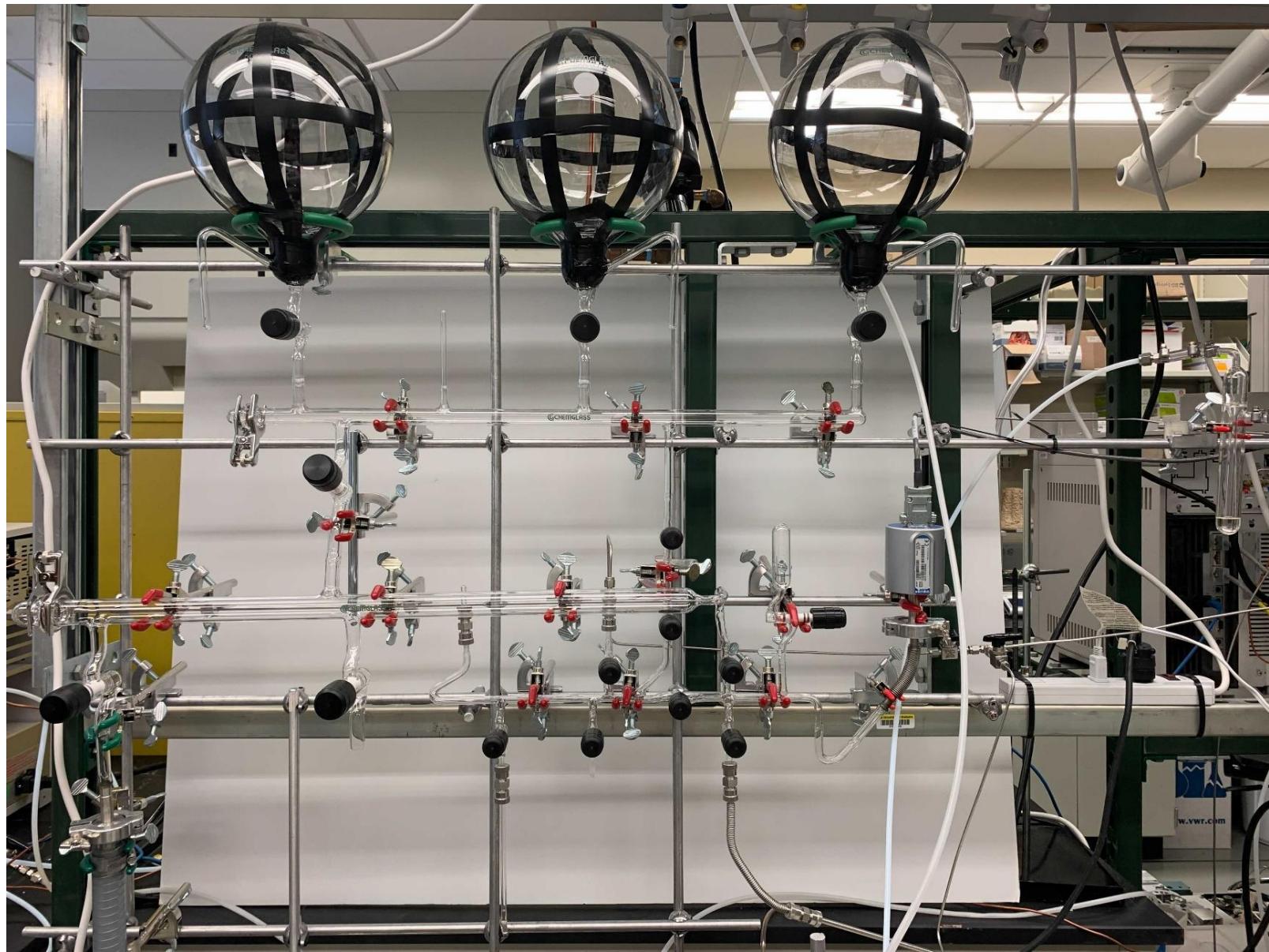
b = path length

C = concentration

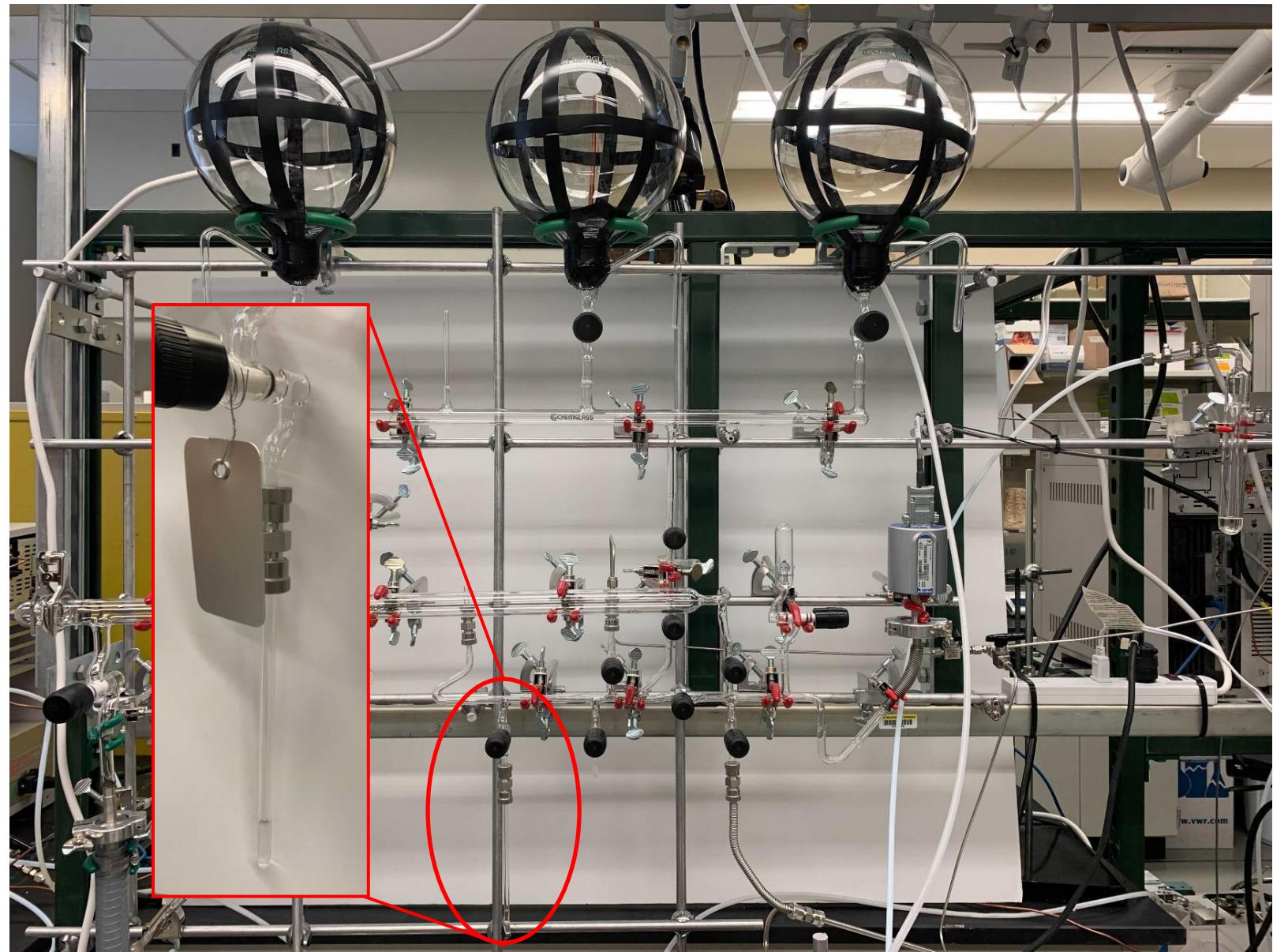


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Custom Glass Vacuum Manifold

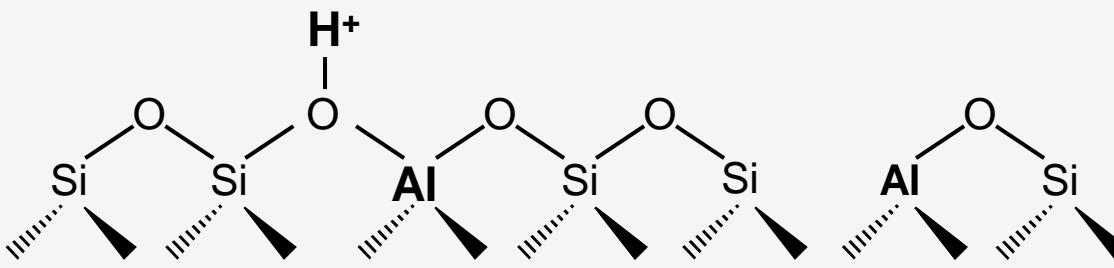
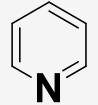


Custom Glass Vacuum Manifold

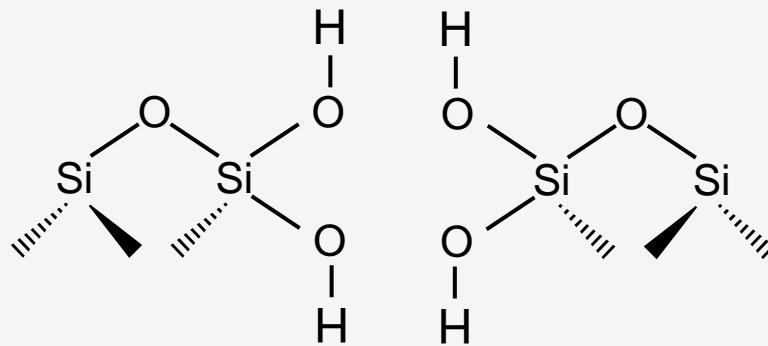


Pyridine Adsorption on Dealuminated Beta

423 K
10 – 40 torr



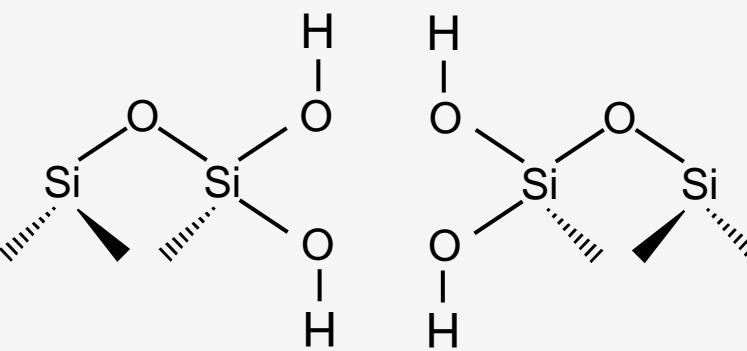
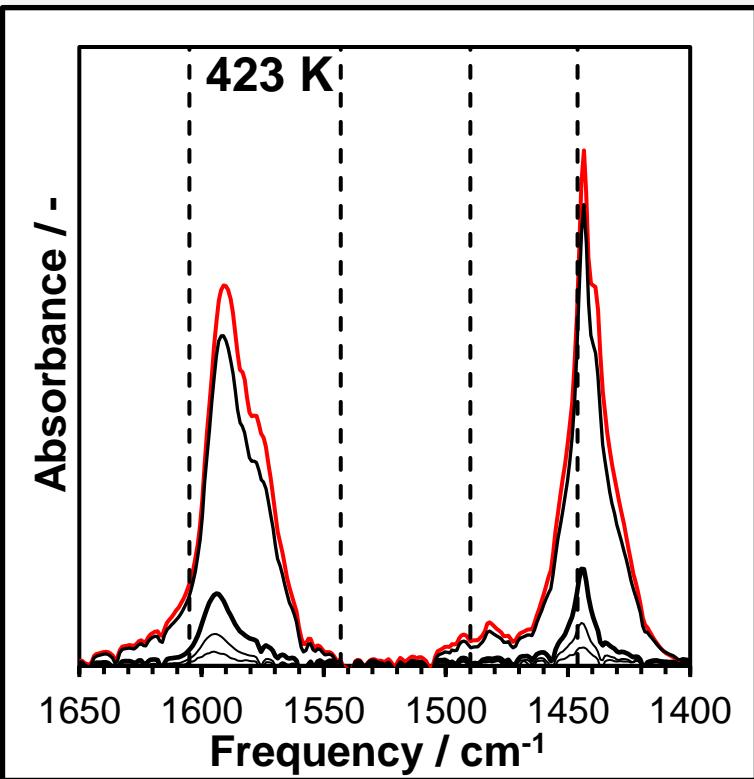
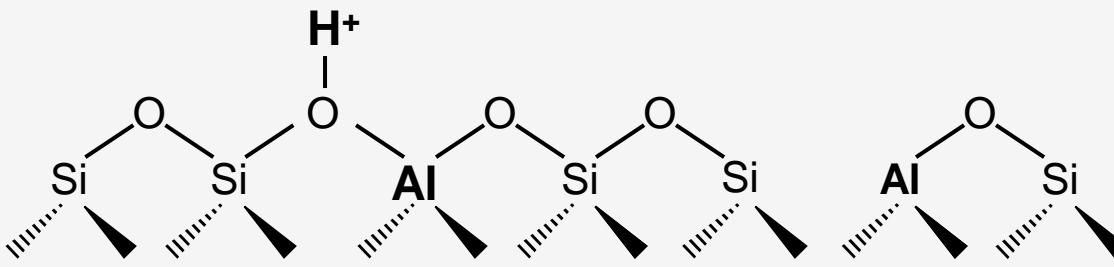
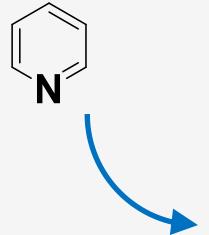
H-Beta



Dealuminated
Beta

Pyridine Adsorption on Dealuminated Beta

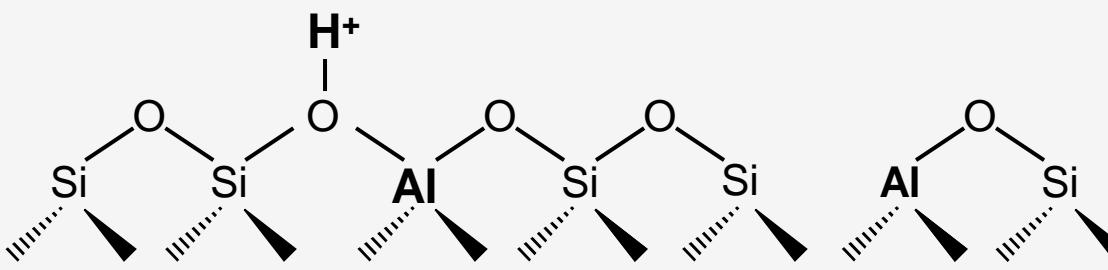
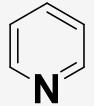
423 K
10 – 40 torr



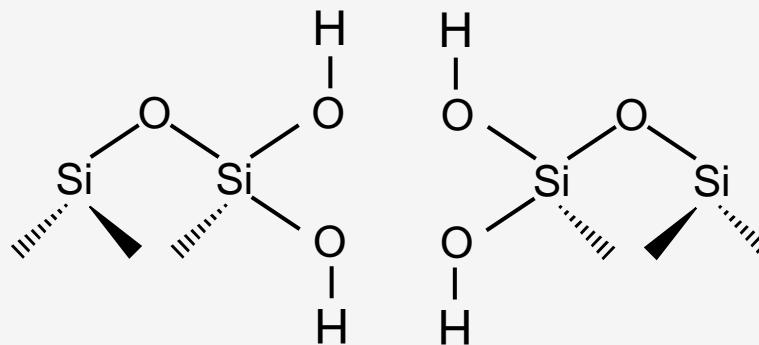
- Red = pyridine flow
- Black = He purge

Pyridine Titration of Lewis Acid Sites

423 K
10 – 40 torr



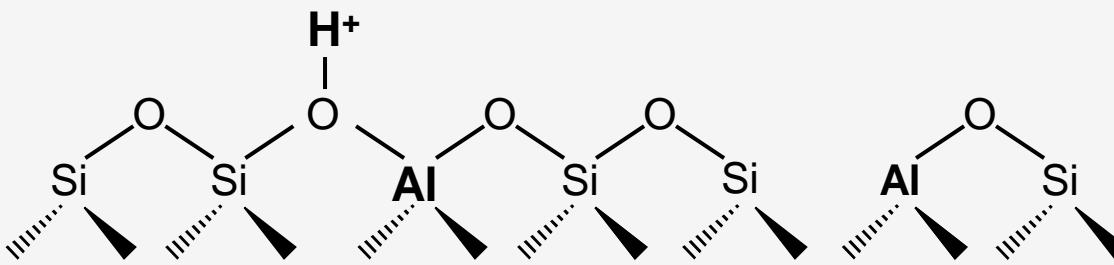
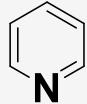
H-Beta



Dealuminated
Beta

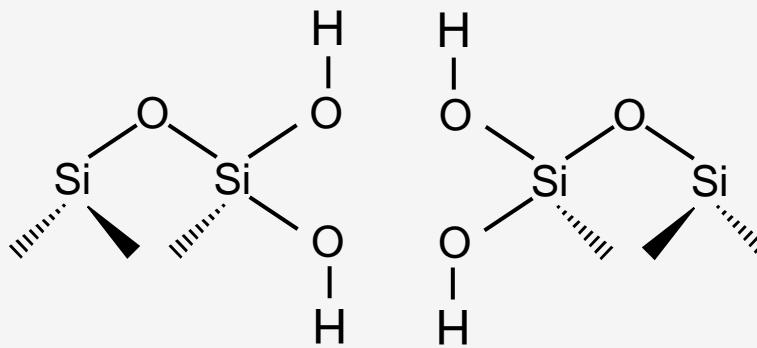
Pyridine Titration of Lewis Acid Sites

423 K
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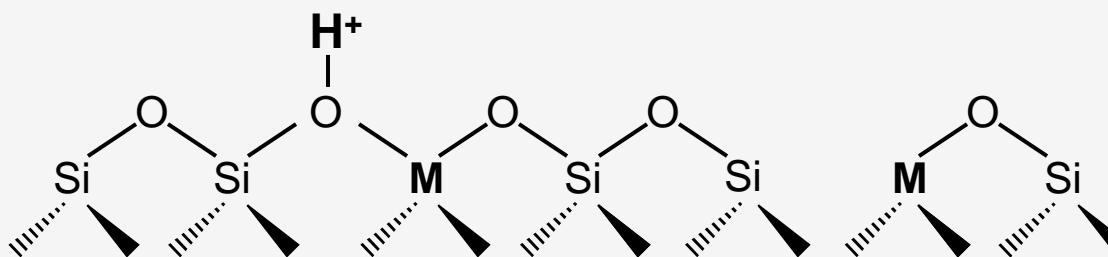


H-Beta

**We would expect
Y-containing
zeolites to have
charge balancing
protons (akin to
aluminosilicate
zeolites)**



Dealuminated
Beta



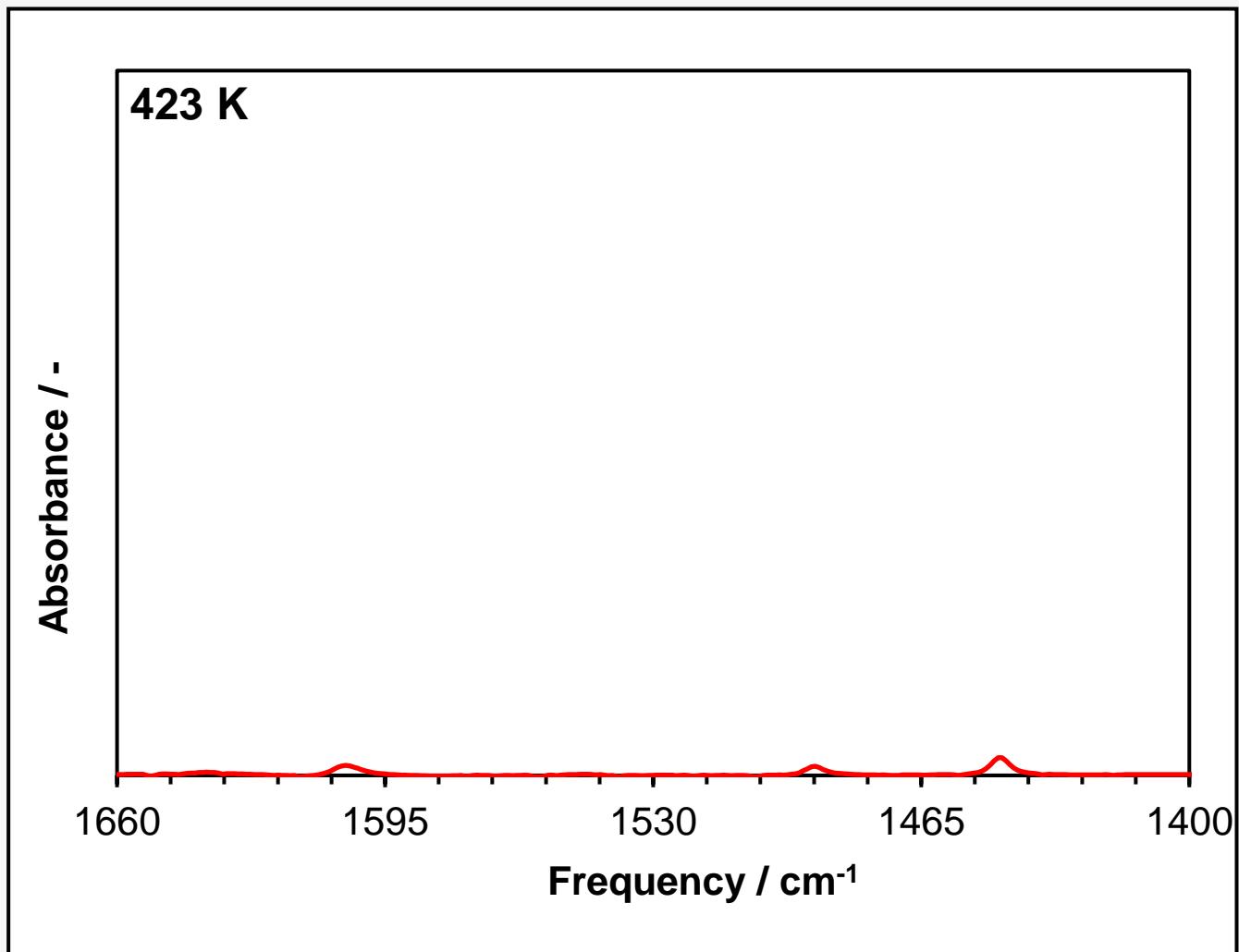
M Beta

Pyridine Titration on Y/deAlBeta Under Vacuum

Step 1: Dose

Step 2: Saturate

Step 3: Evacuate

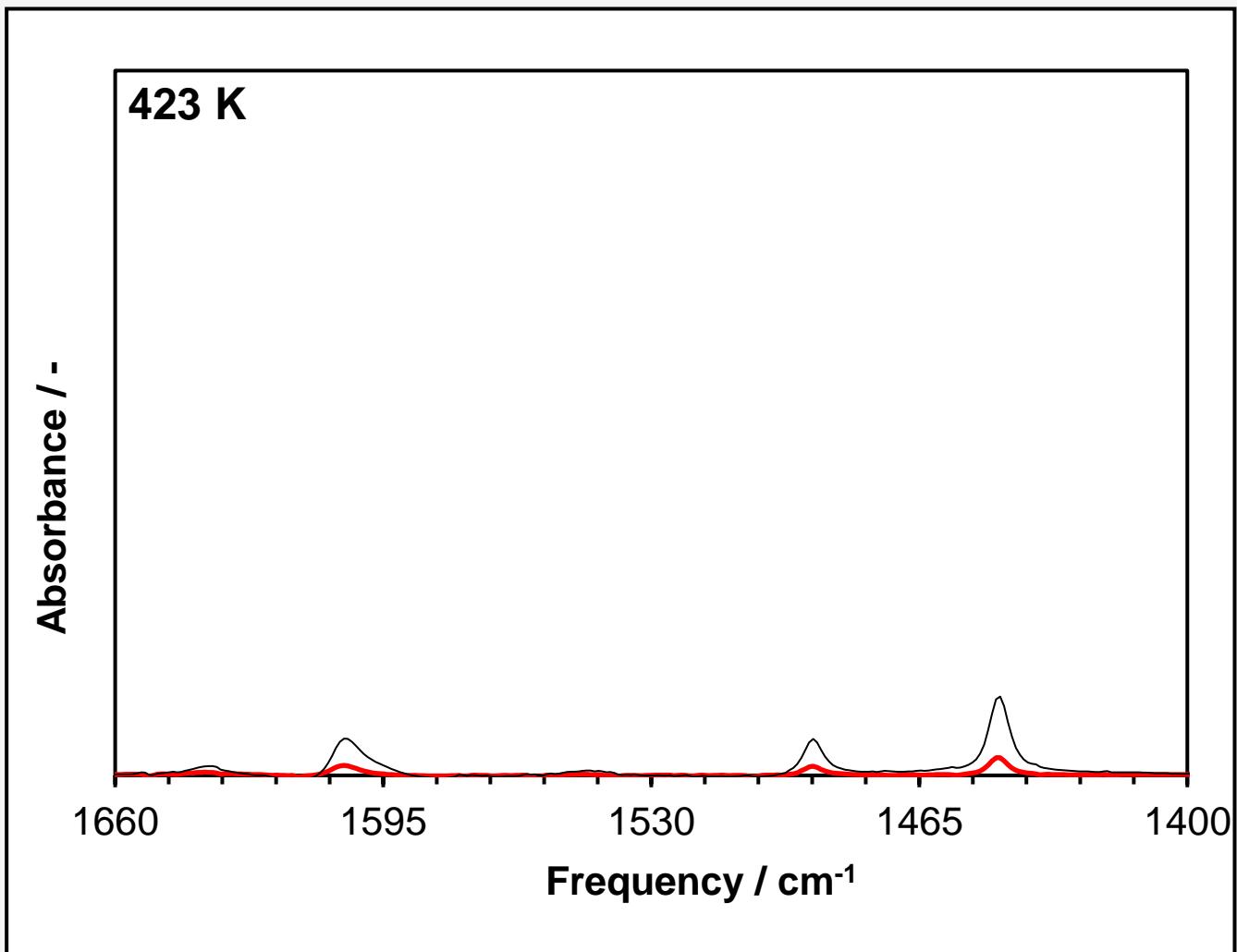


Pyridine Titration on Y/deAlBeta Under Vacuum

Step 1: Dose

Step 2: Saturate

Step 3: Evacuate

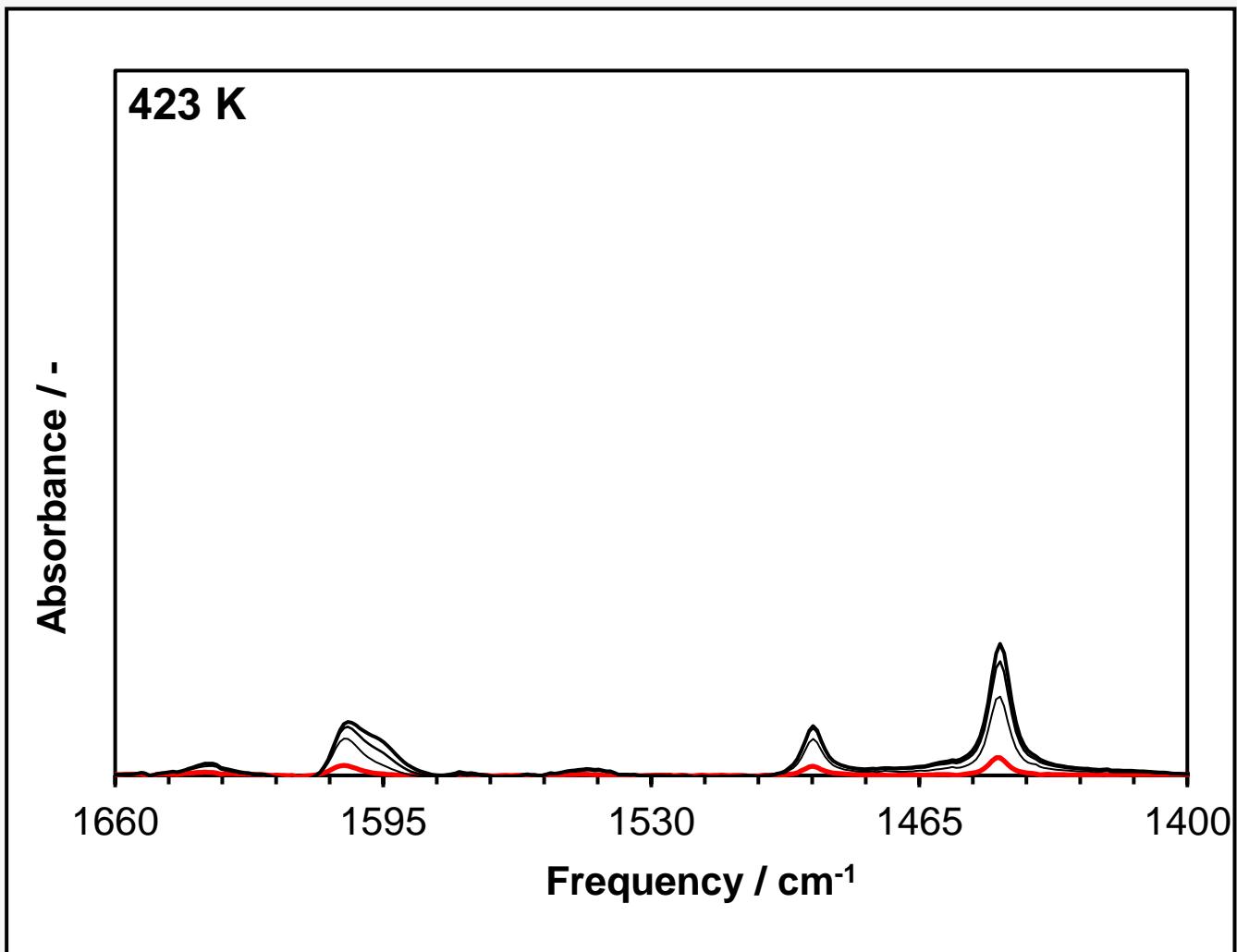


Pyridine Titration on Y/deAlBeta Under Vacuum

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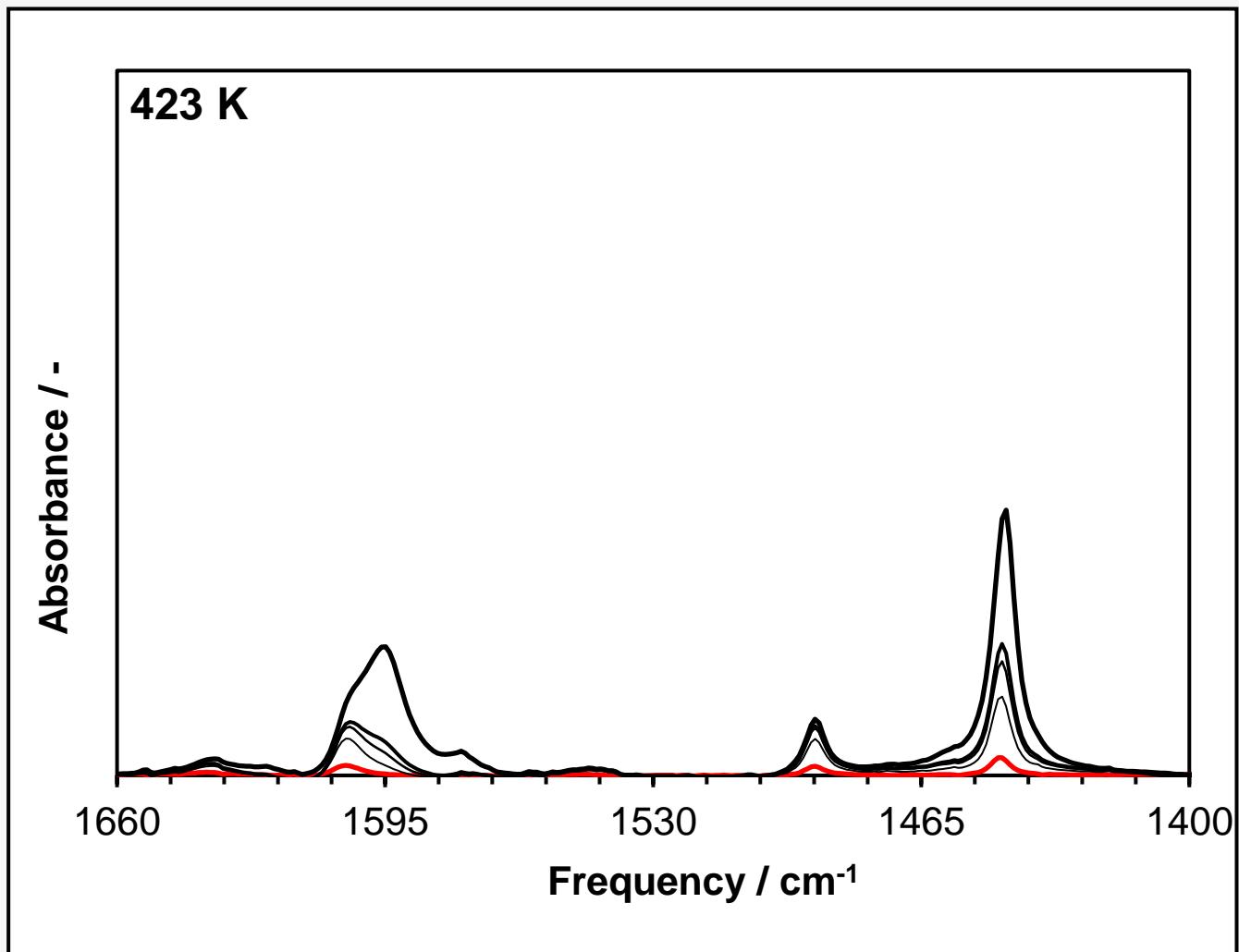


Pyridine Titration on Y/deAlBeta Under Vacuum

Step 1: Dose

Step 2: Saturate

Step 3: Evacuate

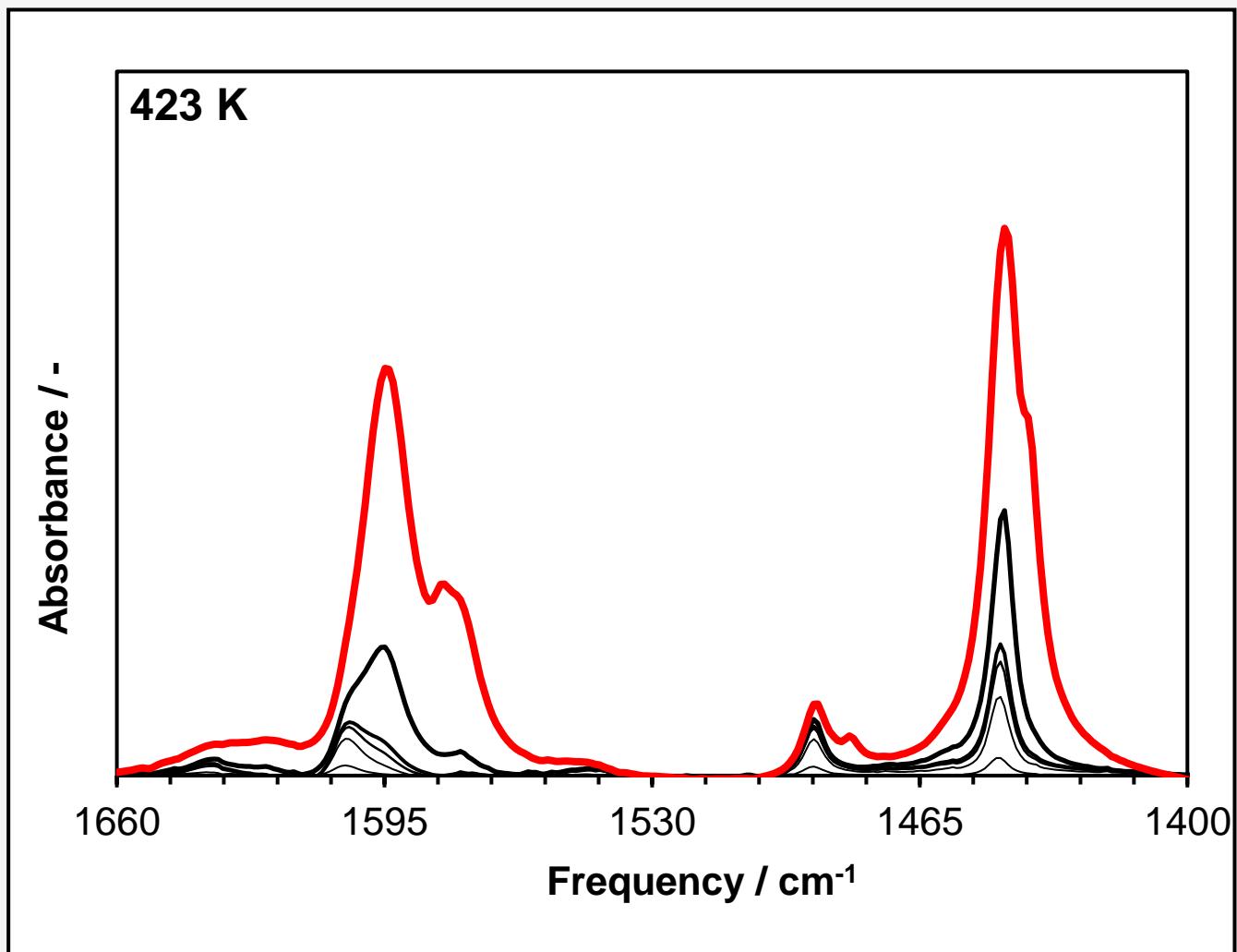


Pyridine Titration on Y/deAlBeta Under Vacuum

Step 1: Dose

Step 2: Saturate

Step 3: Evacuate

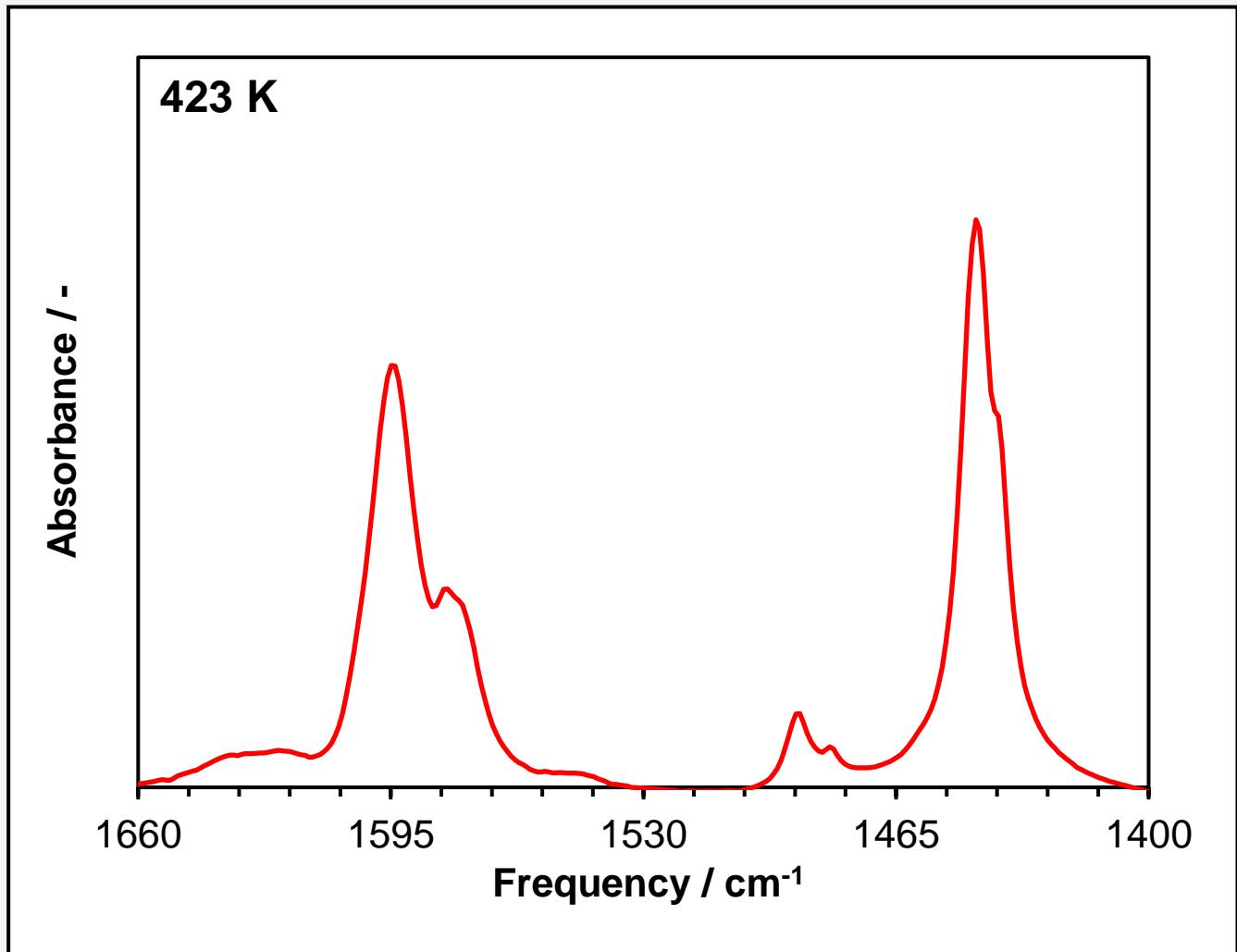


Pyridine Titration on Y/deAlBeta Under Vacuum

Step 1: Dose

Step 2: Saturate

Step 3: Evacuate



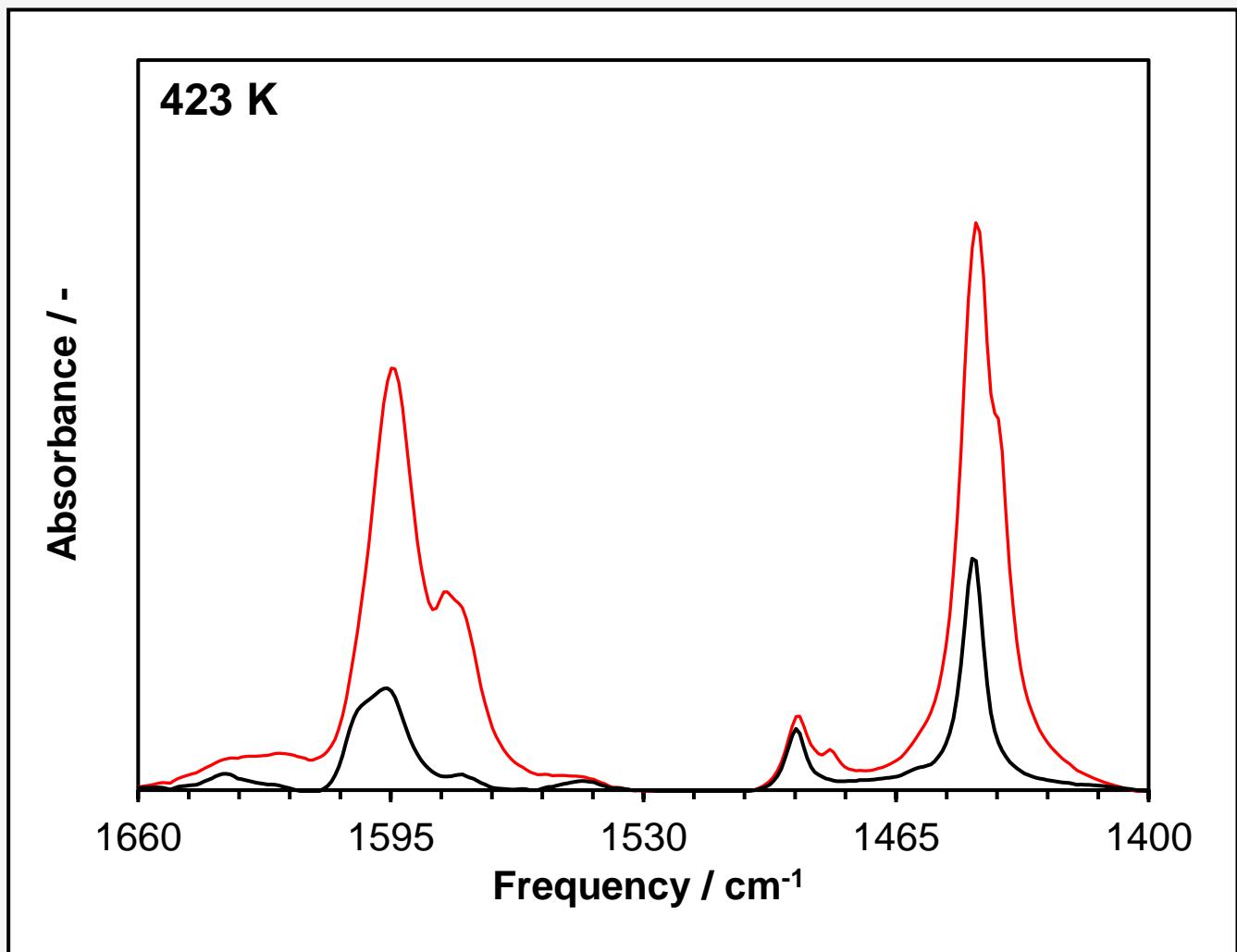
- Red = saturated pyridine dose

Pyridine Titration on Y/deAlBeta Under Vacuum

Step 1: Dose

Step 2: Saturate

Step 3: Evacuate



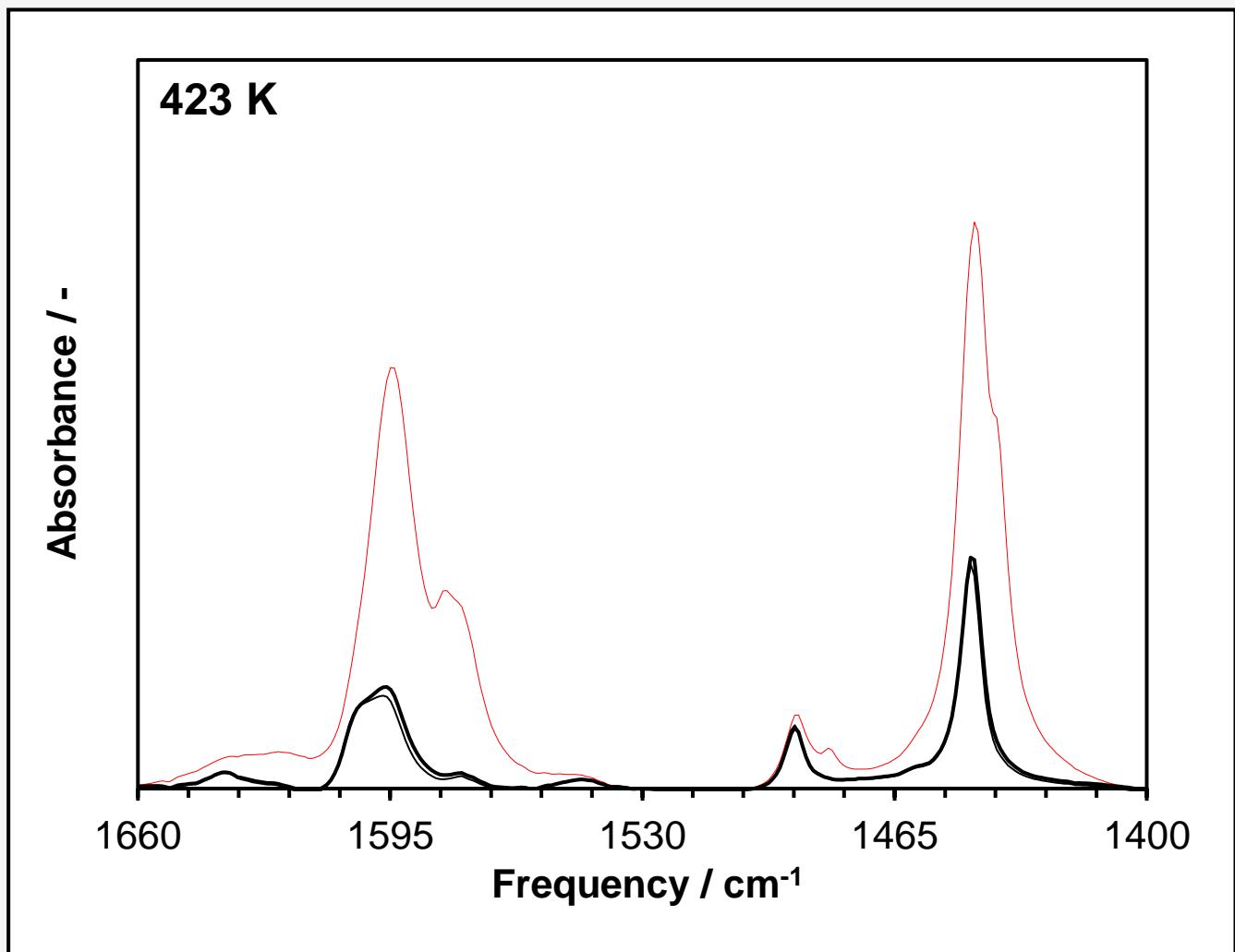
- Red = saturated pyridine dose
- Black = evacuation

Pyridine Titration on Y/deAlBeta Under Vacuum

Step 1: Dose

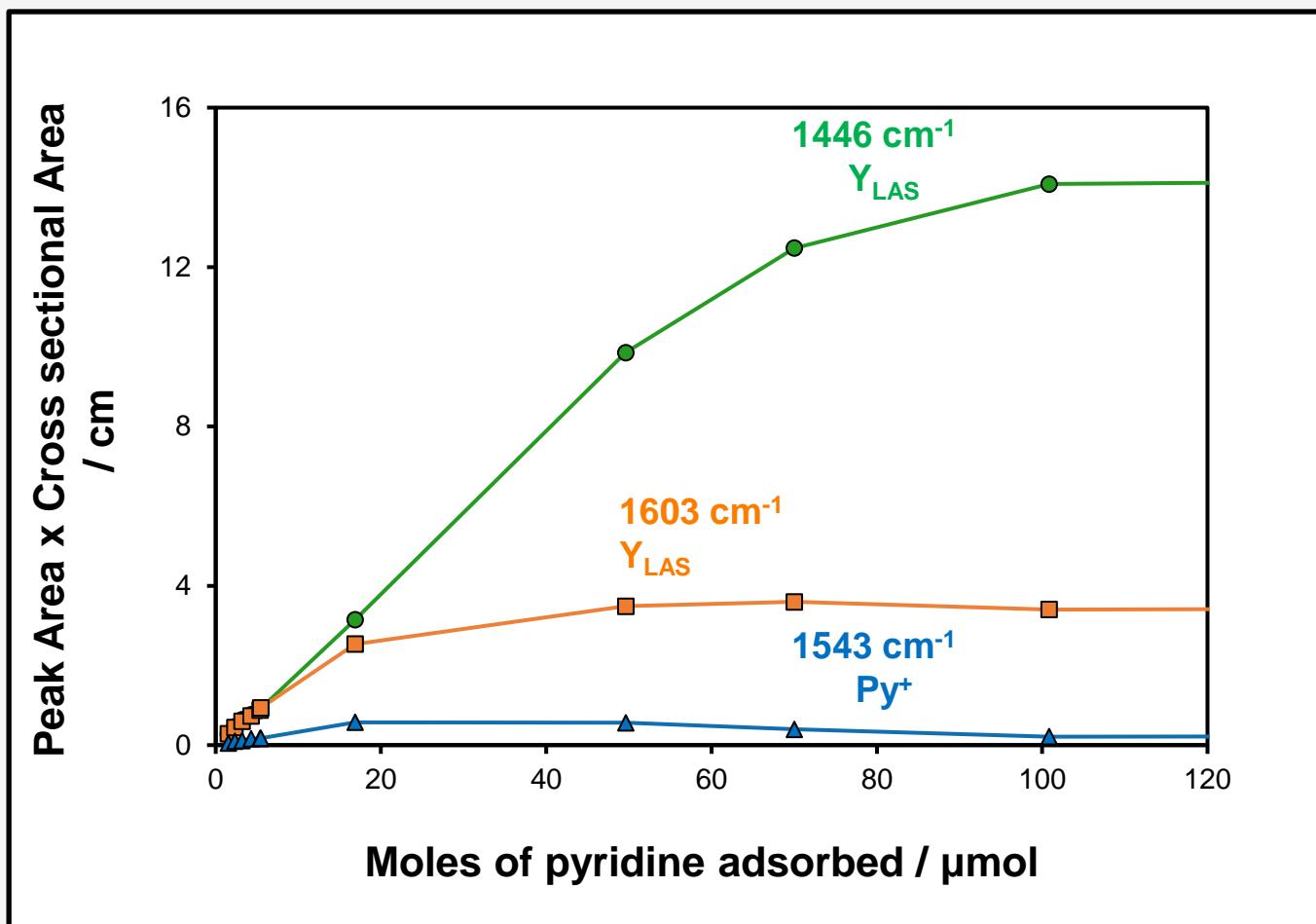
Step 2: Saturate

Step 3: Evacuate

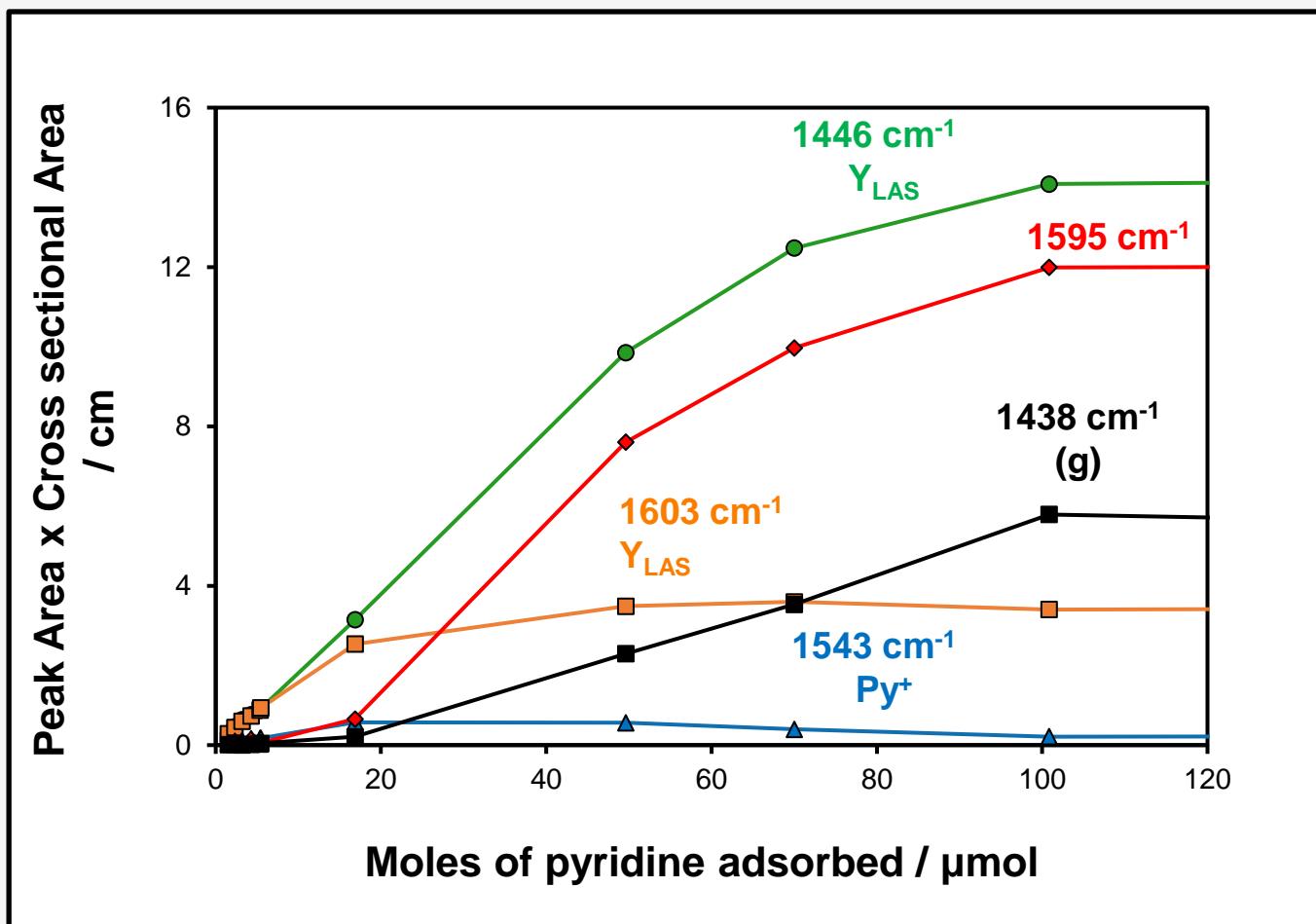


- Red = saturated pyridine dose
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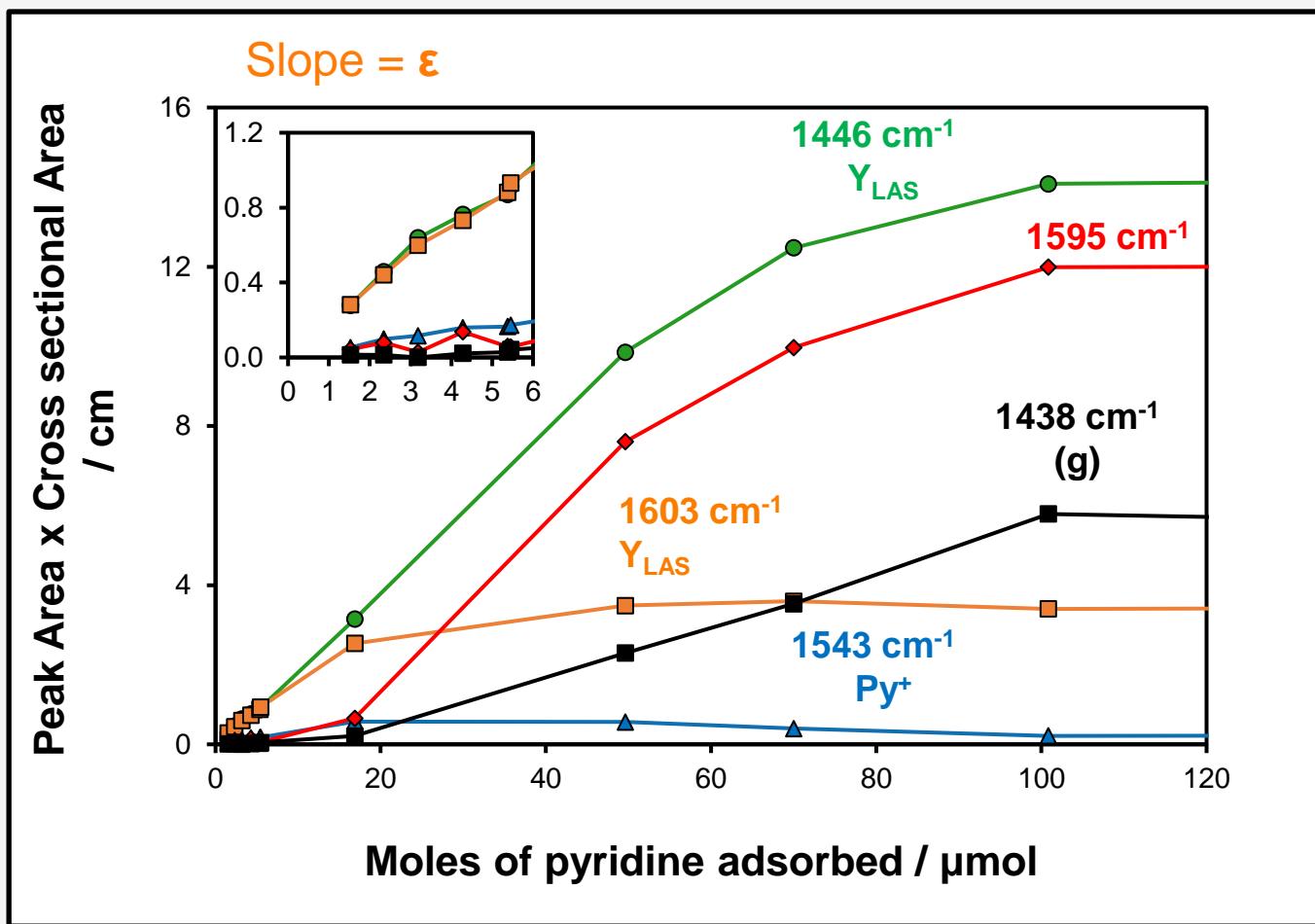
IMEC for Pyridine Bound to Lewis Acidic Y sites ($Y_{10}/deAlBeta$)



IMEC for Pyridine Bound to Lewis Acidic Y sites ($Y_{10}/deAlBeta$)

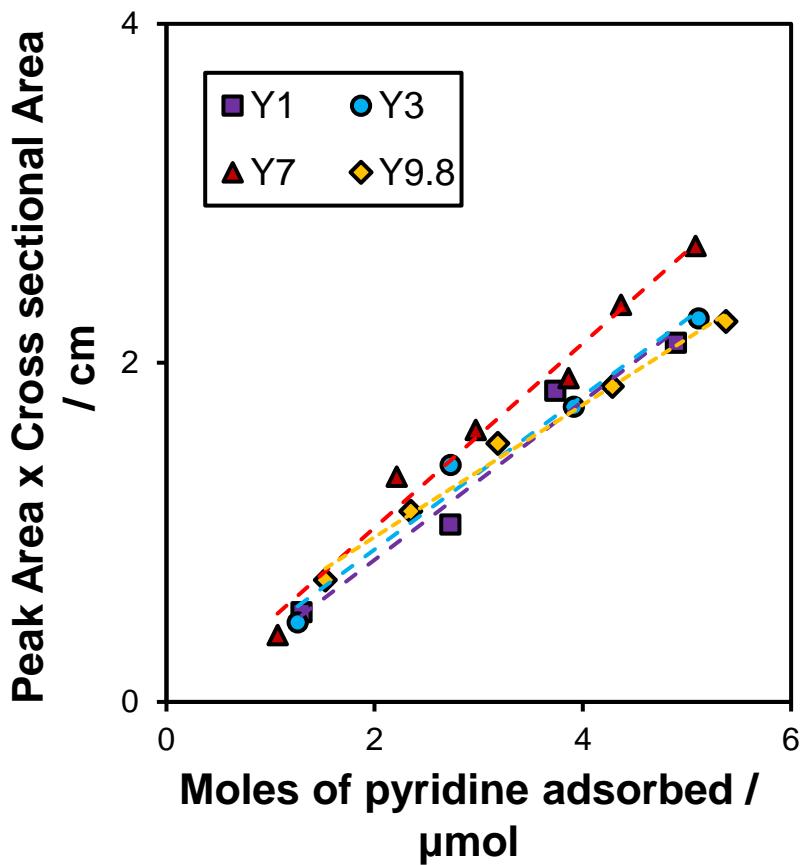


IMEC for Pyridine Bound to Lewis Acidic Y sites ($Y_{10}/deAlBeta$)

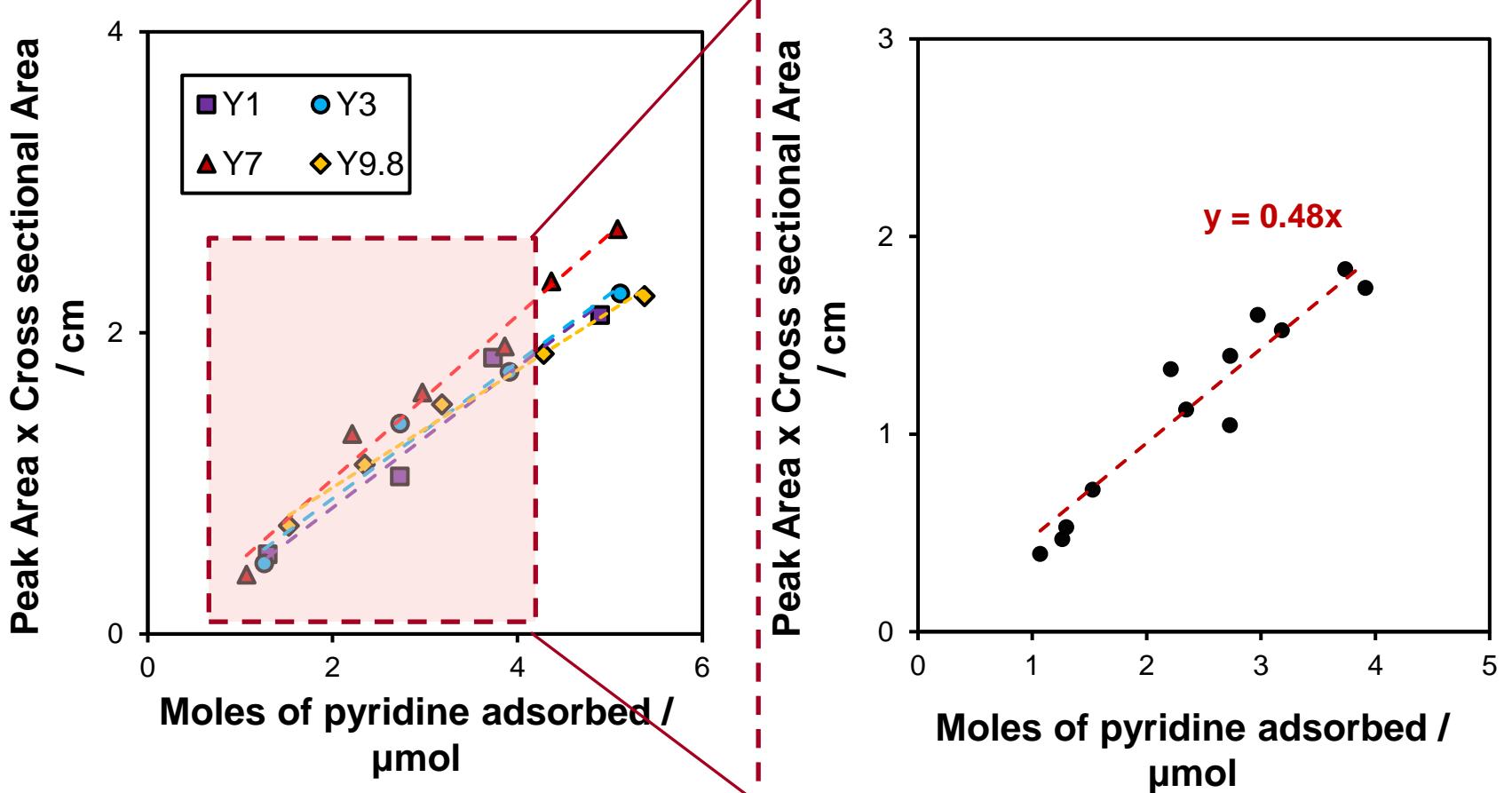


$$A = \epsilon b C$$

Comparison of Initial Slopes – Various Y/deAlBeta Samples

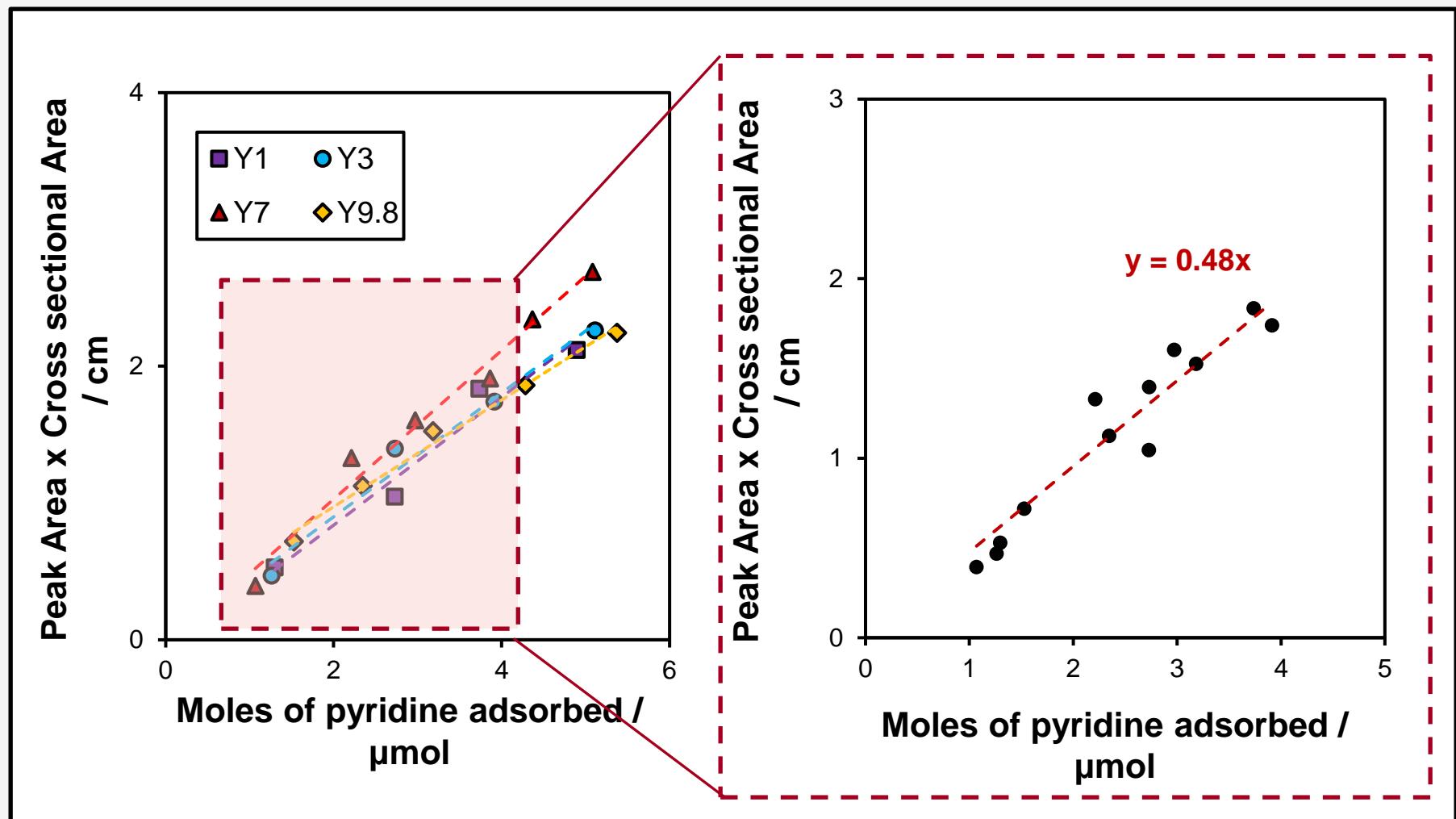


Comparison of Initial Slopes – Various Y/deAlBeta Samples



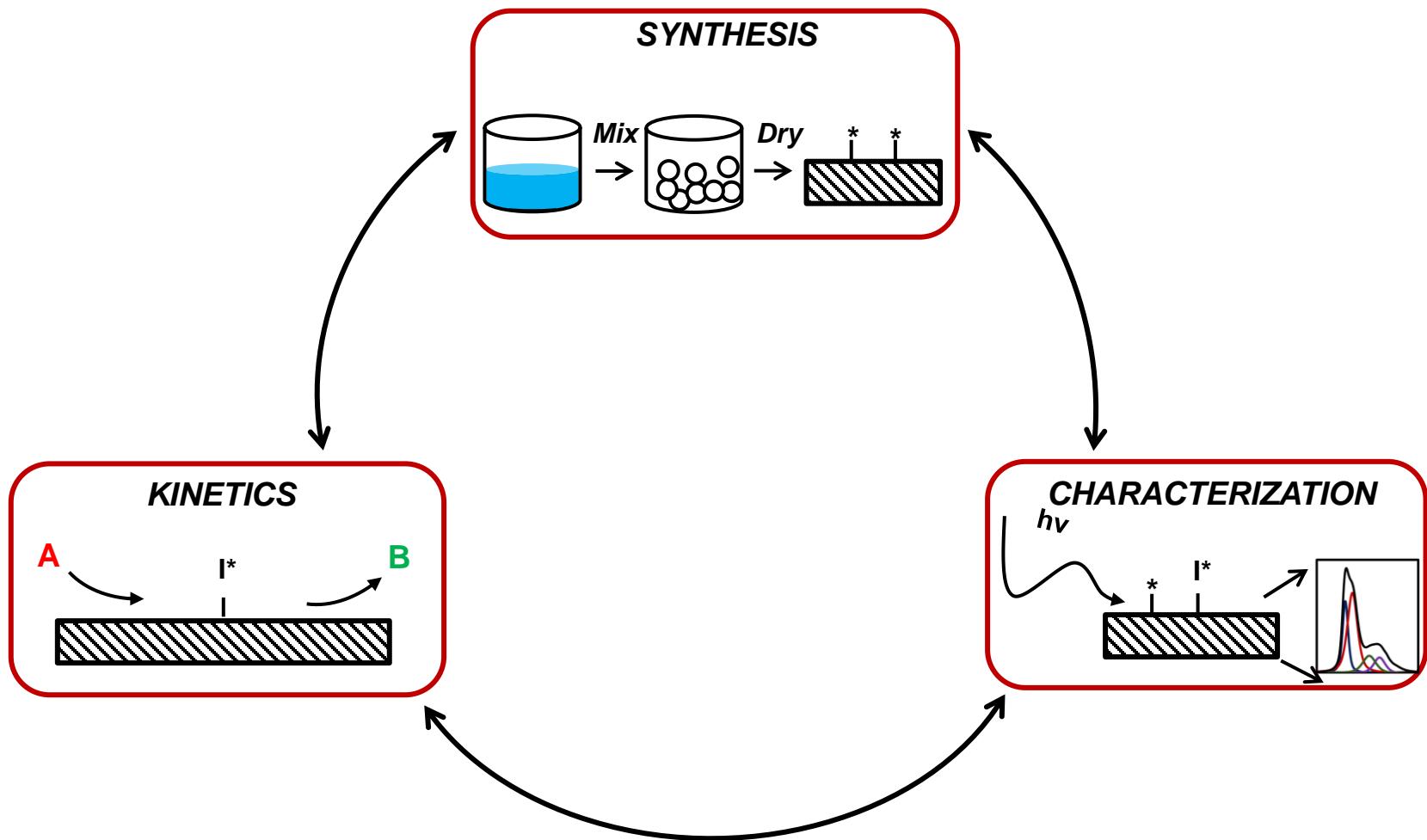
$$A = \epsilon b C$$

Comparison of Initial Slopes – Various Y/deAlBeta Samples

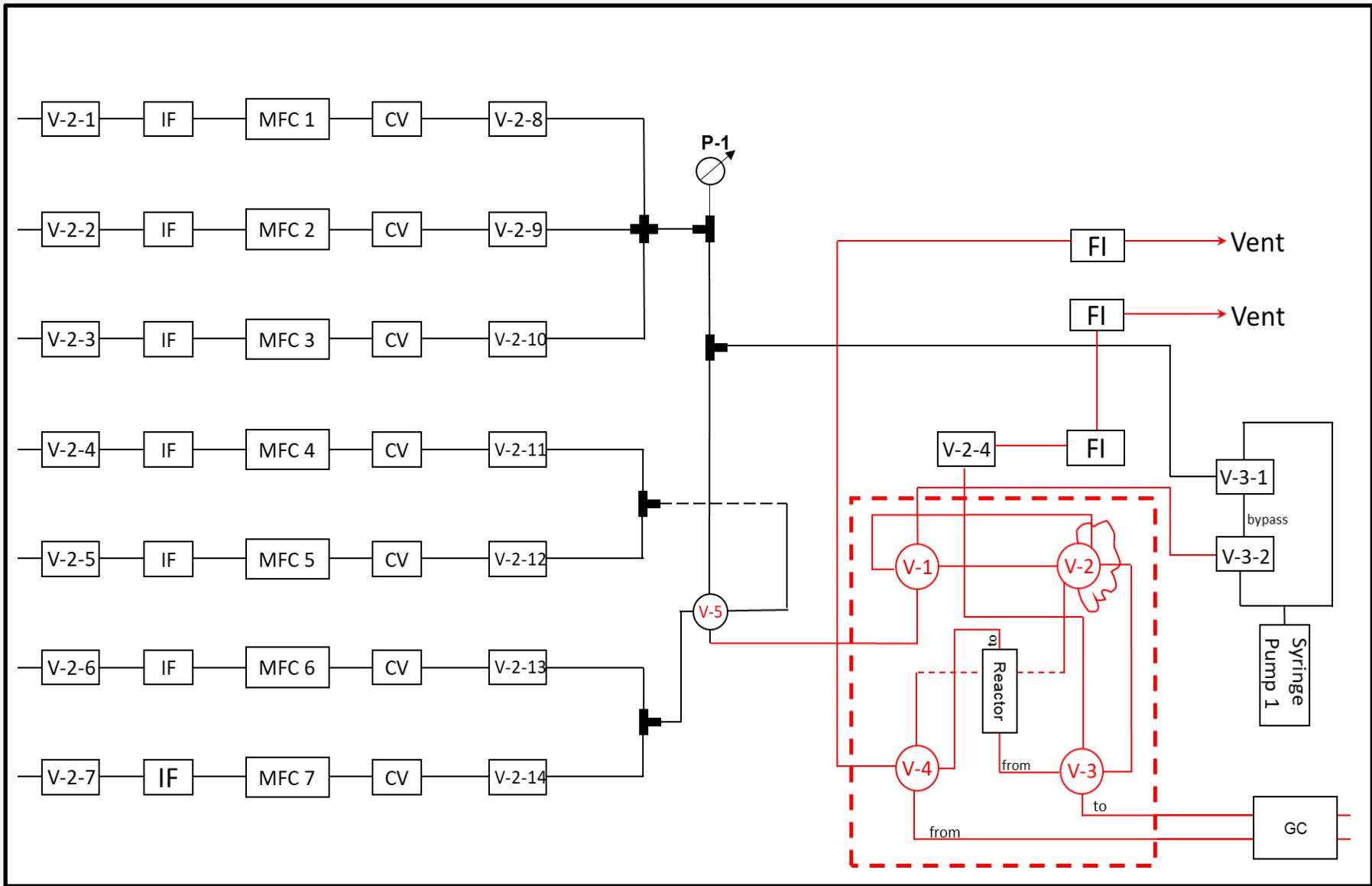


We can quantify YLAS by ex situ pyridine IR, but is that a relevant quantity?

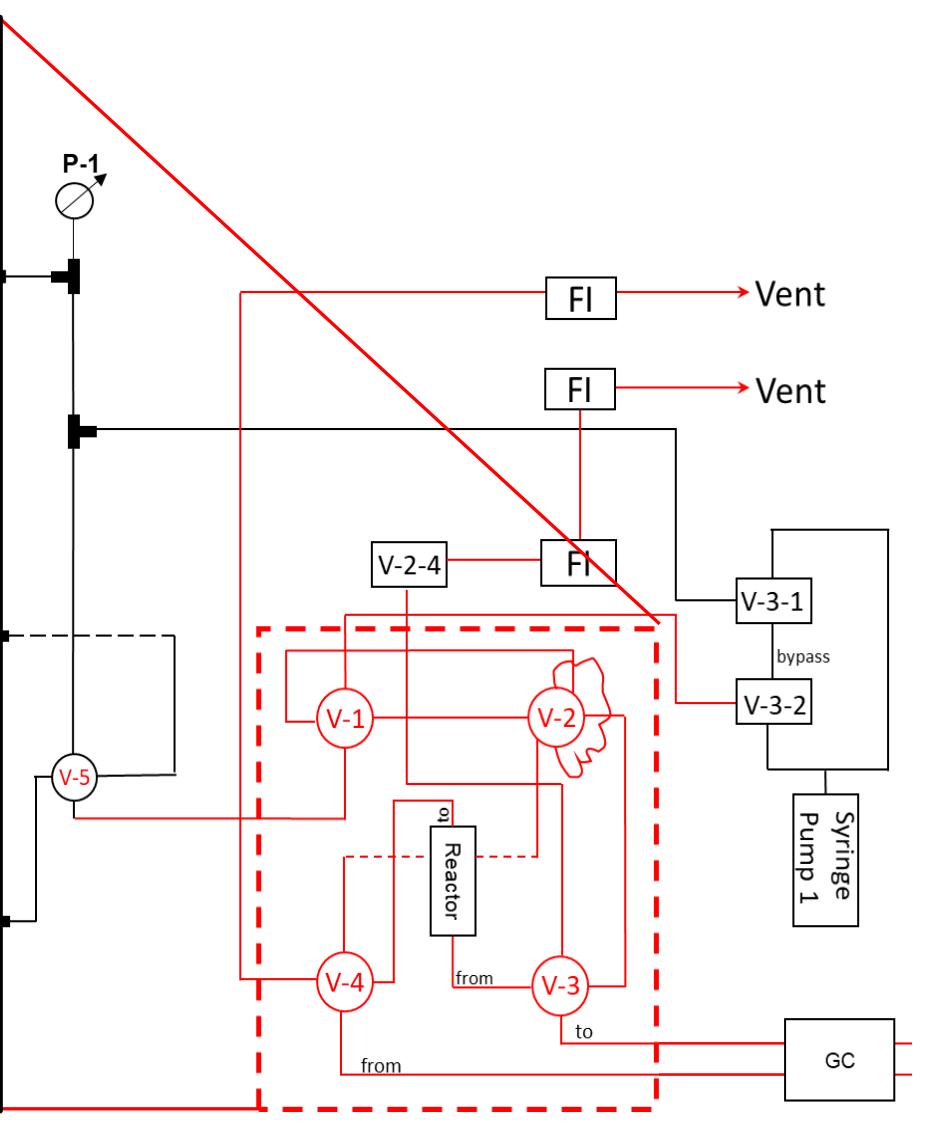
Kinetic measurements



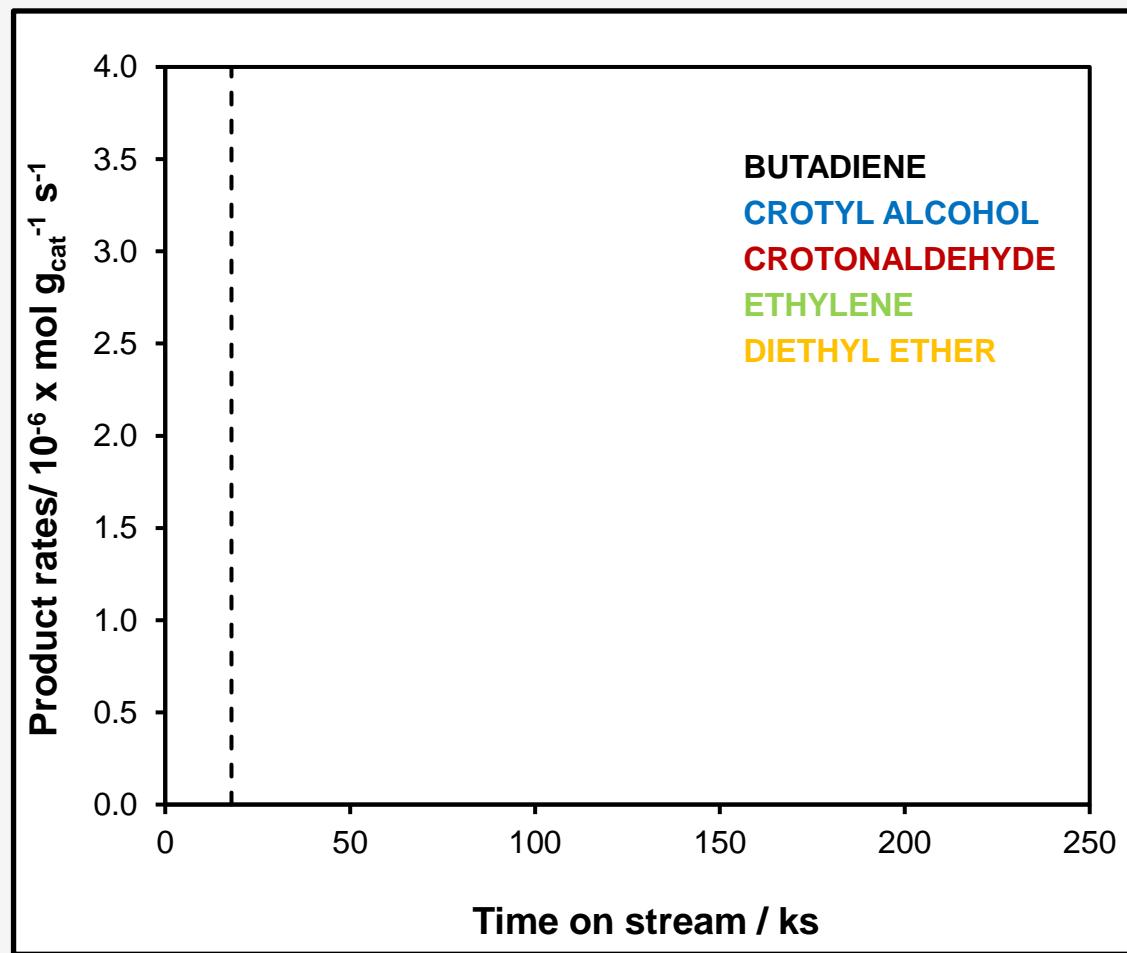
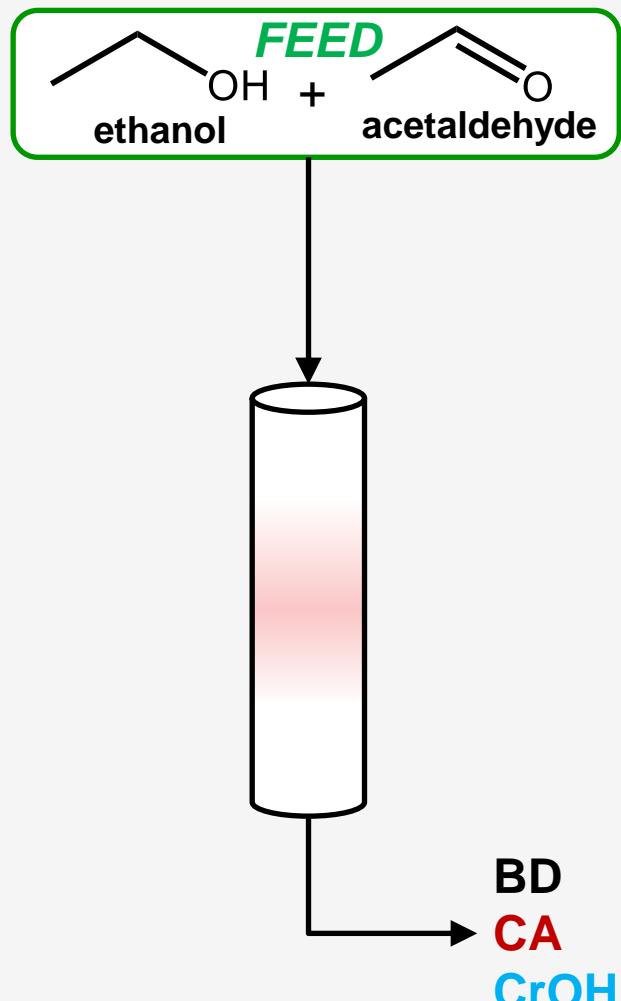
Process Flow Diagram of Reactor Setup



Process Flow Diagram of Reactor Setup



Quantification of Y Active Sites via In Situ Titrations



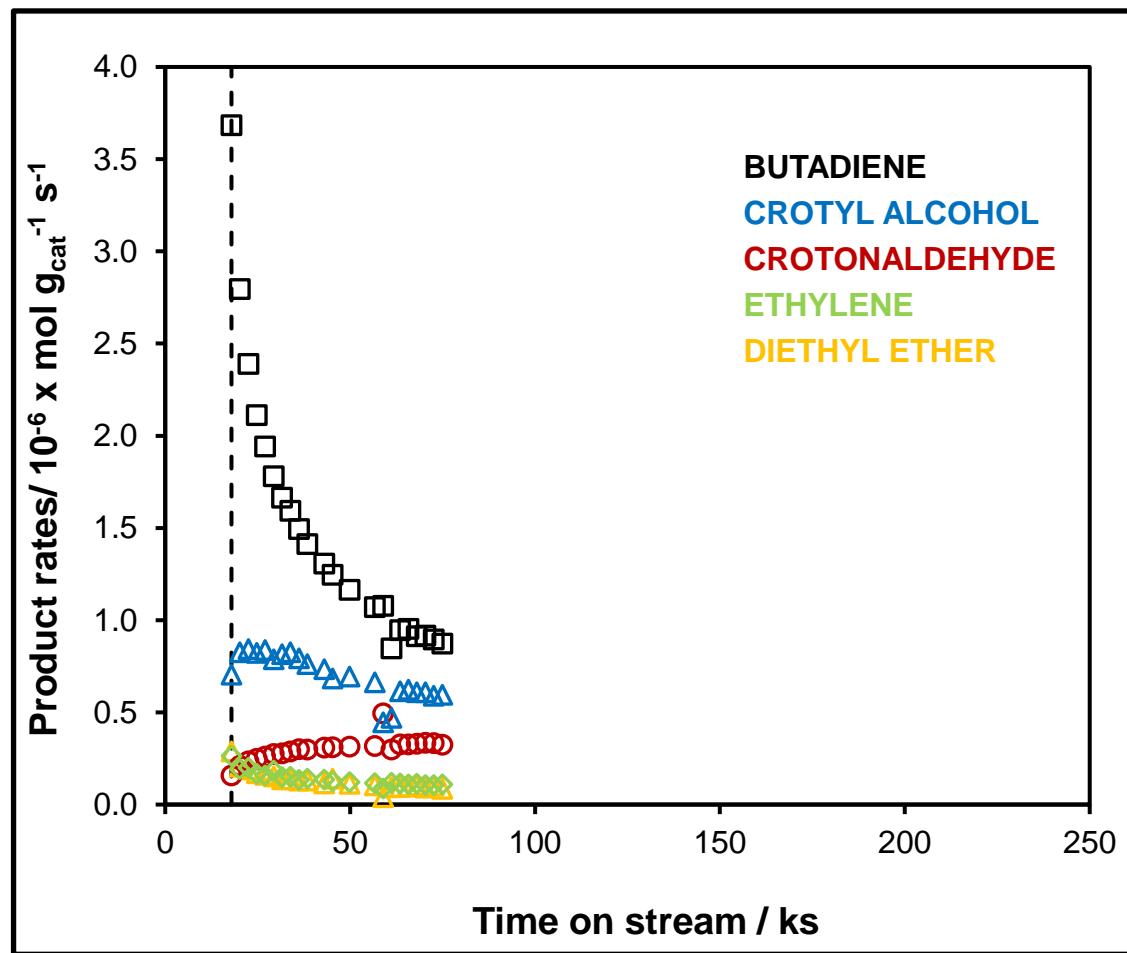
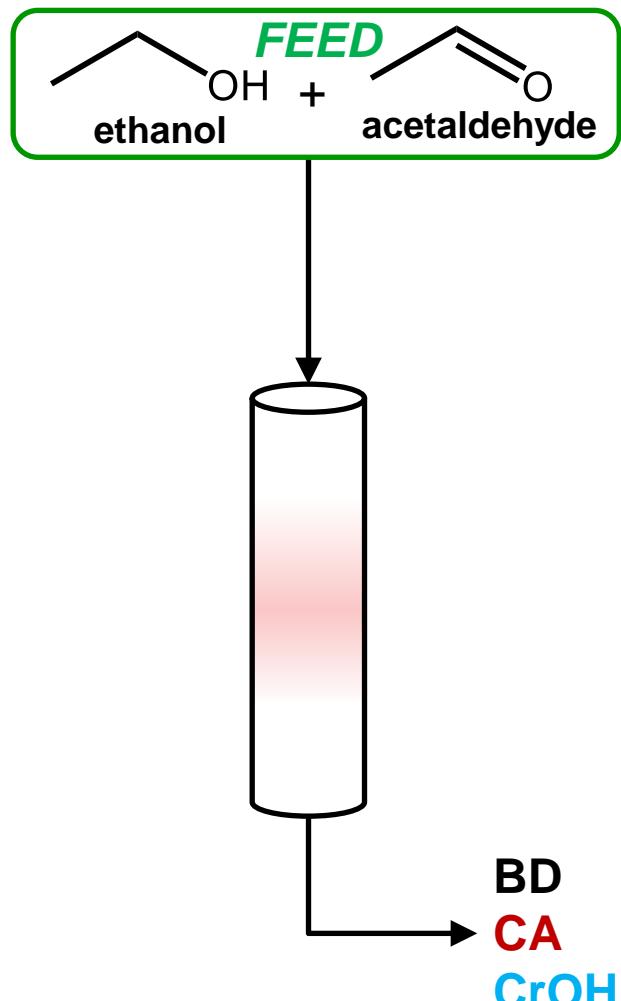
Reaction conditions: T = 503 K; P = 124 kPa;

Gas Flows: 0.4 kPa AcH, 0.000148 kPa Py (0.01% in EtOH), 3 kPa EtOH,
0.98 kPa CH₄, bal He; Total flow 100 cm³.min⁻¹;

Catalyst: 0.01 g Y₃/Beta diluted in 0.09 g SiO₂

Borate, Samad, Harris et al., *in prep*

Quantification of Y Active Sites via In Situ Titrations



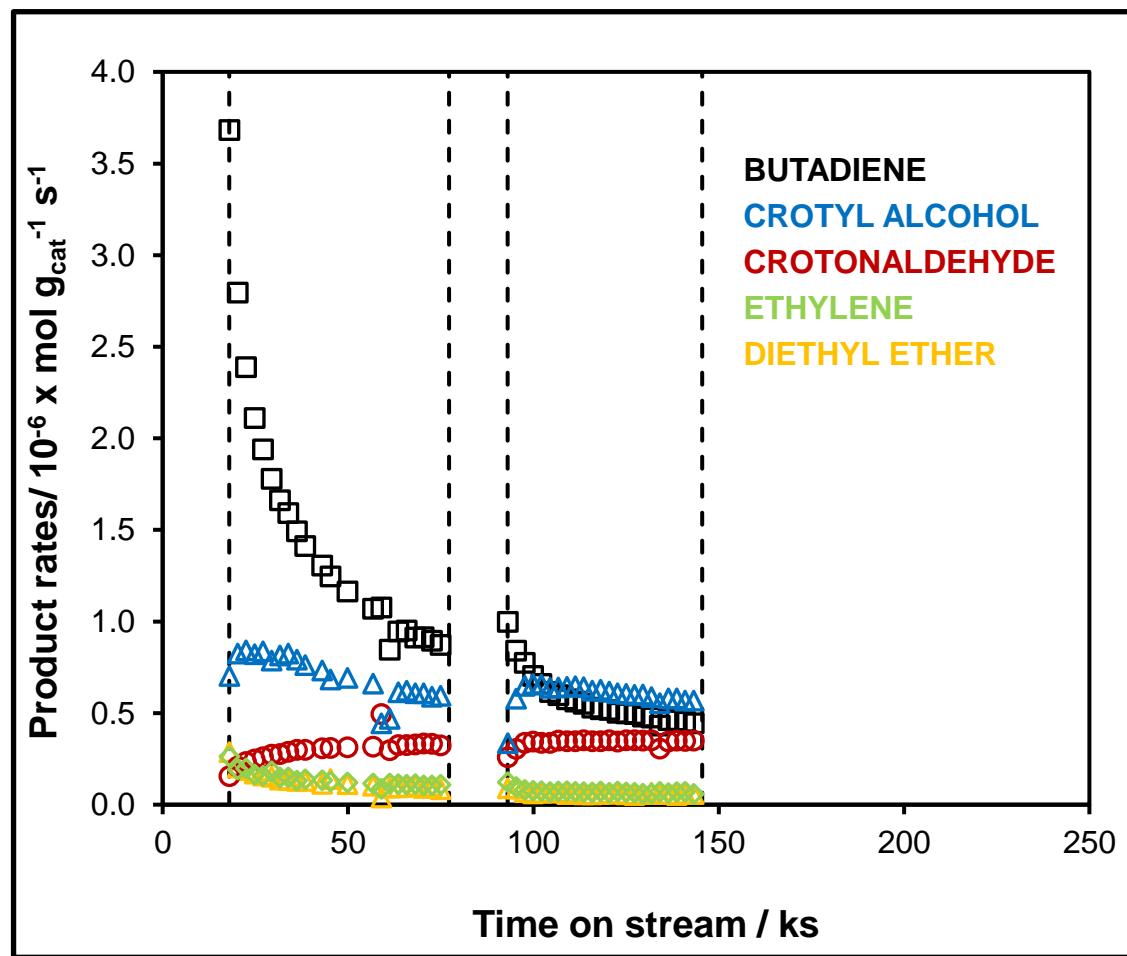
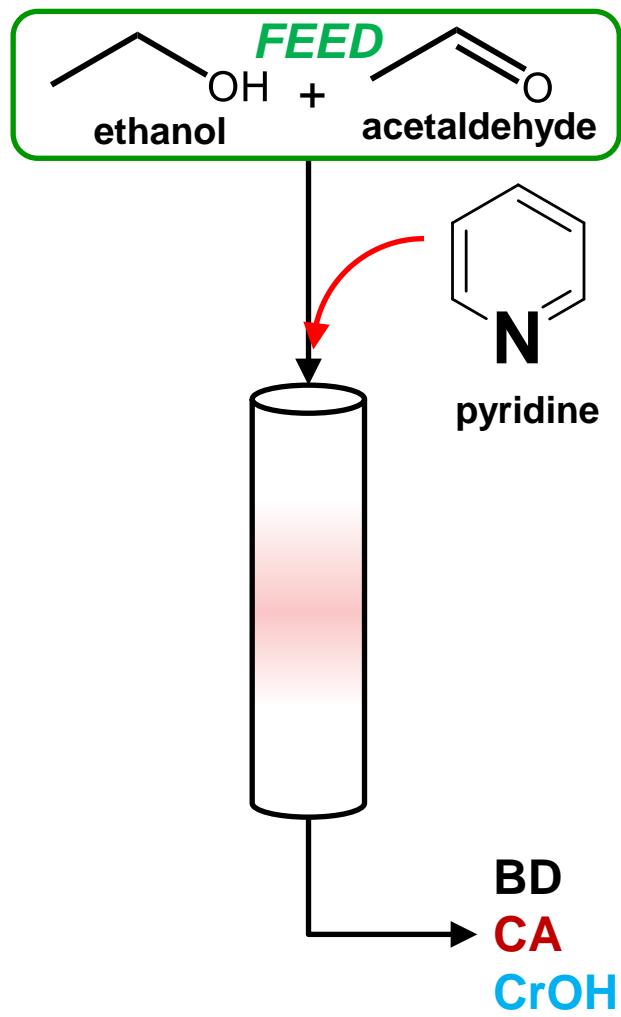
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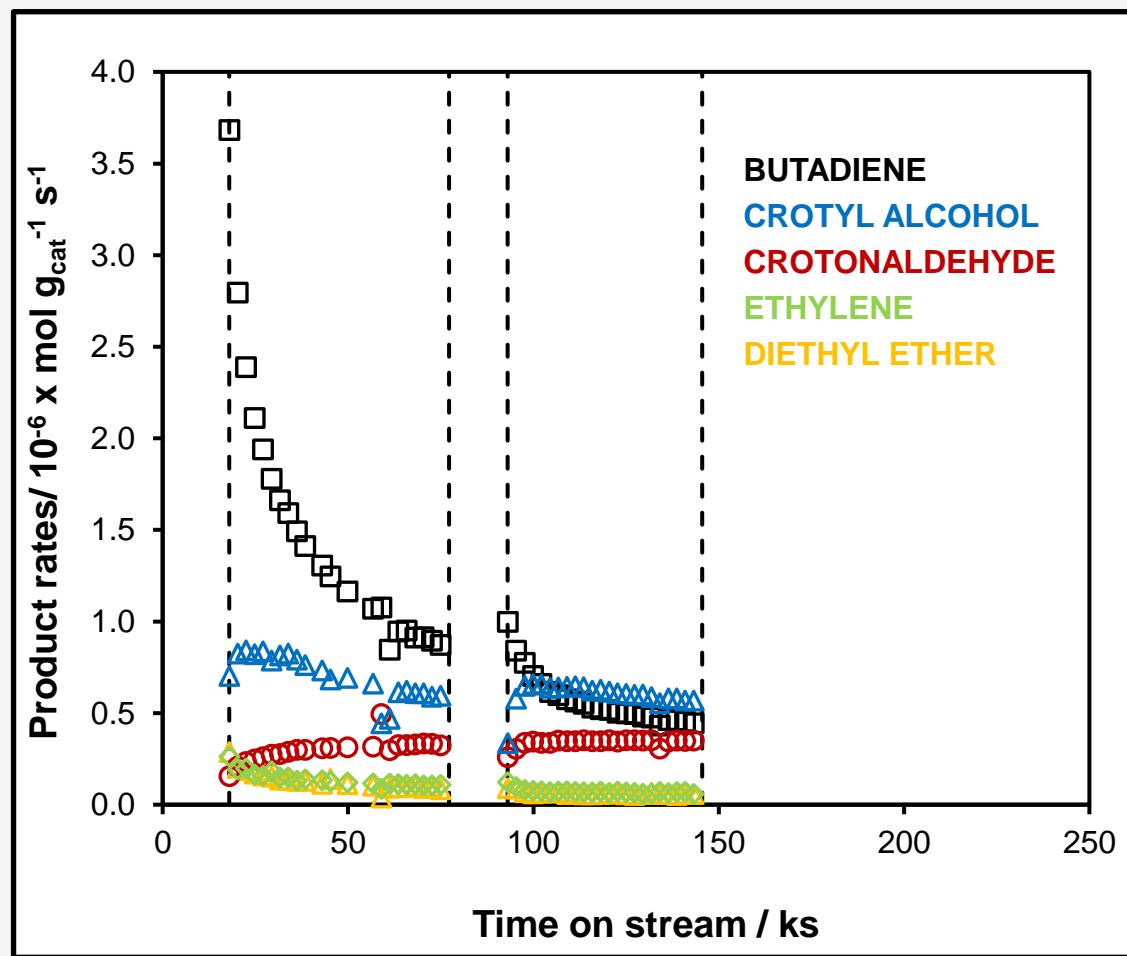
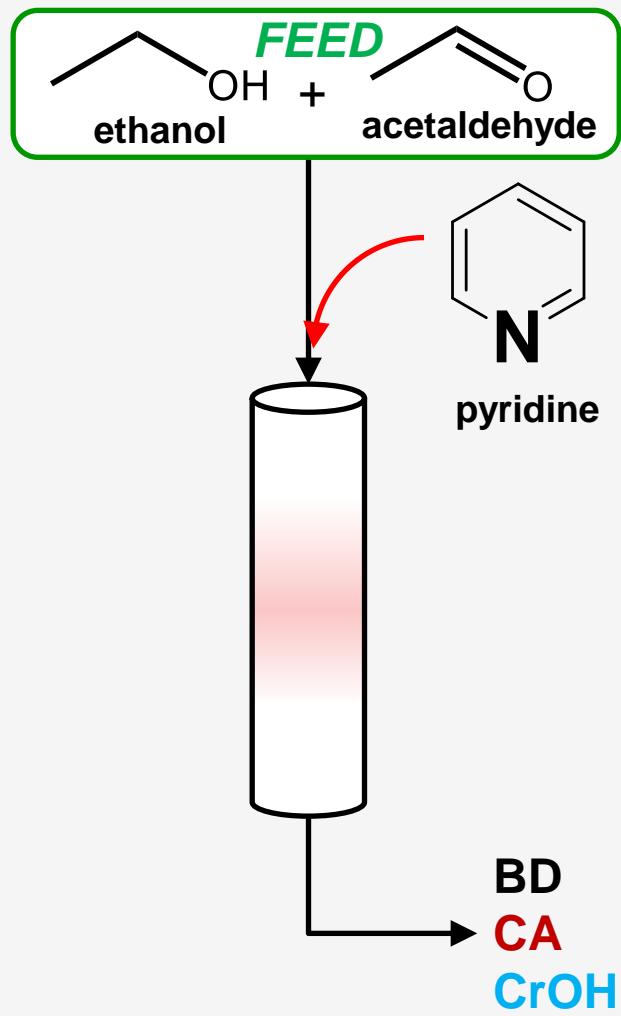
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Quantification of Y Active Sites via In Situ Titrations



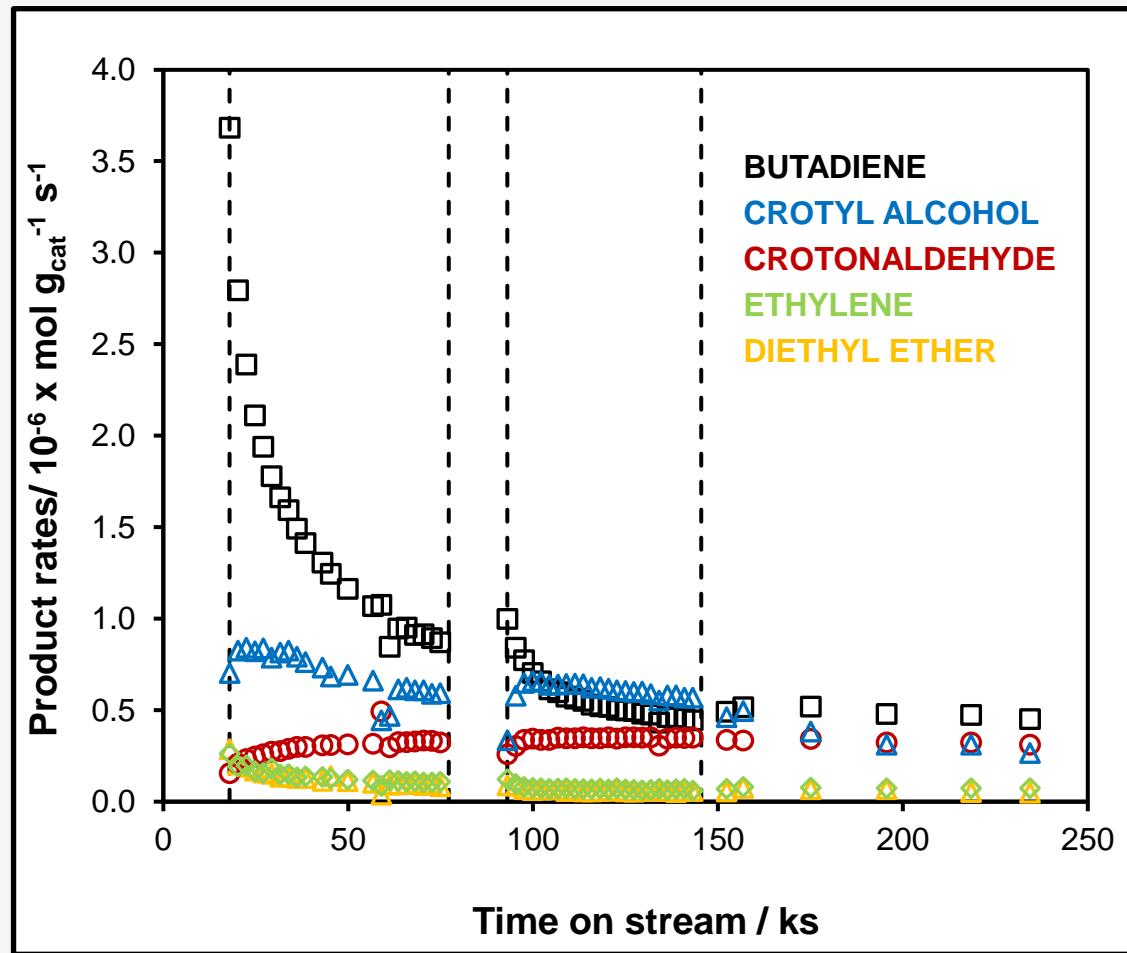
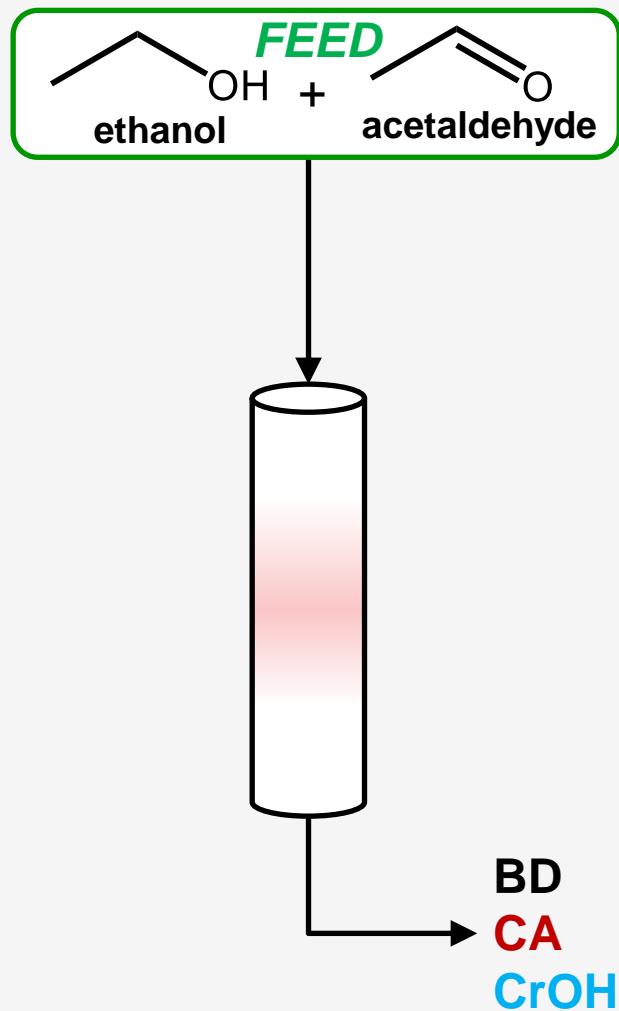
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Catalyst: 0.01 g Y₃/deAlBeta diluted in 0.09 g SiO₂

Borate, Samad, Harris et al., *in prep*

Quantification of Y Active Sites via In Situ Titrations



Reaction conditions: T = 503 K; P = 124 kPa;

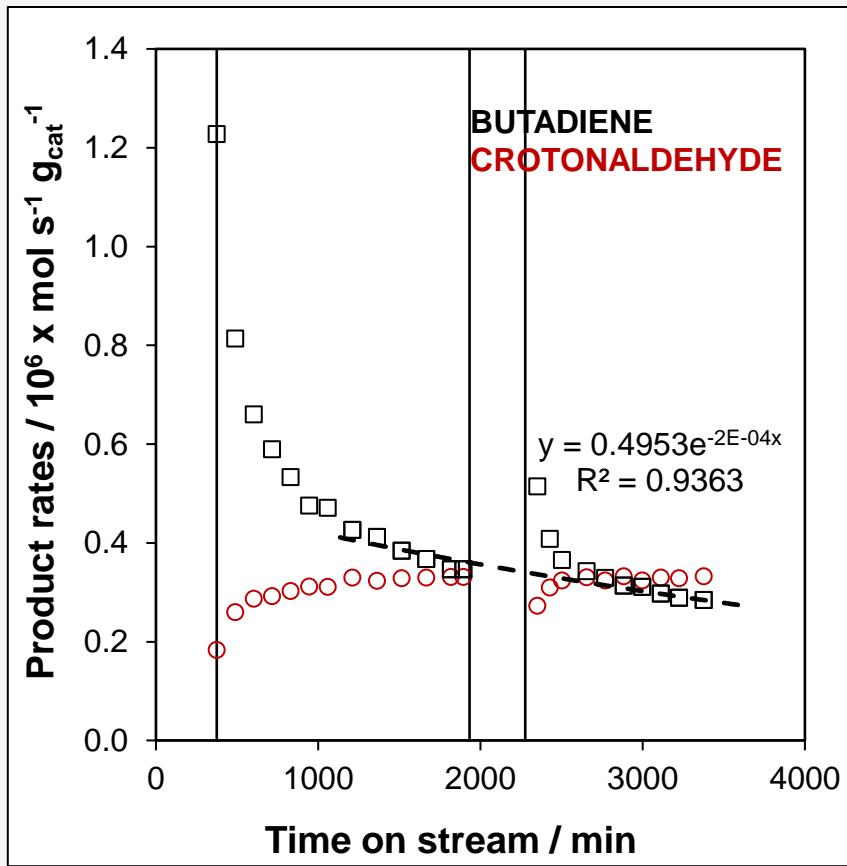
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Catalyst: 0.01 g Y₃/deAlBeta diluted in 0.09 g SiO₂

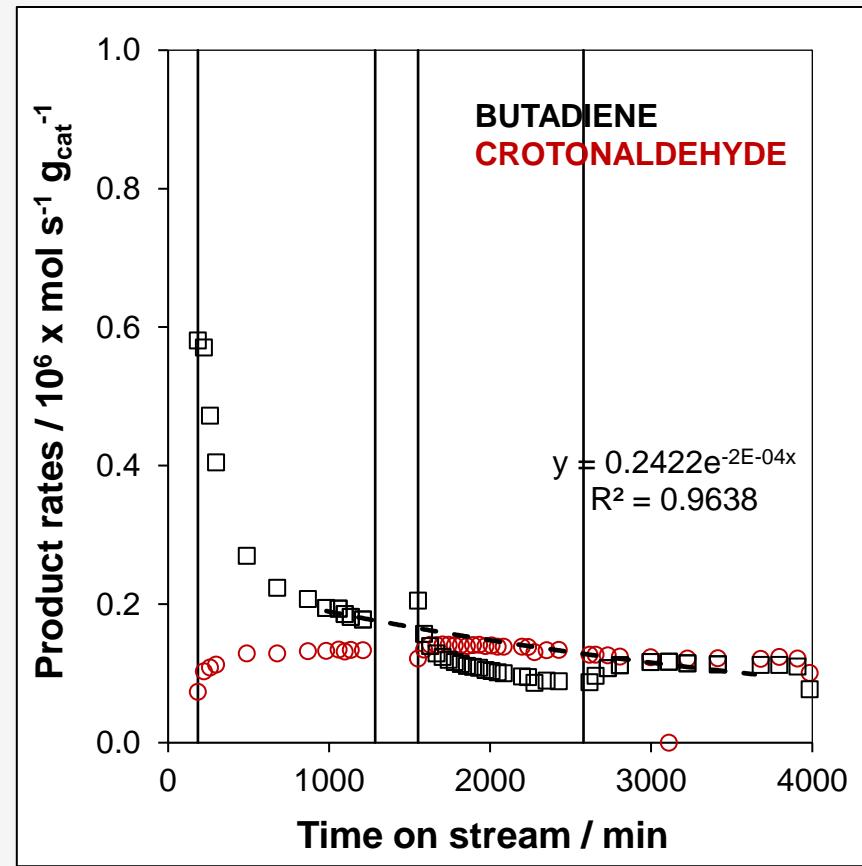
Borate, Samad, Harris et al., *in prep*

EtOH-AcH co feed on Y_{0.5}/deAlBeta

TOS data without pyridine titration



TOS data with pyridine titration



Reaction conditions: T= 503 K, P=124 kPa

Gas flows: without Py titration- 0.7 kPa AcH, 3 kPa EtOH

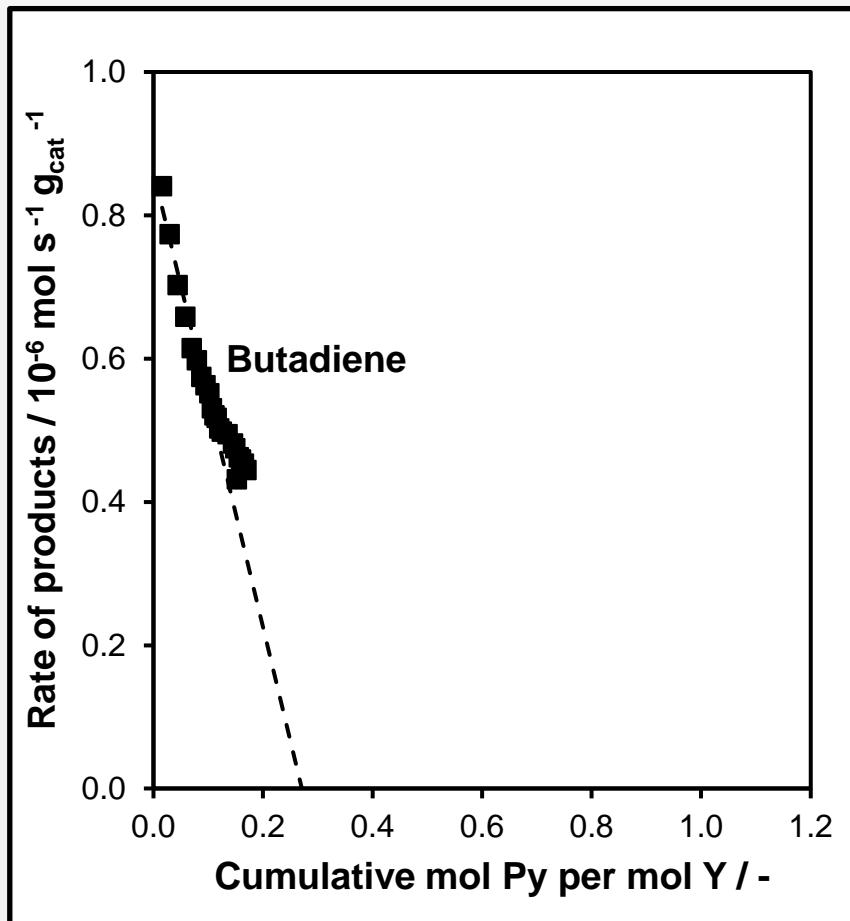
with Py titration- 0.5 kPa AcH, 0.000148 kPa Py (0.01% in EtOH), 3 kPa EtOH

0.98 kPa CH₄, bal He. Total flow: 100 cm³ min⁻¹

Catalyst: 0.01 g Y_{0.5}/deAlBeta diluted with SiC or SiO₂

Quantification of Active Sites via In Situ Titrations

Y₃/deAlBeta



Reaction conditions: T = 503 K; P = 124 kPa;

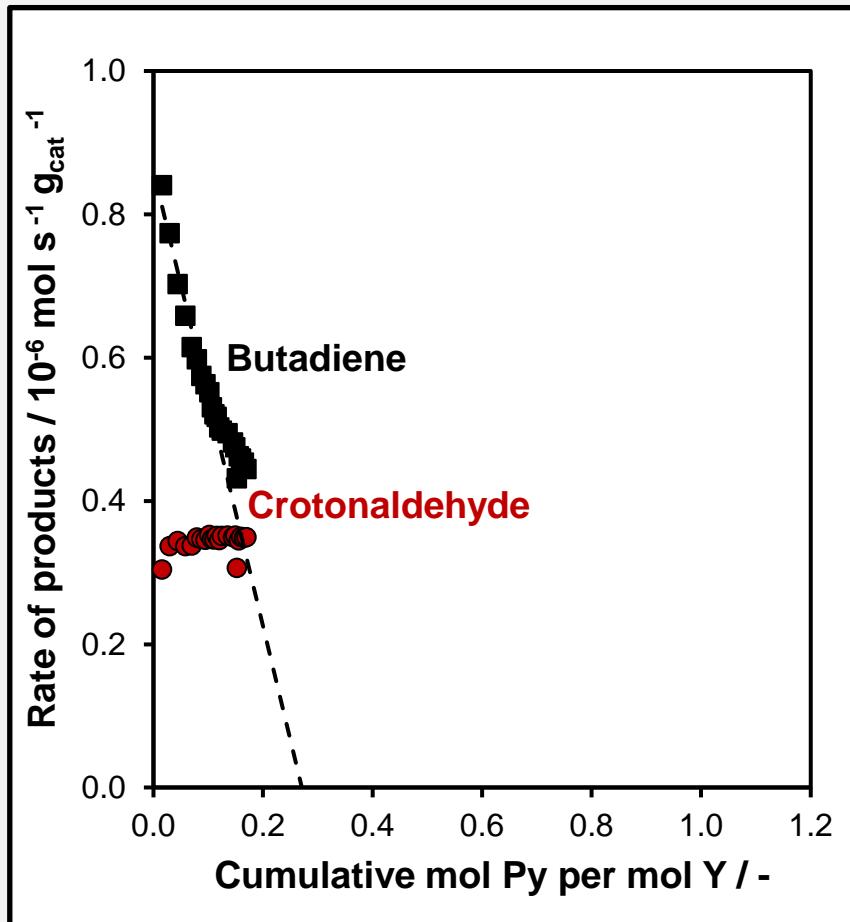
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Catalyst: 0.01 g Y₃/Beta diluted in 0.09 g SiO₂,

Borate, Samad, Harris et al., *in prep*

Quantification of Active Sites via In Situ Titrations

Y₃/deAlBeta



Reaction conditions: T = 503 K; P = 124 kPa;

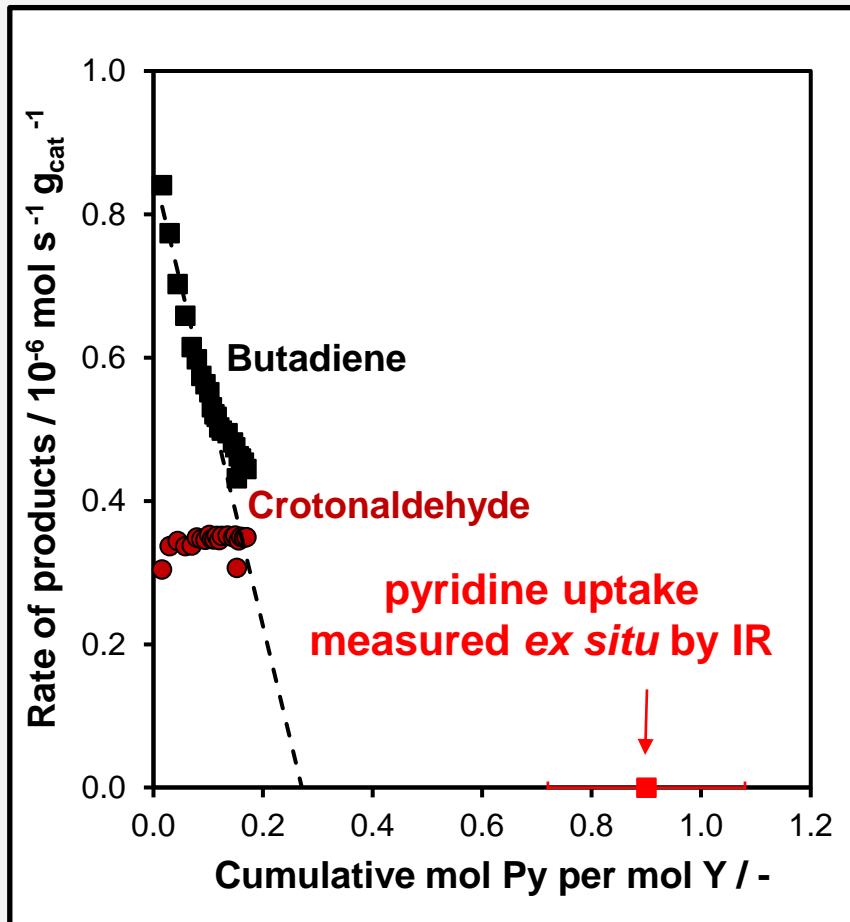
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Catalyst: 0.01 g Y₃/Beta diluted in 0.09 g SiO₂

Borate, Samad, Harris et al., *in prep*

Quantification of Active Sites via In Situ Titrations

$Y_3/deAlBeta$



Reaction conditions: $T = 503 \text{ K}$; $P = 124 \text{ kPa}$;

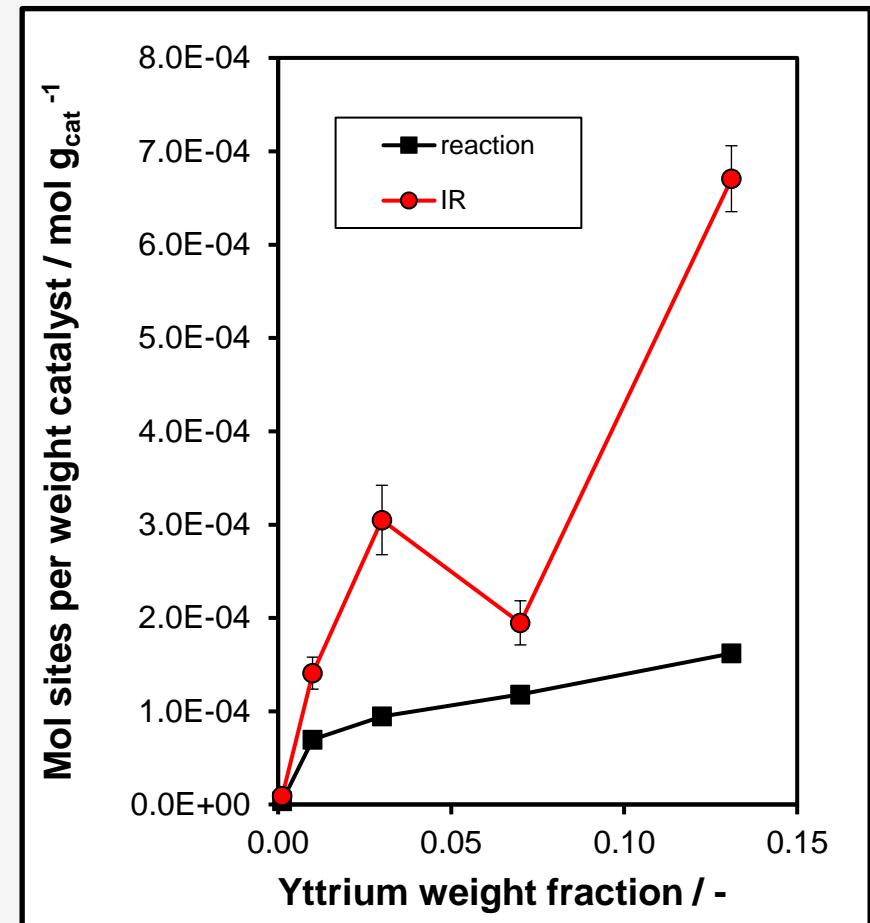
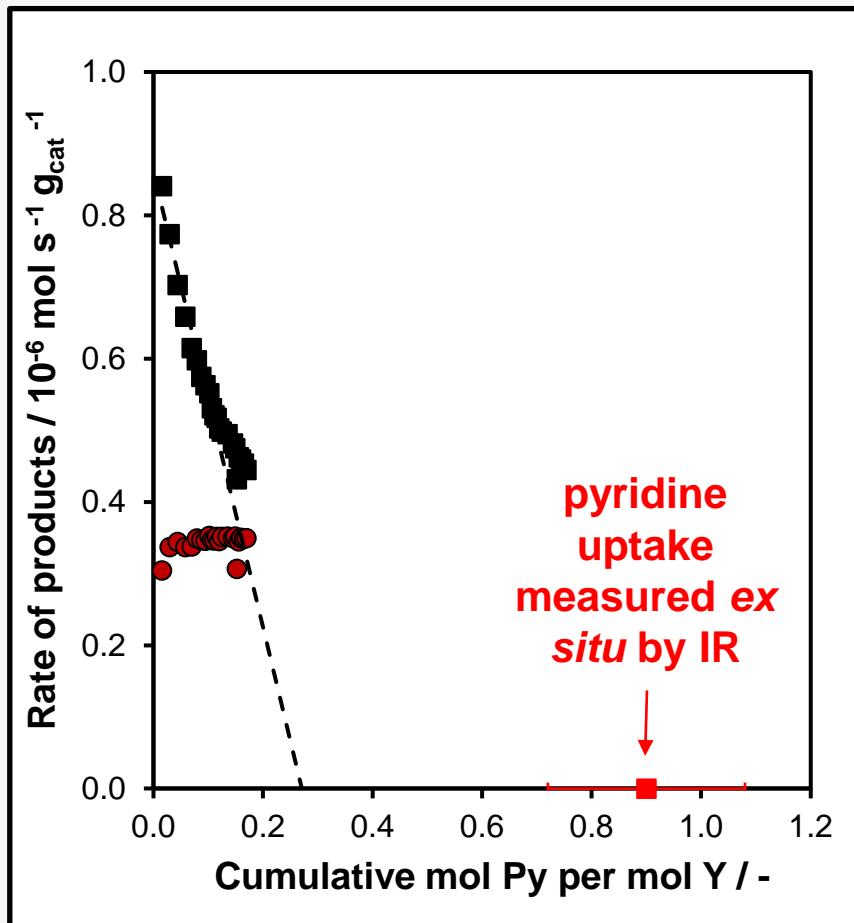
Gas Flows: 0.4 kPa AcH, 0.000148 kPa Py, 3 kPa EtOH,
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Catalyst: 0.01 g Y₃/Beta diluted in 0.09 g SiO₂

Borate, Samad, Harris et al., *in prep*

Comparison of in situ and ex situ site titrations

Y₃/deAlBeta



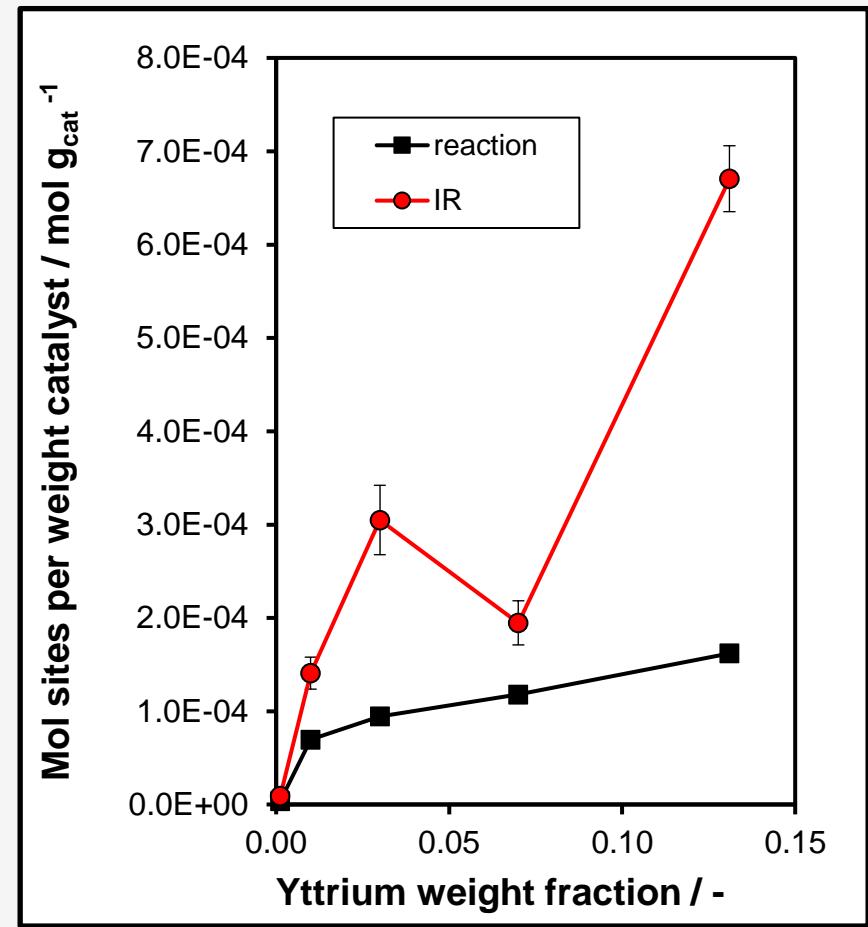
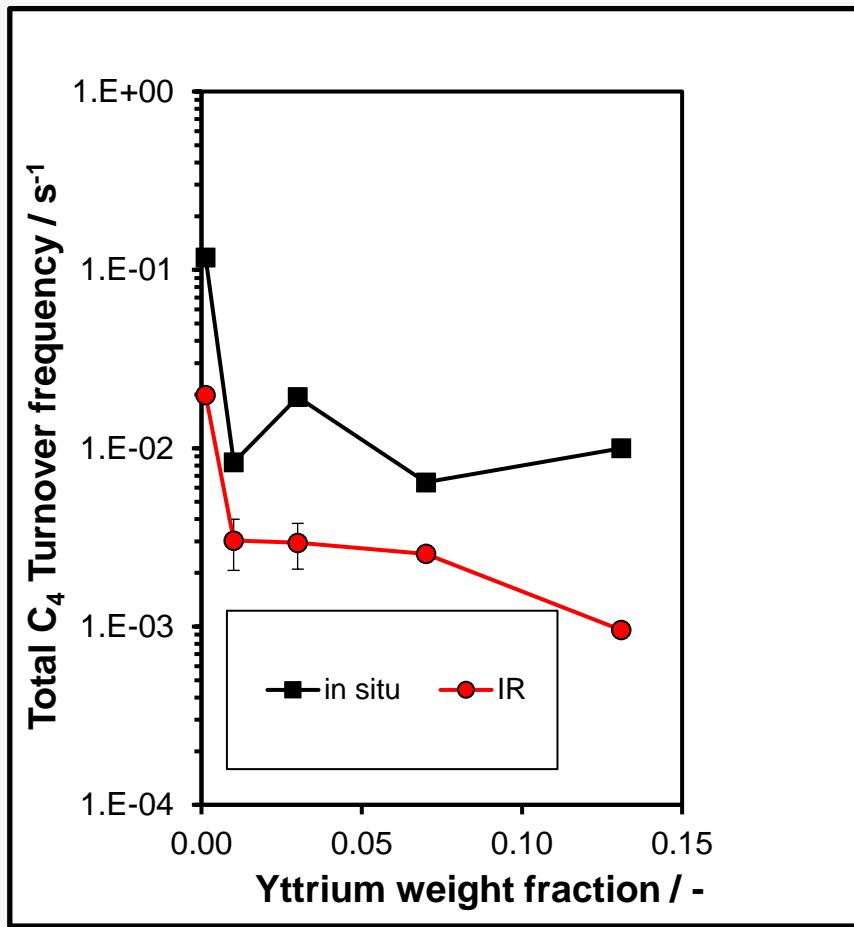
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Borate, Samad, Harris et al., *in prep*

Comparison of in situ and ex situ site titrations



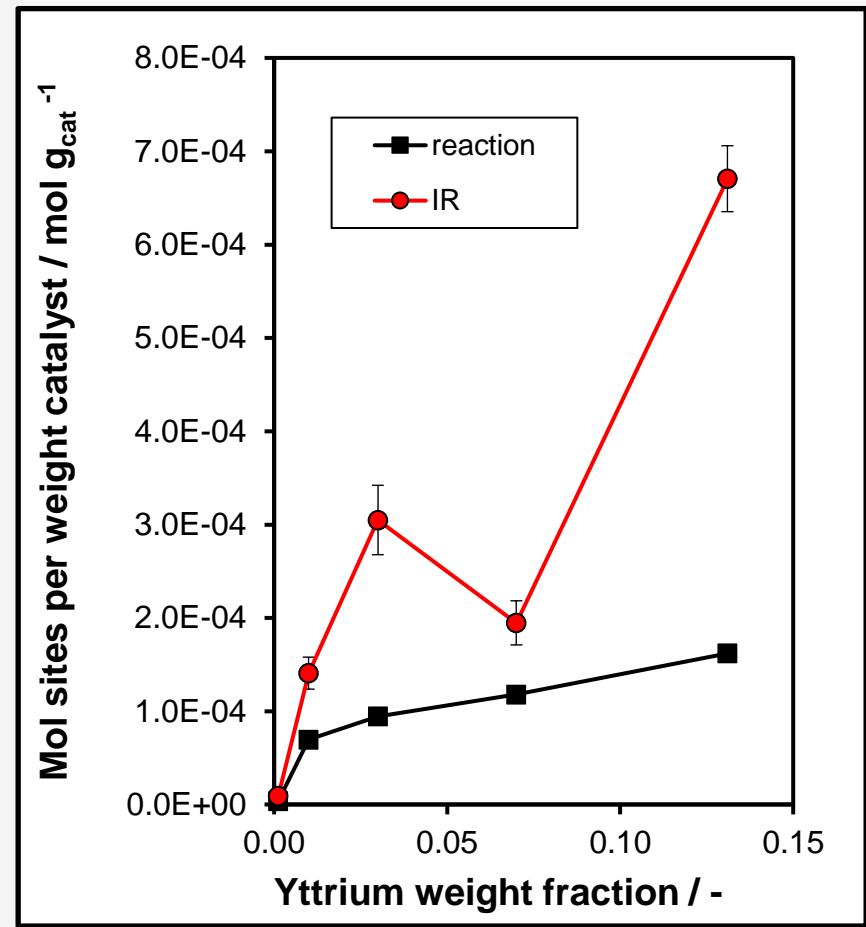
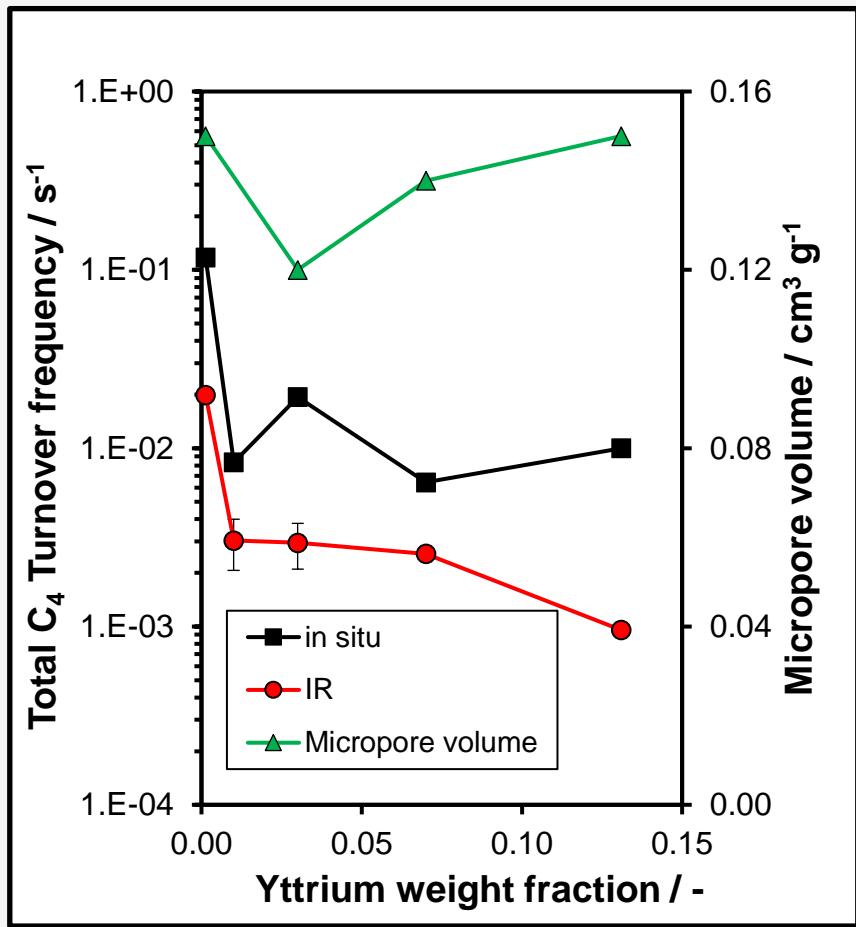
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Catalyst: 0.01 g Y/Beta diluted in 0.09 g SiO₂

Borate, Samad, Harris et al., *in prep*

*Comparison of *in situ* and *ex situ* site titrations*



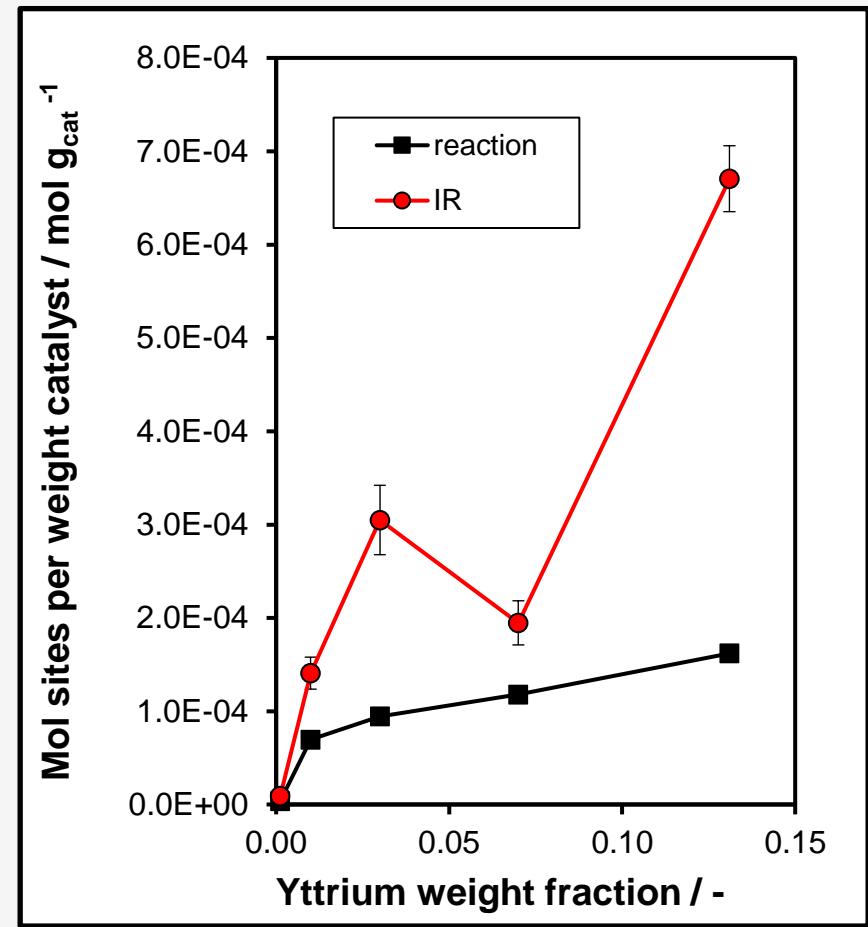
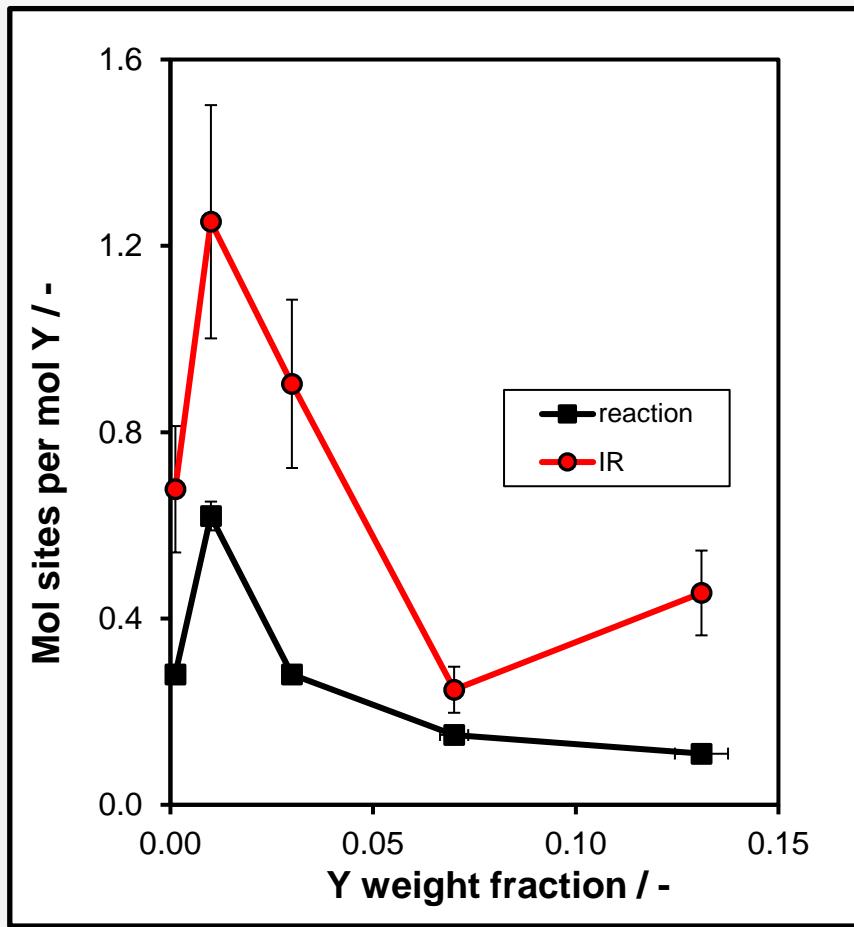
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Gas Flows: 0.4 kPa AcH, 0.000148 kPa Py, 3 kPa EtOH,
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Borate, Samad, Harris et al., *in prep*

Comparison of in situ and ex situ site titrations



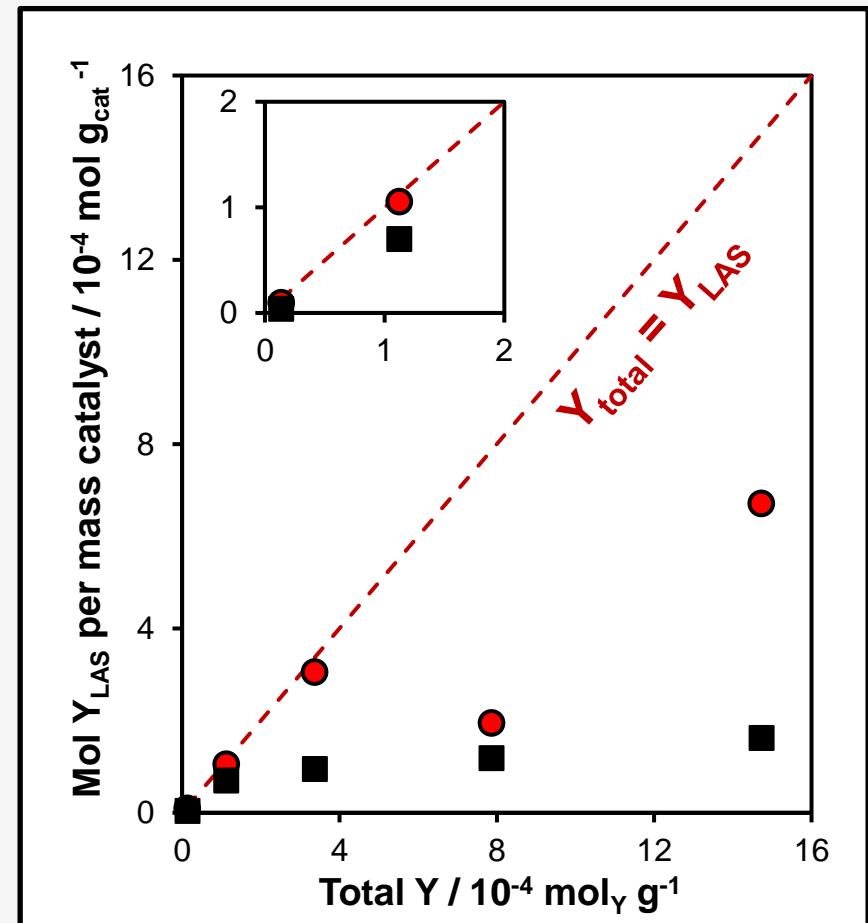
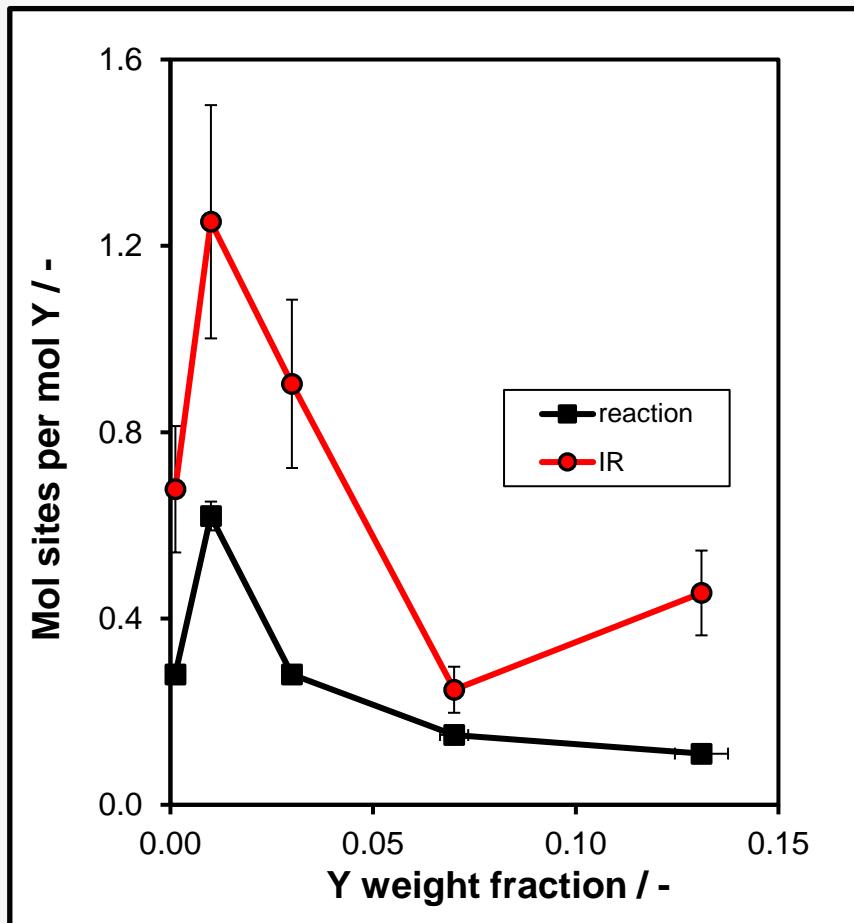
Reaction conditions: T = 503 K; P = 124 kPa;

Gas Flows: 0.4 kPa AcH, 0.000148 kPa Py, 3 kPa EtOH,
0.98 kPa CH₄, bal He; Total flow 100 cm³.min⁻¹;

Catalyst: 0.01 g Y_x/Beta diluted in 0.09 g SiO₂

Borate, Samad, Harris et al., *in prep*

A minority of the total Y binds pyridine during reaction or under vacuum



Reaction conditions: T = 503 K; P = 124 kPa;

Gas Flows: 0.4 kPa Ach, 0.000148 kPa Py, 3 kPa EtOH,
0.98 kPa CH₄, bal He; Total flow 100 cm³.min⁻¹;

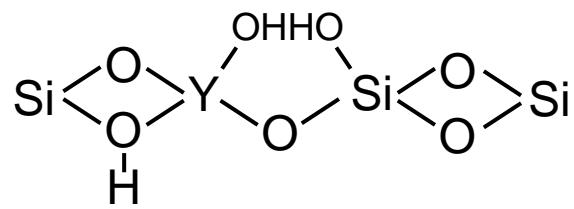
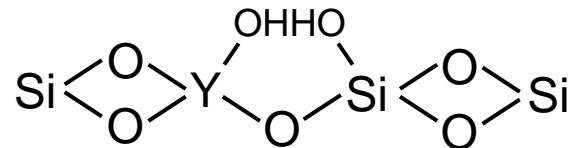
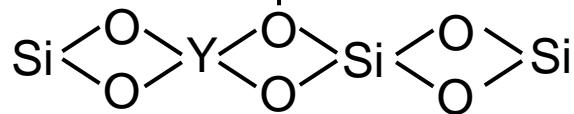
Catalyst: 0.01 g Y_x/Beta diluted in 0.09 g SiO₂

Borate, Samad, Harris et al., *in prep*

What sites are present in Y/deAlBeta samples?

**What are the active sites
and how many are there?**

H⁺

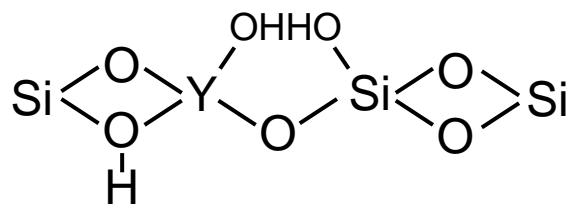
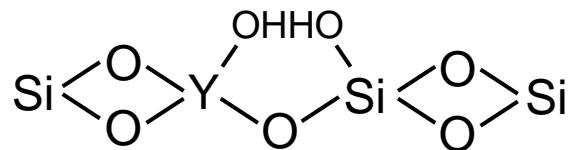
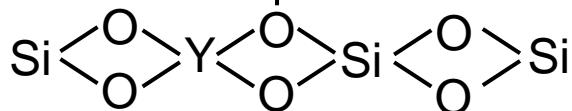


- Minimal H⁺ in Y/deAlBeta
- BD forming sites ≠ sites titrated in IR
- Crotonal forming sites unaffected by pyridine

How do we get from A to D (or E...)?

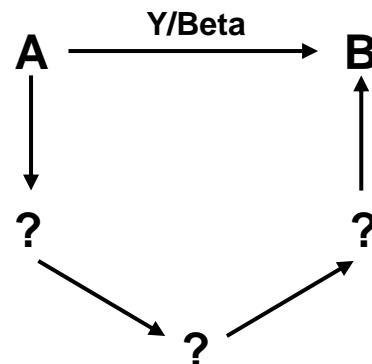
**What are the active sites
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H⁺



- Minimal H⁺ in Y/deAlBeta
- BD forming sites ≠ sites titrated in IR
- Crotonal forming sites unaffected by pyridine

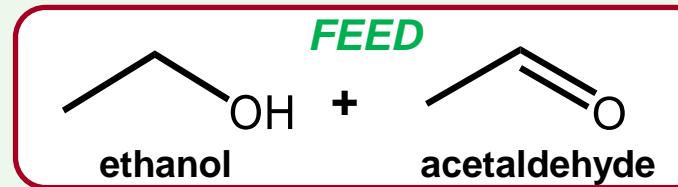
**What is the
reaction pathway?**



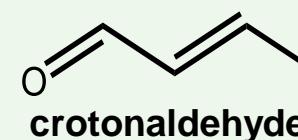
What intermediates?

Proposed Ethanol to Butadiene Reaction Pathway on Y/deAlBeta

Inert environment



Aldol Condensation
Y/deAlBeta



Ag-Zr catalysts

Sushkevich et al., *ChemSusChem*, 7 (2014) 2527-2536

Dagle et al., *Appl. Catal. B.*, 236 (2018) 576-587

Miyake et al., *ACS Sus. Chem. Eng.*, 10 (2022) 1020-1035

Zn and/or Y catalysts

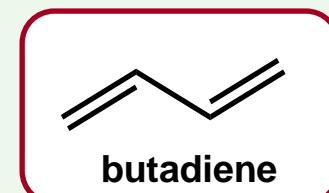
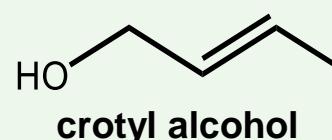
Yan et al., *ACS Catal.*, 8 (2018) 2760-2773

Qi et al., *J. Am. Chem. Soc.*, 142 (2020) 14674-14687

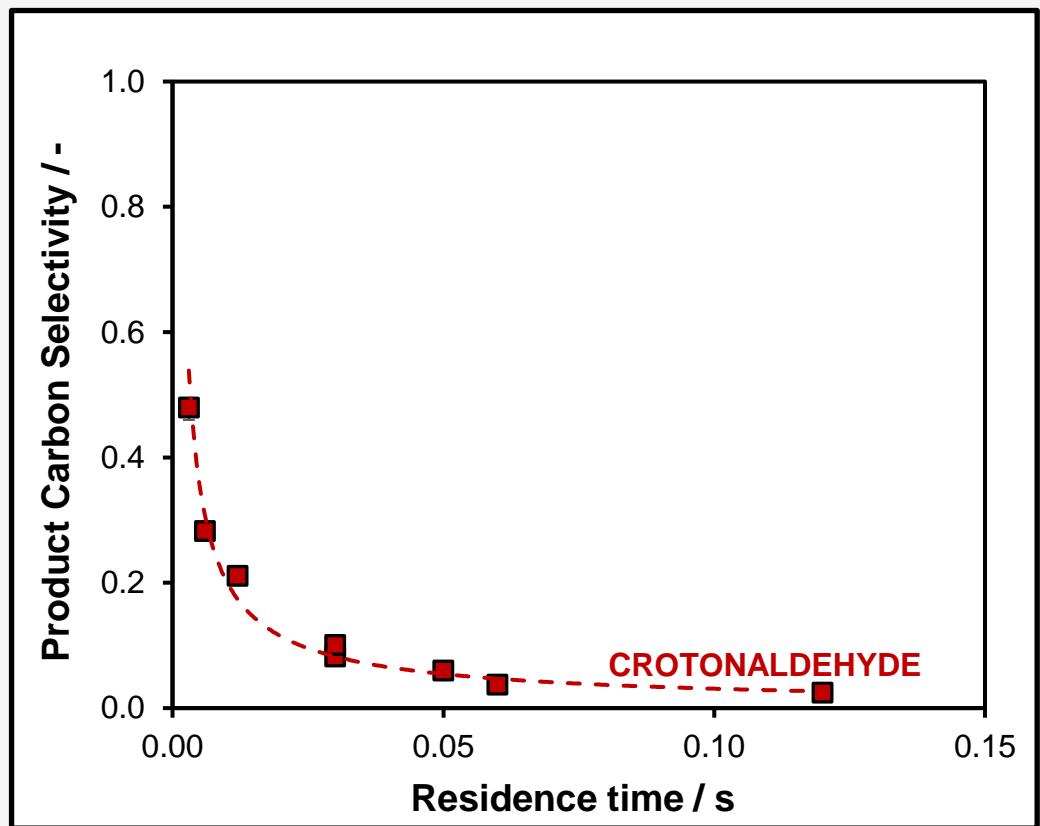
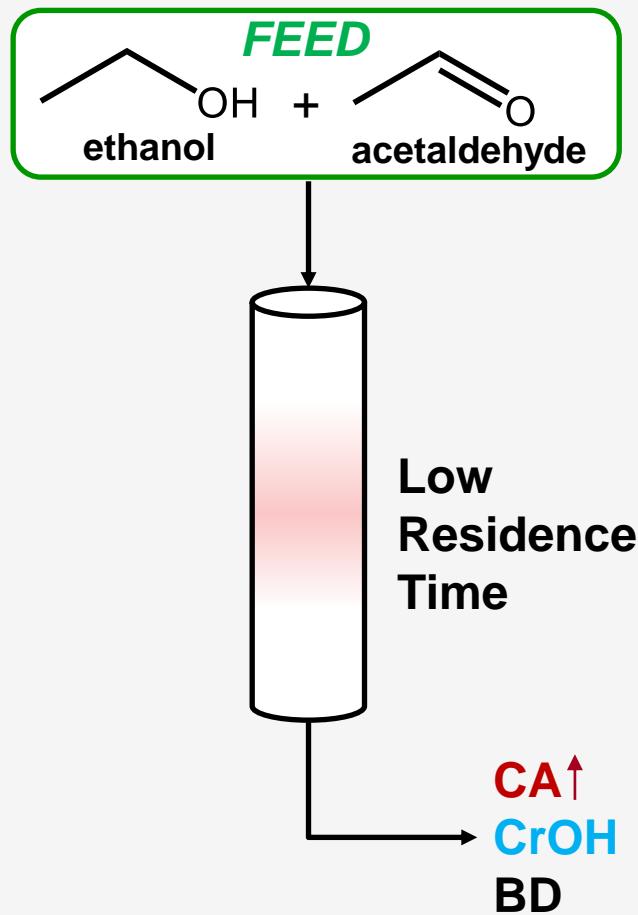
Is crotonaldehyde actually an intermediate en route to butadiene?

**MPV
REDUCTION**
Y/deAlBeta

Dehydration



Probing reaction pathway by varying residence time



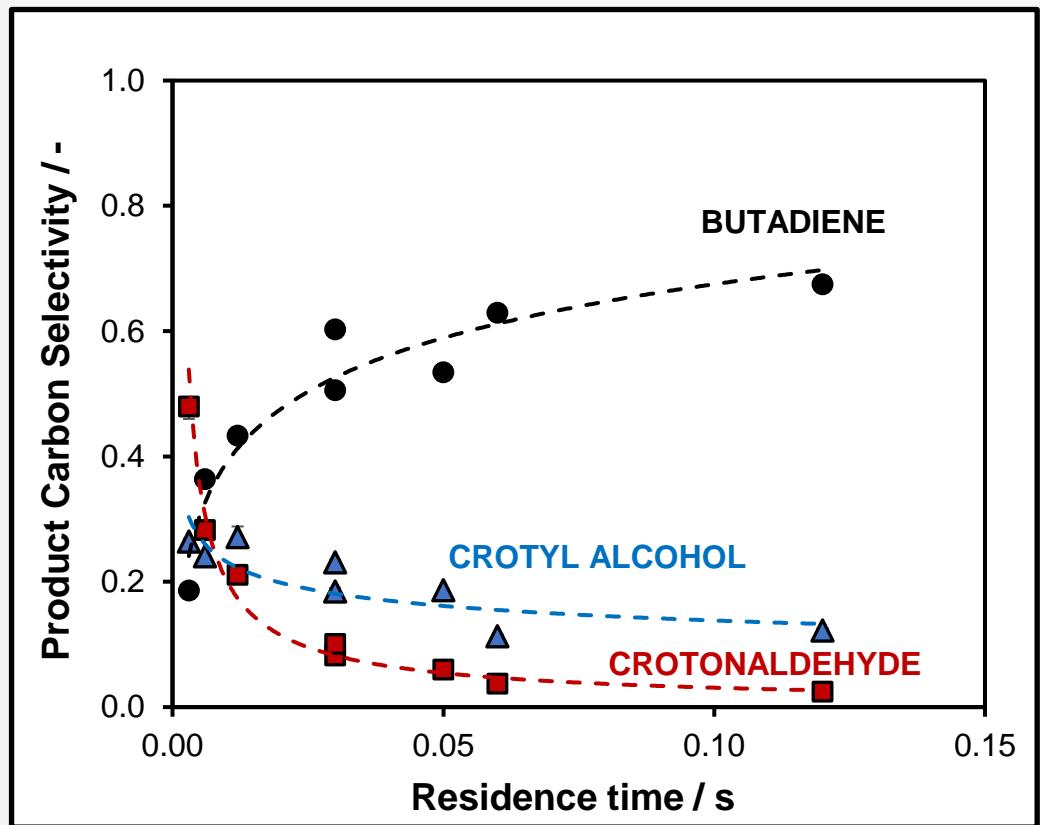
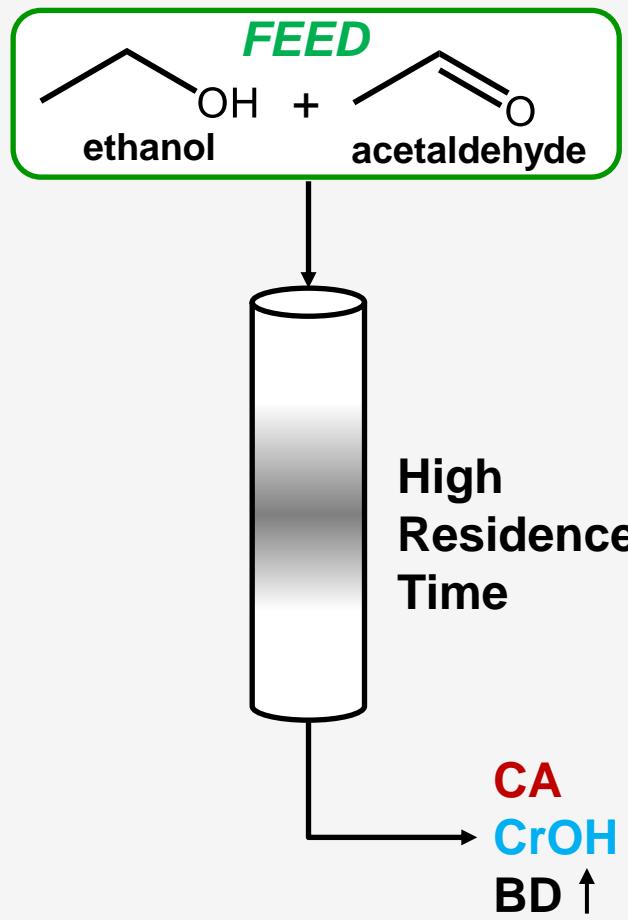
Reaction conditions: T= 503 K;

Gas Flows: $P_{\text{AcH}} = 1 \text{ kPa}$ and $P_{\text{EtOH}} = 5.8 \text{ kPa}$, 0.098 kPa CH_4 , bal He;
Total flowrates varied: $50\text{-}200 \text{ cm}^3 \text{ min}^{-1}$

Catalyst: Pure ~0.1 g $\text{Y}_{0.5}/\text{deAlBeta}$, diluted ~0.01 g $\text{Y}_{0.5}/\text{Beta}$ in ~0.09 g SiC

Borate, Samad, Harris et al., *in prep*

Probing reaction pathway by varying residence time



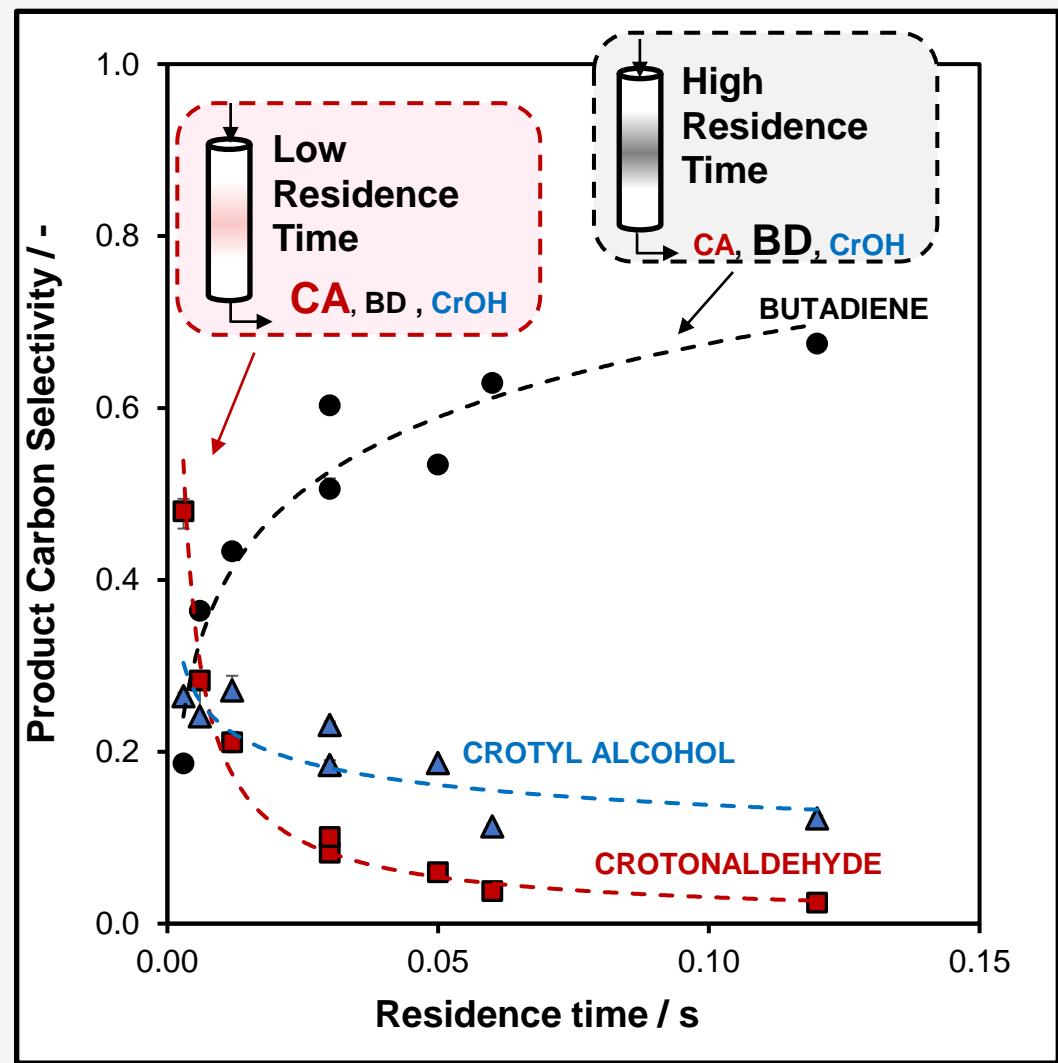
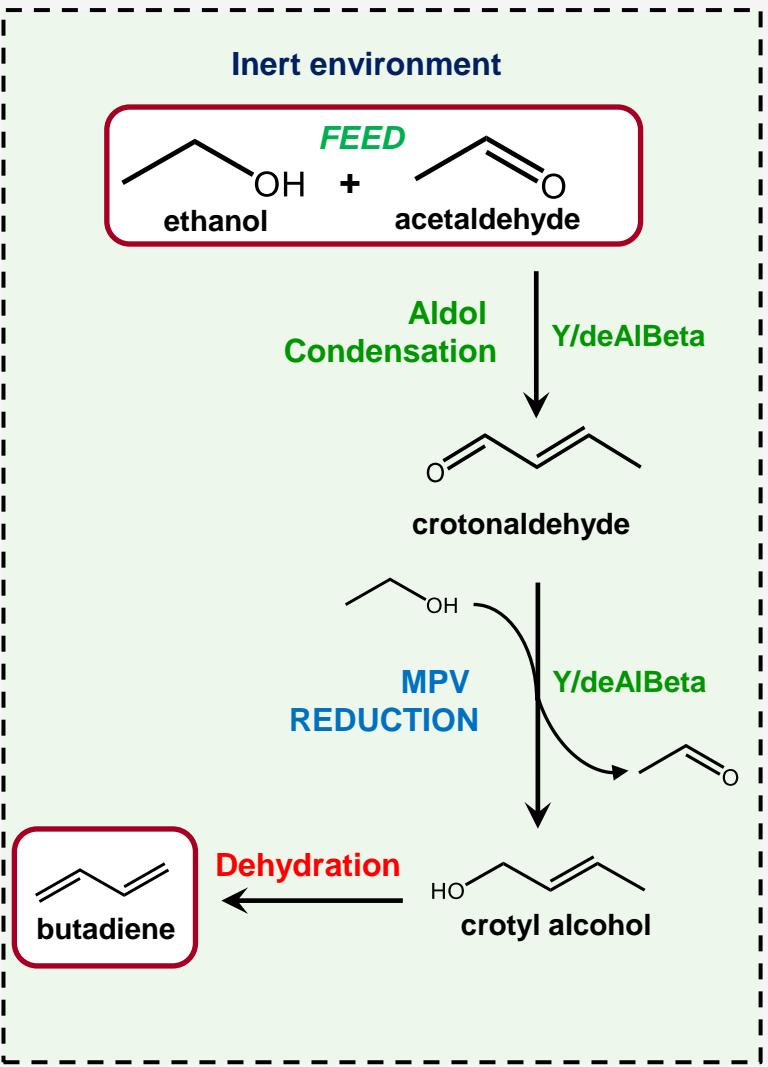
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Borate, Samad, Harris et al., *in prep*

Probing the reaction pathway



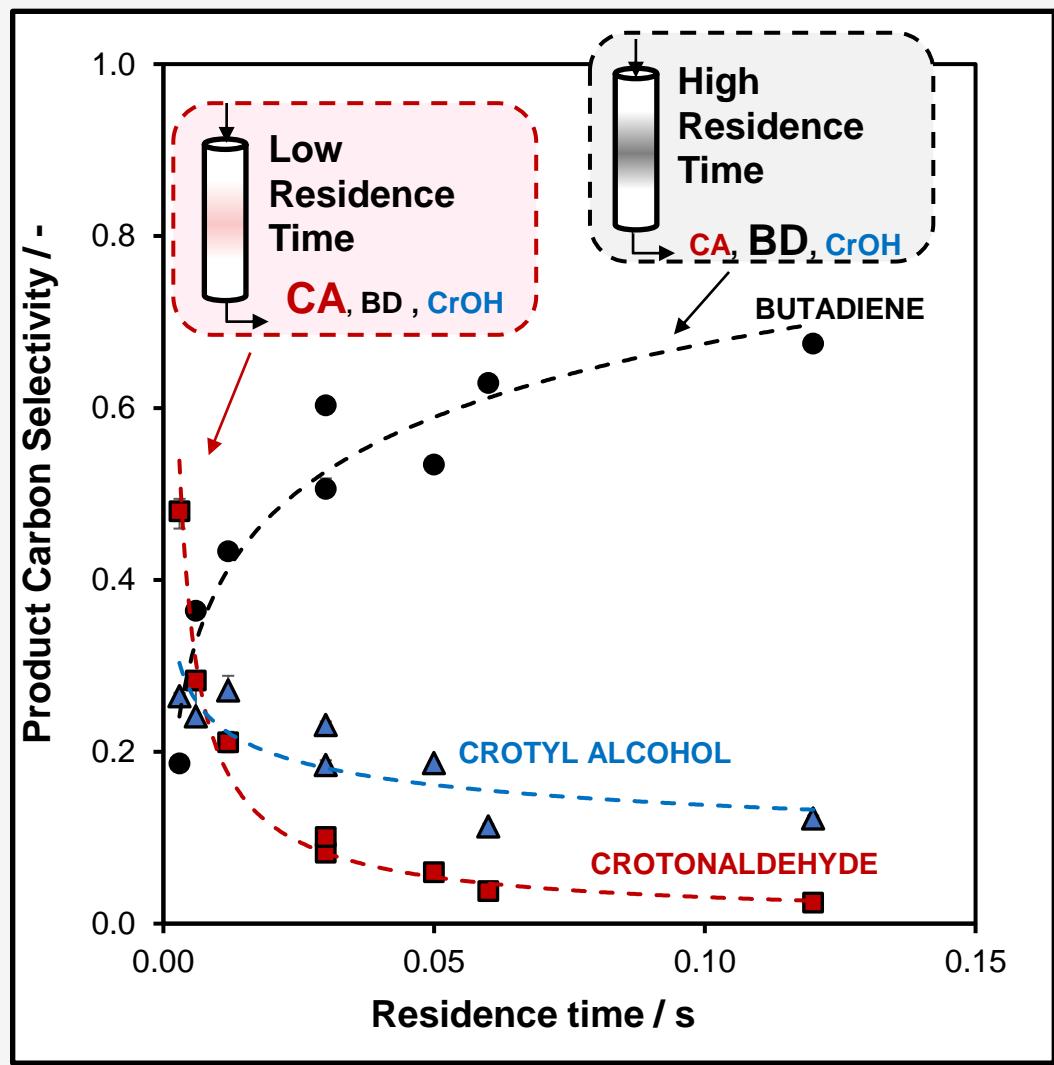
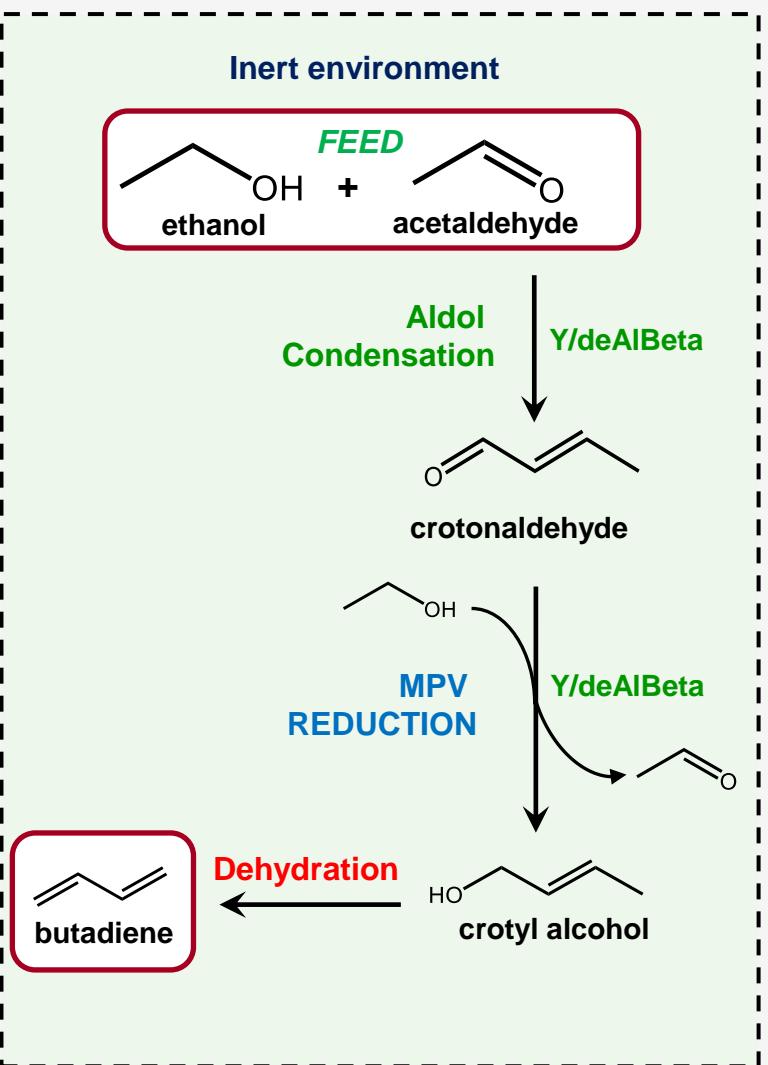
Reaction conditions: T = 503 K;

Gas Flows: $P_{\text{AcH}} = 1 \text{ kPa}$ and $P_{\text{EtOH}} = 5.8 \text{ kPa}$, 0.098 kPa CH_4 , bal He;
Total flowrates varied: 50-200 $\text{cm}^3 \text{ min}^{-1}$

Catalyst: Pure ~0.1 g $\text{Y}_{0.5}/\text{deAlBeta}$, diluted ~0.01 g $\text{Y}_{0.5}/\text{Beta}$ in ~0.09 g SiC

Borate, Samad, Harris et al., *in prep*

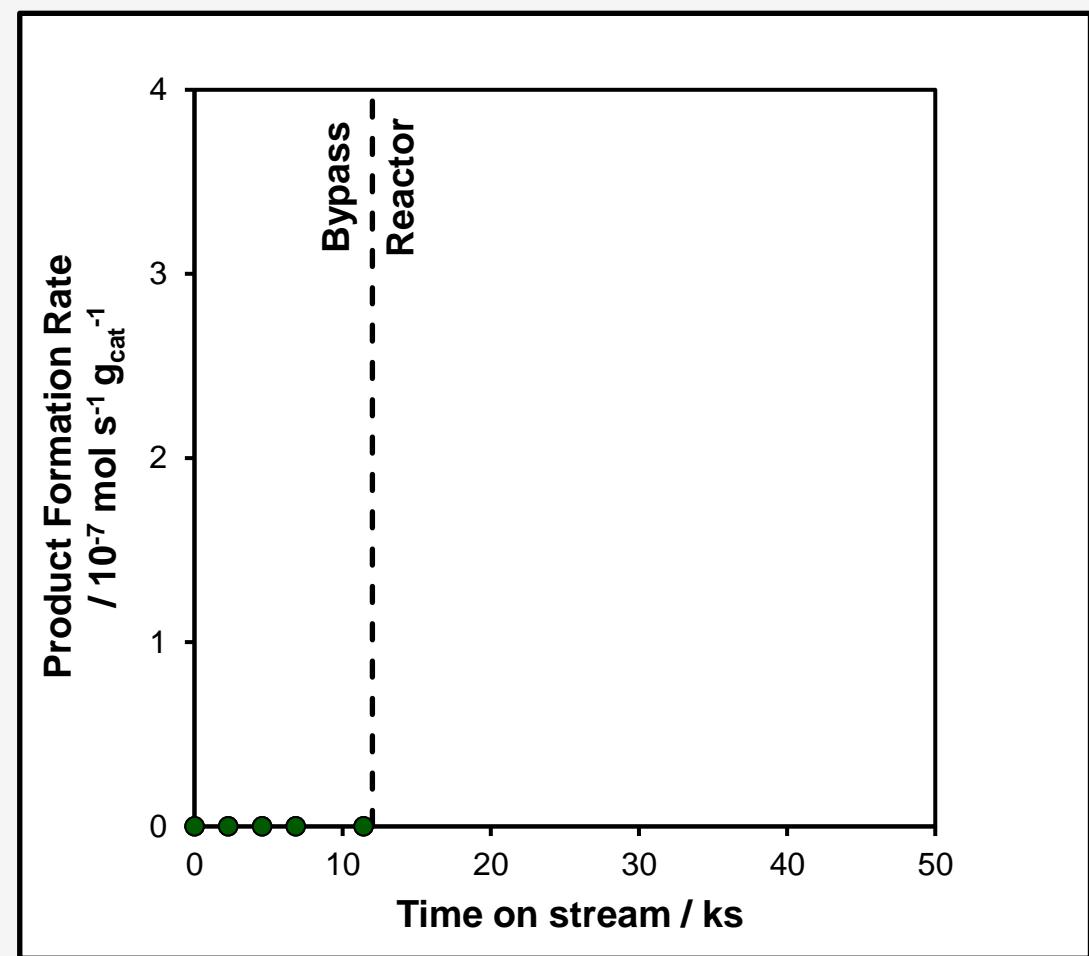
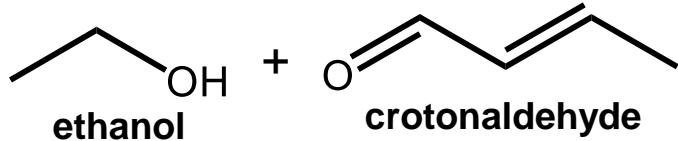
Probing the reaction pathway



Crotonaldehyde is a primary product, butadiene is a terminal product

How is crotonaldehyde consumed? MPV reduction?

FEED



Reaction conditions: T = 483 K; P = 124 kPa

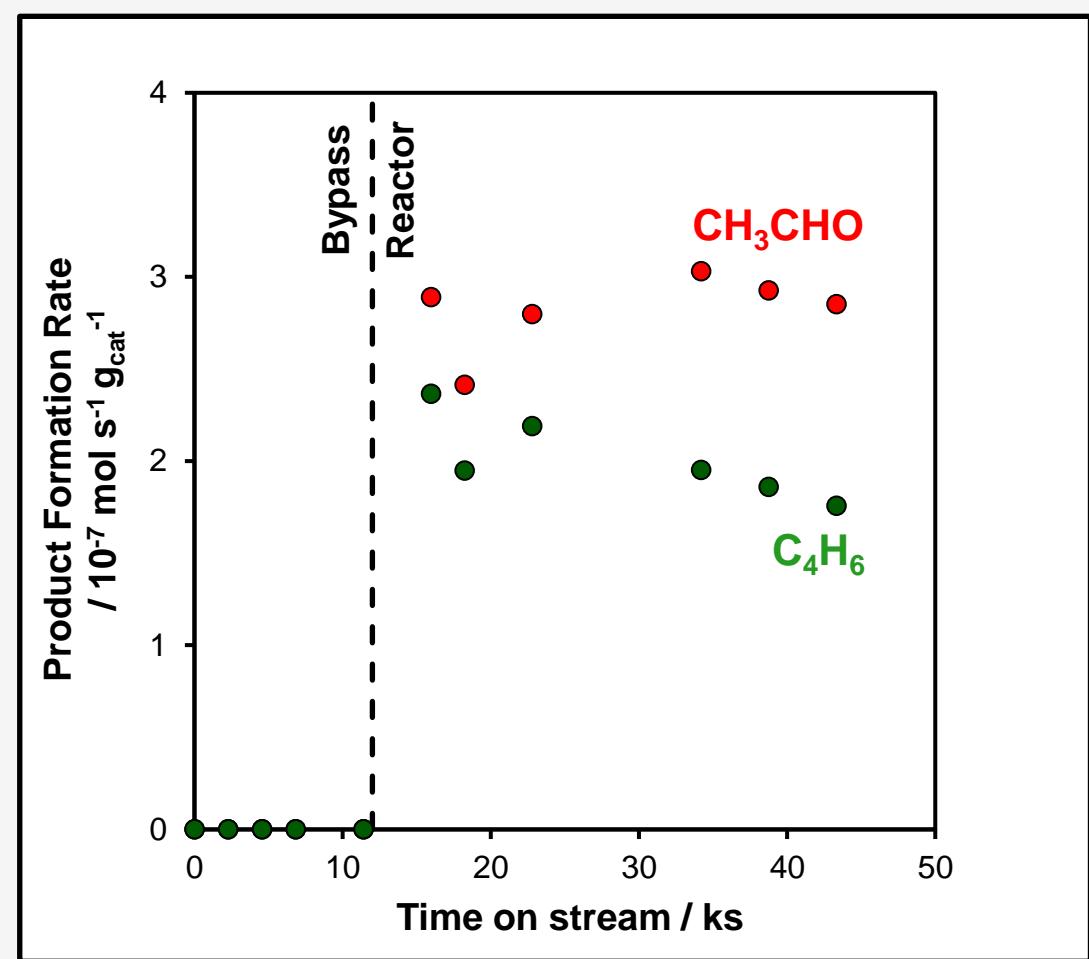
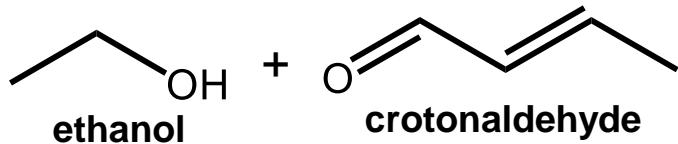
Gas Flows: 0.014 kPa CA, 1 kPa EtOH, 0.98 kPa CH₄, bal He; Total flowrate 100 cm³ min⁻¹

Catalyst: diluted ~0.01 g Y₃/deAlBeta in ~0.09 g SiC

Borate, Samad, Harris et al., *in prep*

How is crotonaldehyde consumed? MPV reduction?

FEED



Reaction conditions: T= 483 K; P=124 kPa

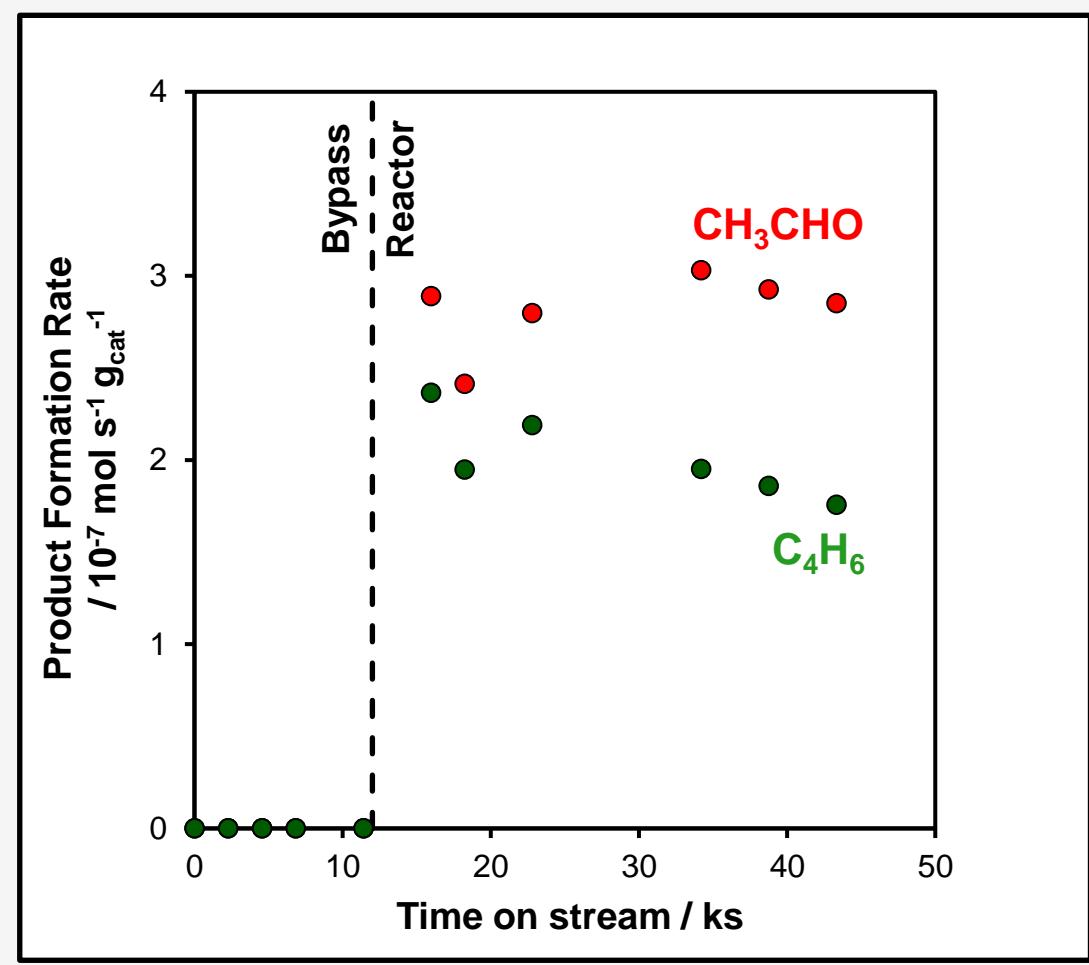
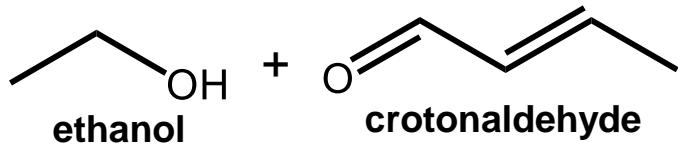
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Catalyst: diluted ~0.01 g Y₃/deAlBeta in ~0.09 g SiC

Borate, Samad, Harris et al., *in prep*

How is crotonaldehyde consumed? MPV reduction?

FEED



Crotonaldehyde reacts with ethanol to form acetaldehyde and BD

Reaction conditions: T= 483 K; P=124 kPa

Gas Flows: 0.014 kPa CA, 1 kPa EtOH, 0.98 kPa CH₄, bal He; Total flowrate 100 cm³ min⁻¹

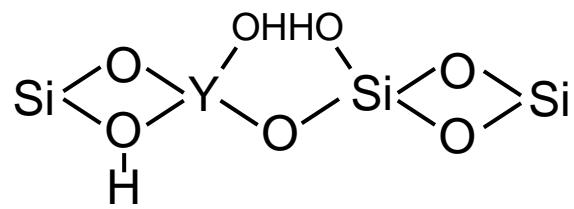
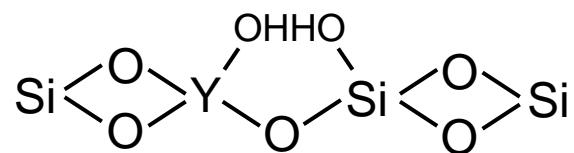
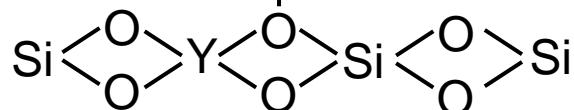
Catalyst: diluted ~0.01 g Y₃/deAlBeta in ~0.09 g SiC

Borate, Samad, Harris et al., *in prep*

How do we get from acetaldehyde and ethanol to butadiene?

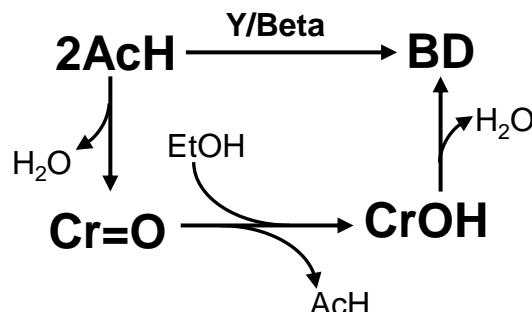
What are the active sites and how many are there?

H⁺



- Minimal H⁺ in Y/deAlBeta
- BD forming sites ≠ sites titrated in IR
- Crotonal forming sites unaffected by pyridine

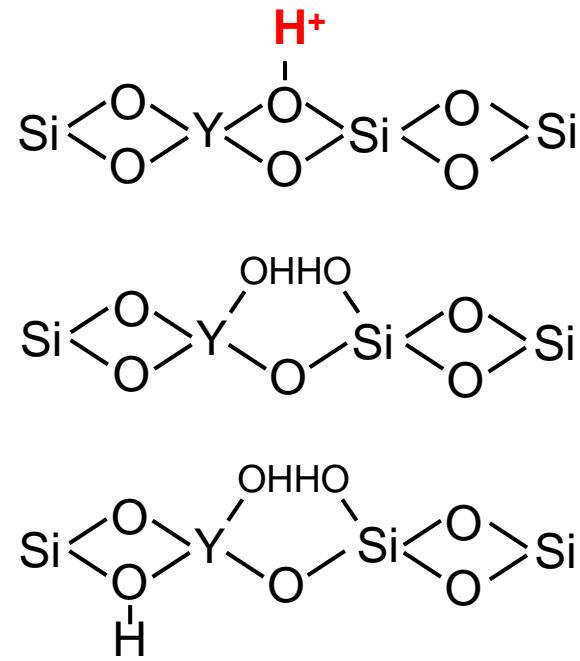
What is the reaction pathway?



- Crotonal is an intermediate that can undergo MPV reduction with ethanol, which leads to BD formation

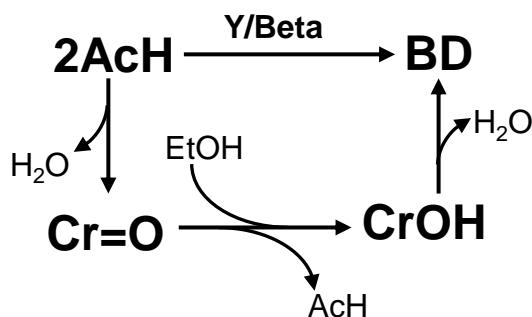
Can we measure kinetics?

What are the active sites and how many are there?



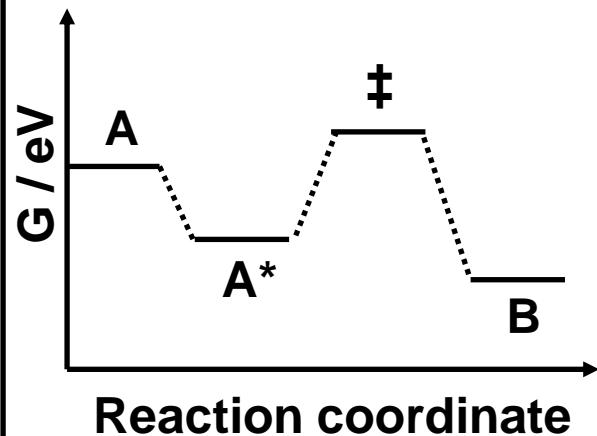
- Minimal H^+ in Y/deAlBeta
- BD forming sites \neq sites titrated in IR
- Crotonal forming sites unaffected by pyridine

What is the reaction pathway?



- Crotonal is an intermediate that can undergo MPV reduction with ethanol, which leads to BD formation

What are the reaction mechanisms?



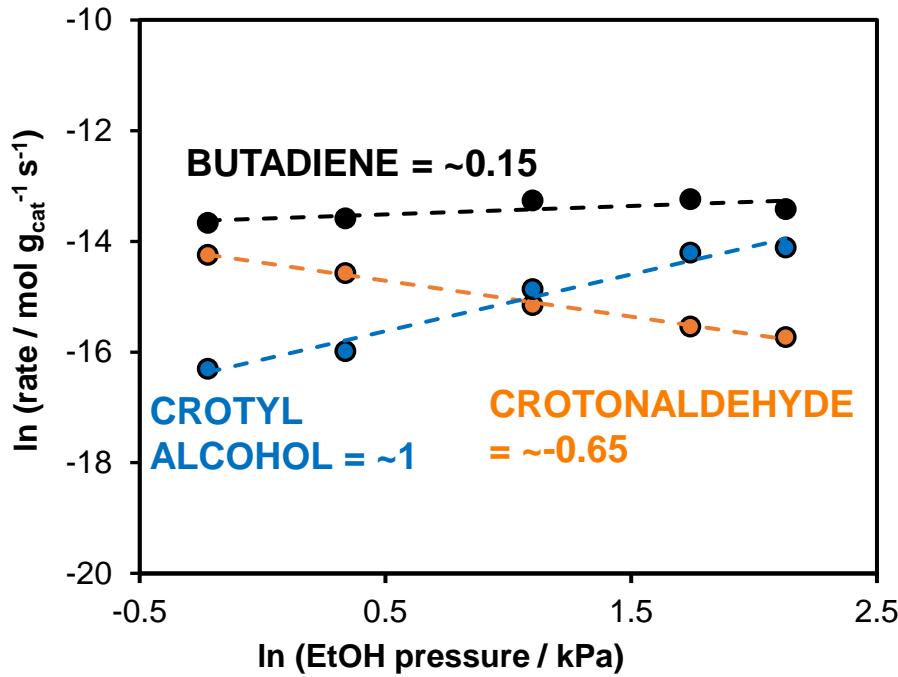
Reaction order test on $Y_{10}/deAlBeta$ (IWI)

**Product rates variation wrt
 P_{EtOH}**

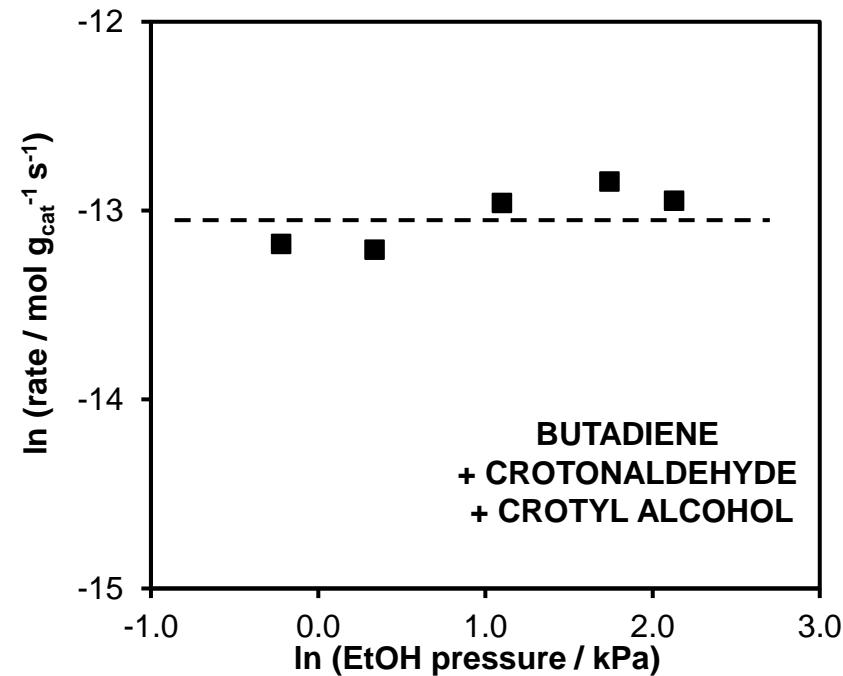
**Sum of C_4 product rate variation
wrt P_{EtOH}**

Ethanol Reaction Order over Y_{10} /deAlBeta (IWI)

**Product rates variation wrt
 P_{EtOH}**



**Sum of C₄ product rate variation
wrt P_{EtOH}**



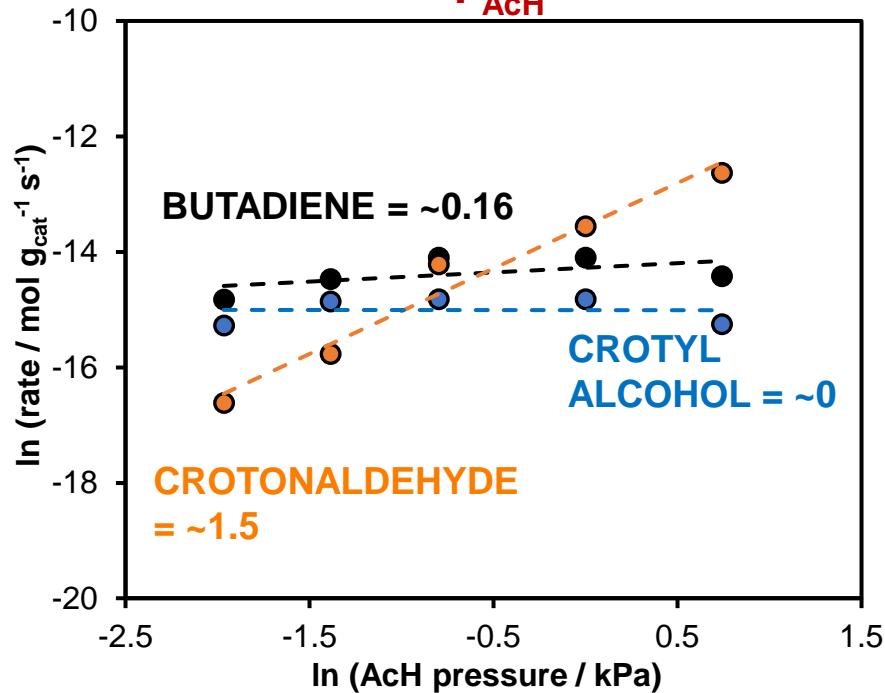
Reaction conditions: T = 503 K; P = 124 kPa

Gas Flows: Partial pressure of EtOH and AcH varied, 0.098 kPa CH₄,
bal He; Total flowrate 100 cm³ min⁻¹

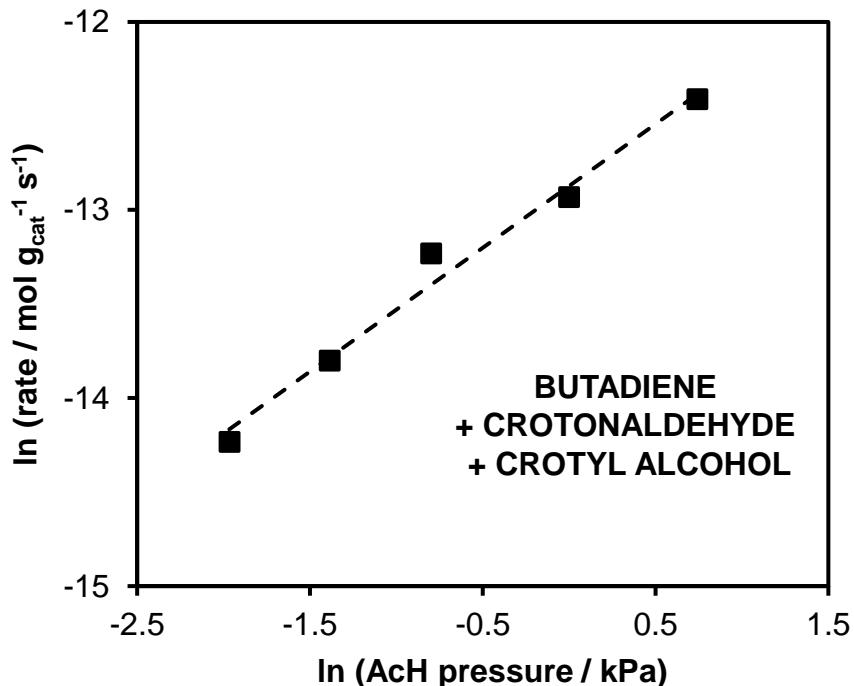
Catalyst: diluted ~0.01 g Y_{10} /deAlBeta in ~0.09 g SiC

Acetaldehyde Reaction Order over Y_{10} /deAlBeta (IWI)

**Product rates variation wrt
 P_{AcH}**



Sum C_4 variation with P_{AcH}



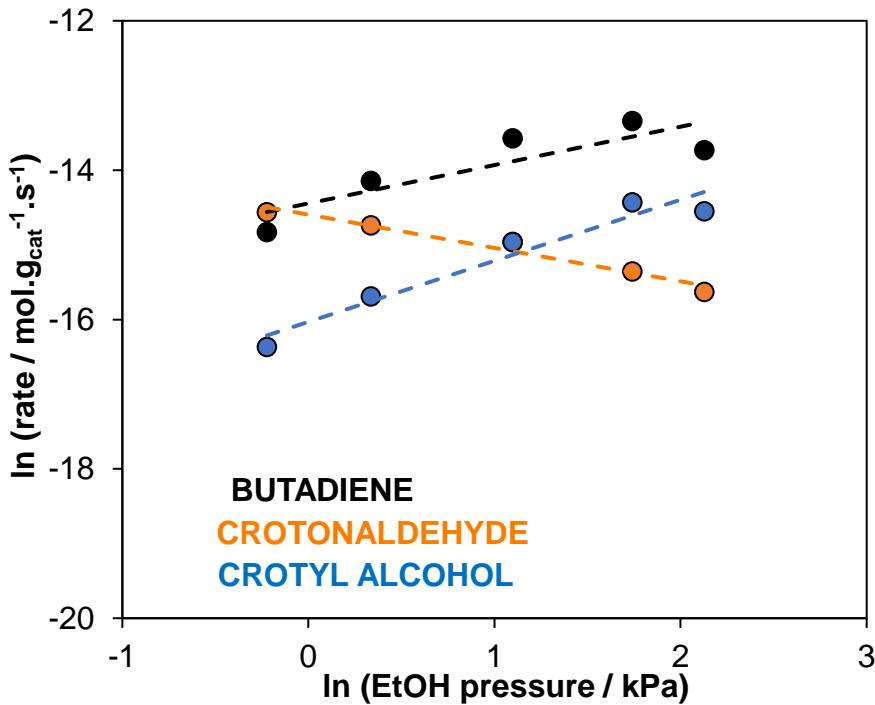
Reaction conditions: T = 503 K; P = 124 kPa

Gas Flows: Partial pressure of EtOH and AcH varied, 0.098 kPa CH₄,
bal He; Total flowrate 100 cm³ min⁻¹

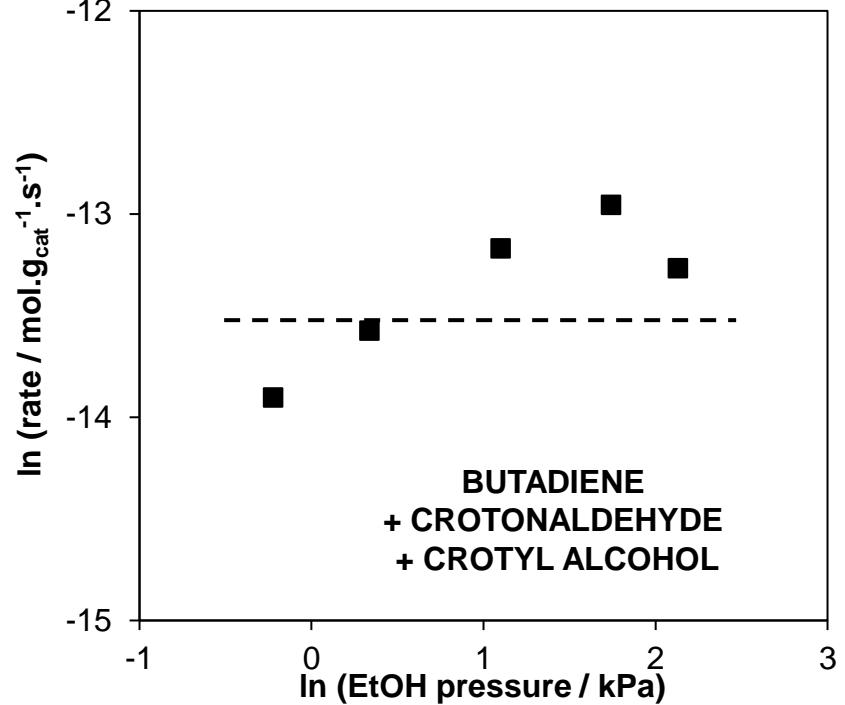
Catalyst: diluted ~0.01 g Y_{10} /deAlBeta in ~0.09 g SiC

Reaction order test on $\text{La}_4/\text{deAlBeta}$ (IWI)

**Product rates variation wrt
 P_{EtOH}**



**Sum of C_4 product rate
variation wrt P_{EtOH}**



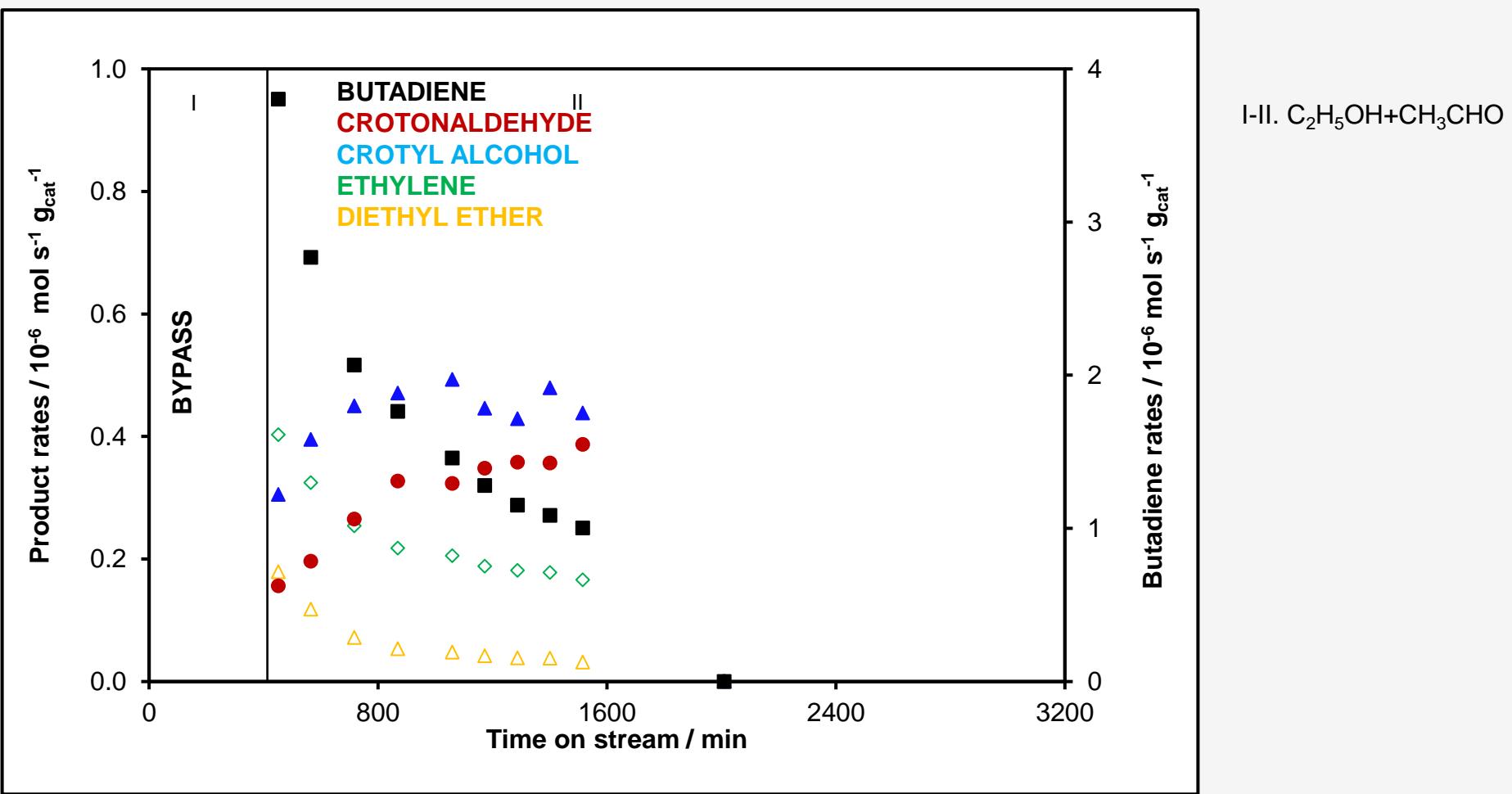
Kinetic dependencies likely vary with identity of the rare earth metal

Reaction conditions: T= 503 K; P=124 kPa

Gas Flows: Partial pressure of EtOH and AcH varied, 0.098 kPa CH₄,
bal He; Total flowrate 100 cm³ min⁻¹

Catalyst: diluted ~0.01 g La₄/deAlBeta in ~0.09 g SiC

Kinetic isotope effect experiments on Y₅/deAlBeta

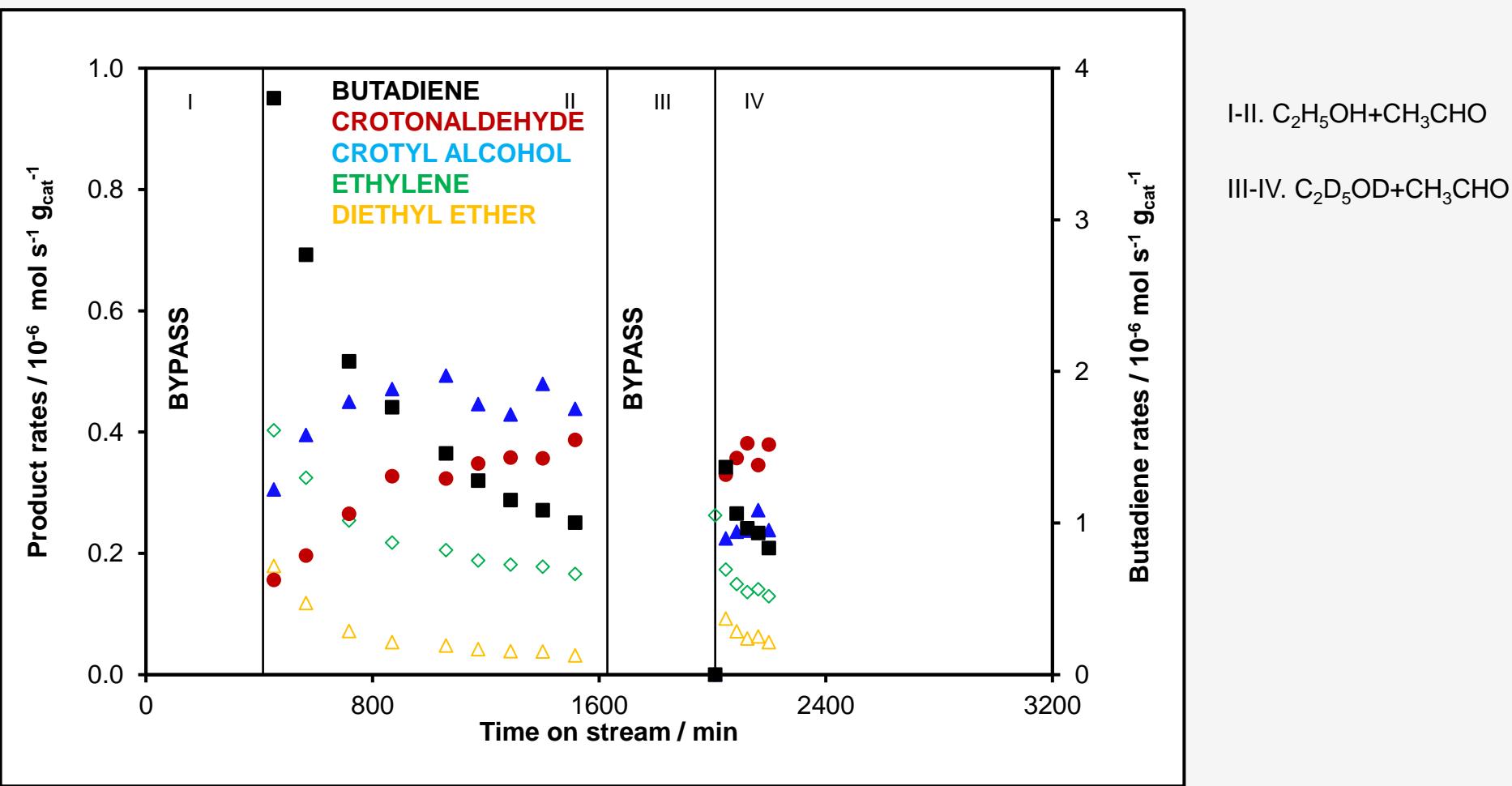


Reaction conditions: T= 503 K, P= 124 kPa

Gas flows: 1.5 kPa EtOH, 0.2 kPa AcH (H form reagents: panels II and VIII, D-form EtOH and H-form AcH panel IV, D-form EtOH and AcH: panel VI, Bypass conditions: panels I, III, V and VII), 0.98 kPa CH₄, Balance He. Total flow 50 cm³ min⁻¹

Catalyst: 0.01 g Y₅/deAlBeta(19) diluted with 0.09 g SiC

Kinetic isotope effect experiments on Y₅/deAlBeta

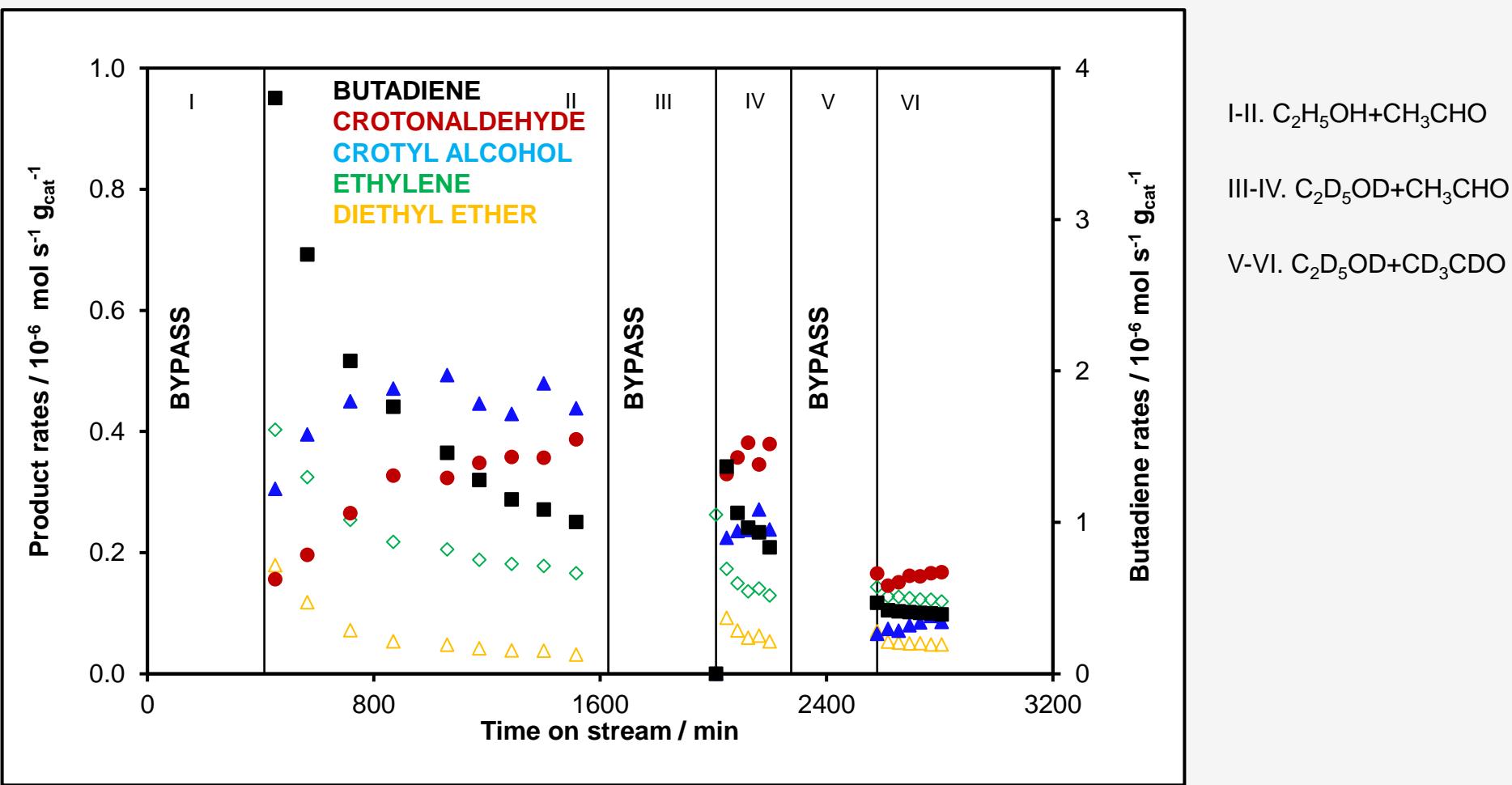


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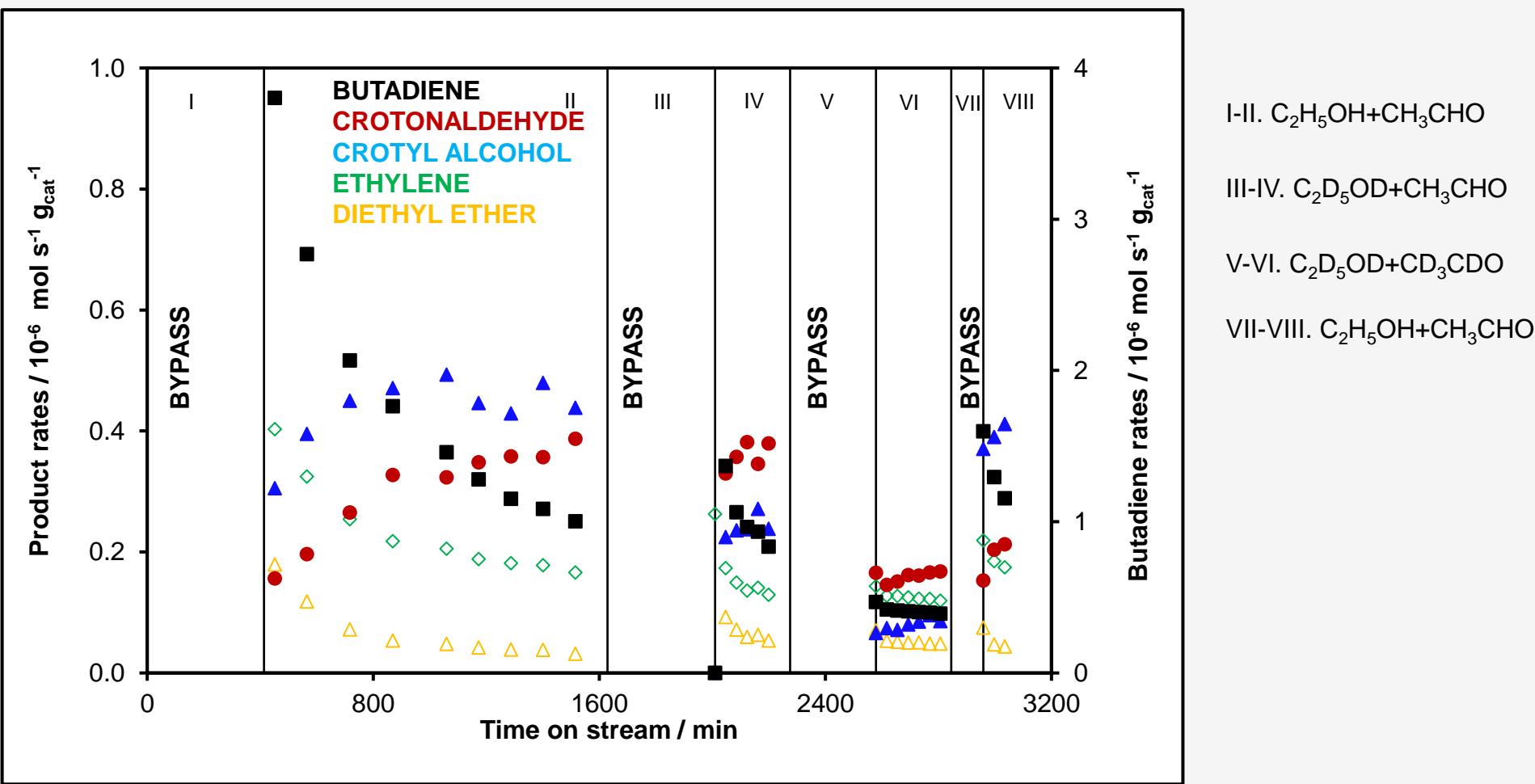


Reaction conditions: T= 503 K, P= 124 kPa

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Catalyst: 0.01 g Y₅/deAlBeta(19) diluted with 0.09 g SiC

Kinetic isotope effect experiments on Y₅/deAlBeta



Reaction conditions: T= 503 K, P= 124 kPa

Gas flows: 1.5 kPa EtOH, 0.2 kPa AcH (H form reagents: panels II and VIII, D-form EtOH and H-form AcH panel IV, D-form EtOH and AcH: panel VI, Bypass conditions: panels I, III, V and VII), 0.98 kPa CH₄, Balance He. Total flow 50 cm³ min⁻¹

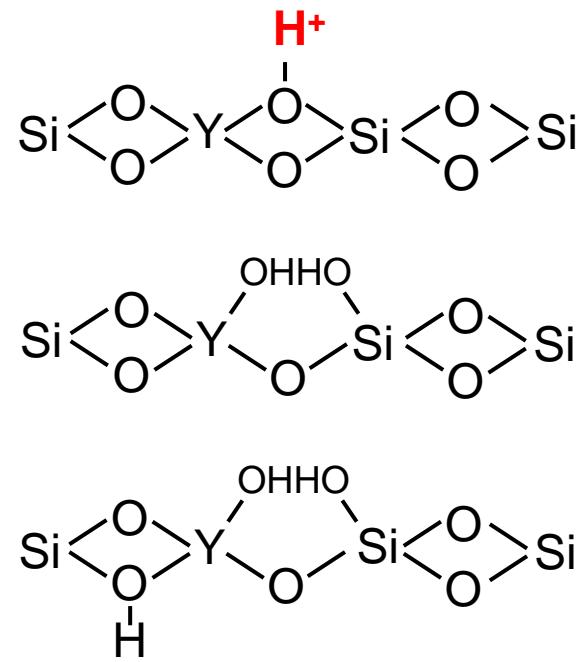
Catalyst: 0.01 g Y₅/deAlBeta(19) diluted with 0.09 g SiC

Isotopic labeling experiments on Y₅/deAlBeta

Products	Measured rates averaged / 10 ⁻⁶ mol s ⁻¹ g _{cat} ⁻¹				KIE values	
	R _H -initial	R _H -final	R _D -EtOH D ₆	R _D -EtOH D ₆ +AcH-D ₄	R _H /R _D only ethanol labeled	R _H /R _D both labeled
Butadiene	1.08	1.23	0.91	0.40	1.2	3.1
Crotonaldehyde	0.37	0.21	0.37	0.16	1.0	1.3
Crotyl alcohol	0.45	0.40	0.25	0.09	1.8	4.6
Total C₄	1.90	1.83	1.53	0.65	1.2	2.8
Ethylene	0.18	0.18	0.14	0.12	1.3	1.5
DEE	0.04	0.05	0.06	0.05	0.6	0.9

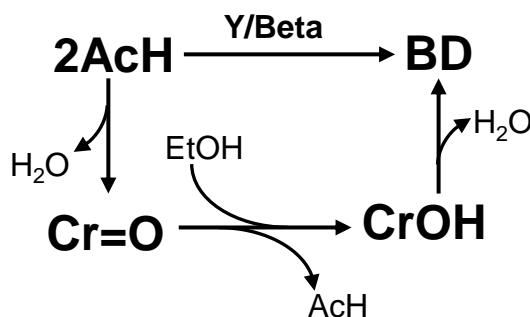
Can we measure kinetics?

What are the active sites and how many are there?



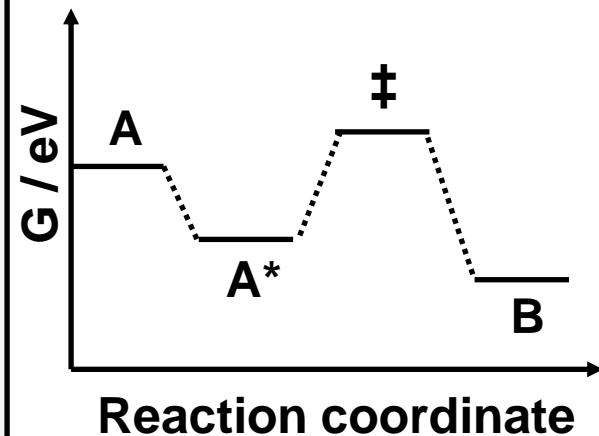
- Minimal H^+ in $\text{Y}/\text{deAlBeta}$
- BD forming sites \neq sites titrated in IR
- Crotonal forming sites unaffected by pyridine

What is the reaction pathway?



- Crotonal is an intermediate that can undergo MPV reduction with ethanol, which leads to BD formation

What are the reaction mechanisms?



- C_4+ product formation is:
 - ~0 order in $\text{C}_2\text{H}_5\text{OH}$
 - >1st order in CH_3CHO

Acknowledgements

U. Alabama

- Nohor “River” Samad (M.S. 2022, Westrock)
- Sumin Lee (B.S. 2020; Ga. Tech)
- Ryan Kitchen (B.S. 2022)
- Chase McGee (REU 2022, U. Conn.)
- Zahra Almohamedhusain (B.S. 2024)

Johns Hopkins U.

- Prof. Brandon Bukowski
- Prof. Michael Tsapatsis

Oak Ridge National Laboratory

- Dr. Junyan Zhang
- Dr. Michael Cordon
- Dr. Stephen Purdy
- Dr. Meijun Li
- Dr. Andrew Sutton
- Dr. Zhenglong Li (Now: Zhejiang University, China)



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ORAU

2021-2022 Ralph E. Powe
Award

Questions?

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